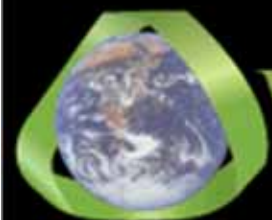


Sulphur Recirculation for reducing corrosion and increasing electrical efficiency in WtE boilers

Dr. Sven Andersson

Götaverken Miljö AB, Sweden

– a Babcock & Wilcox Vølund company



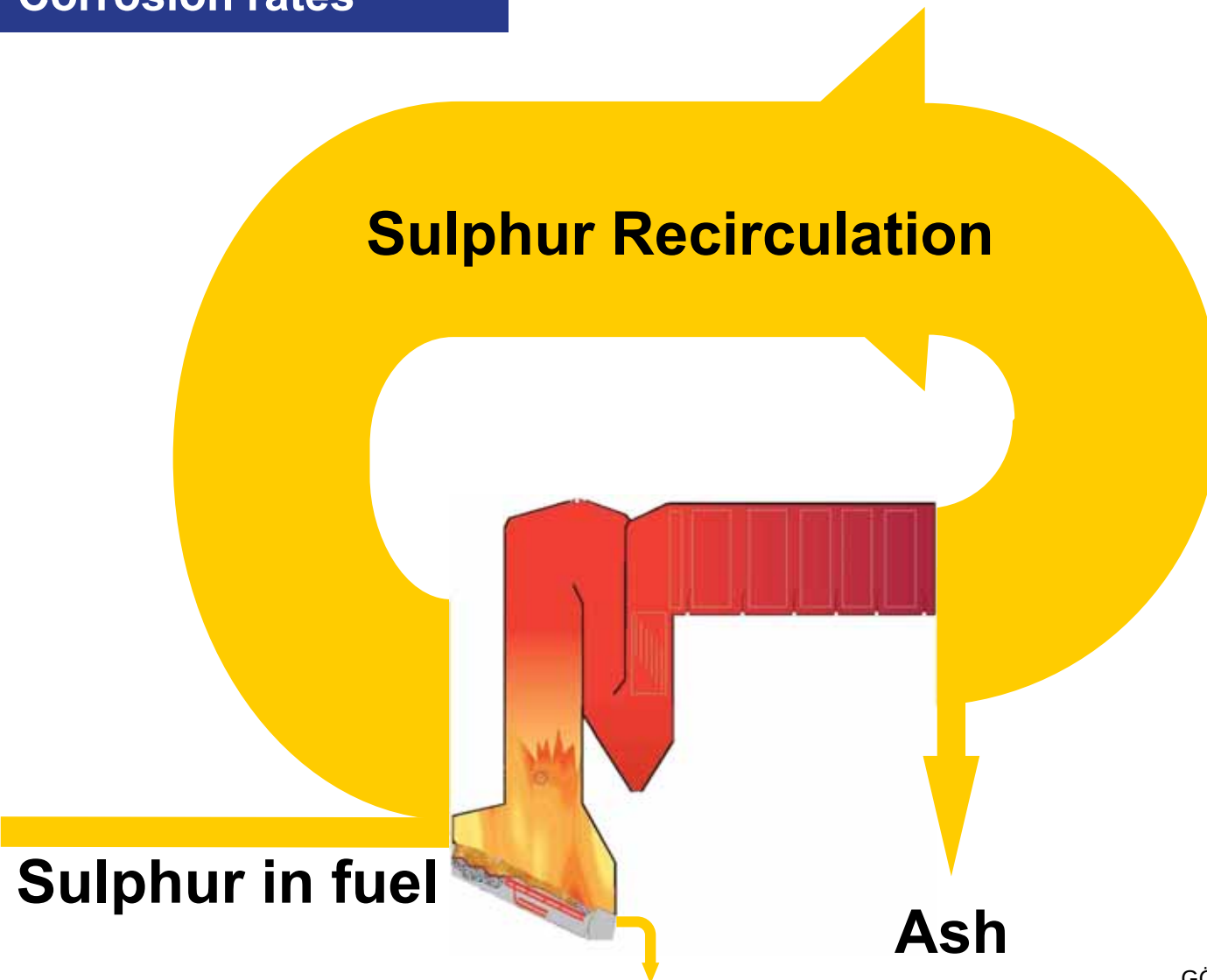
WTERT

Waste-to-Energy Research and Technology Council

Advancing Sustainable Waste Management

Operating principles
Full-scale operation
Ashes and deposits
Emissions
Corrosion rates

Sulphur Recirculation

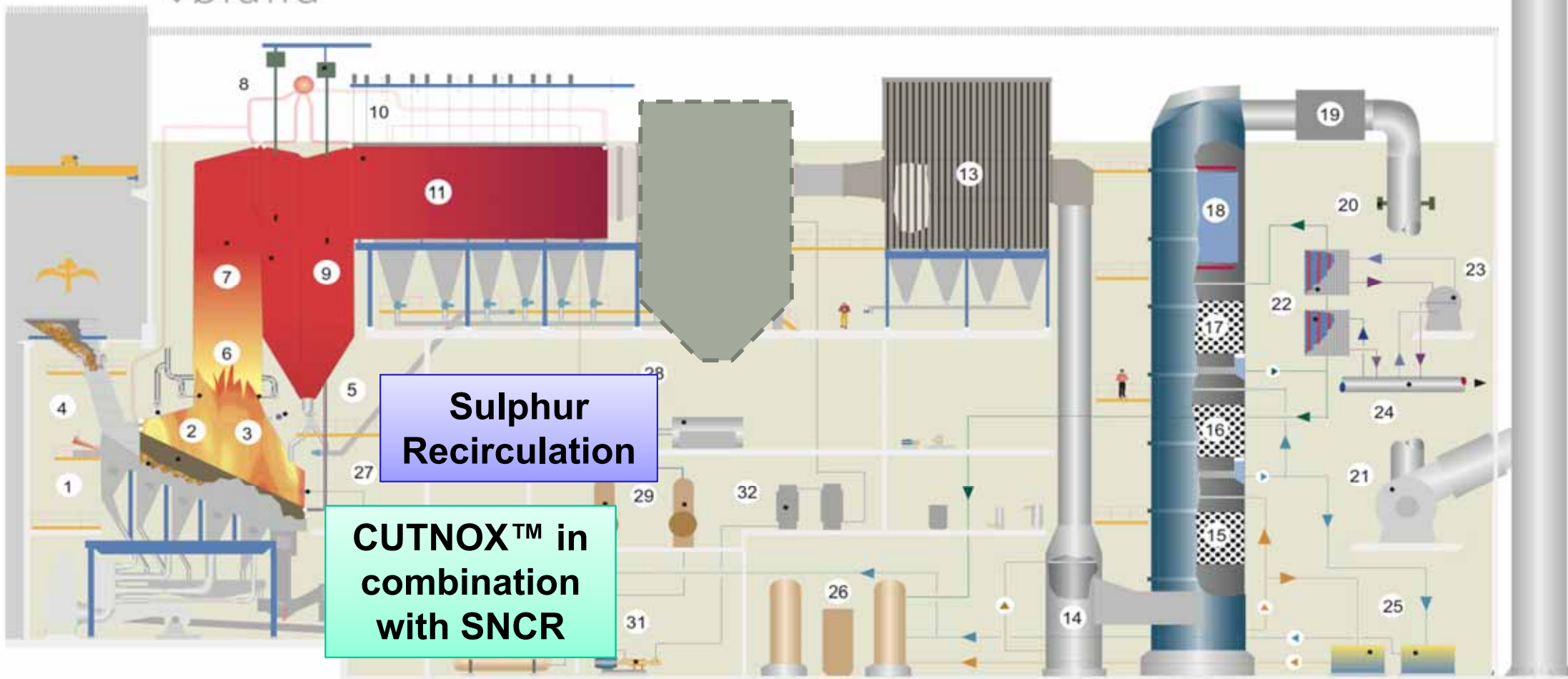


Operating principles
Full-scale installation
NO_x reduction



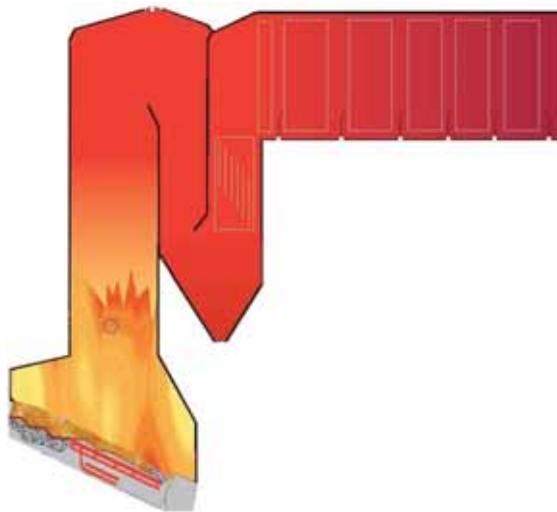
HCl / SO₂ / NH₃
Hg
Dioxins
NO_x
Fine particles
Energy recovery

B&W
vølund

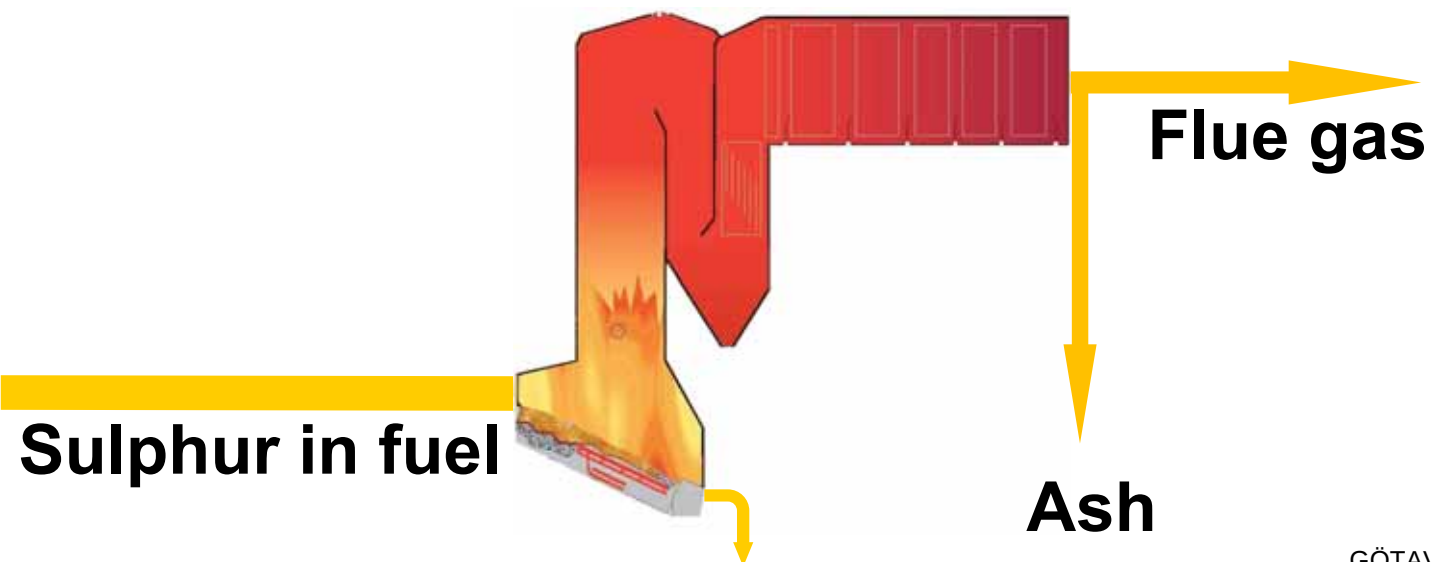


Electricity production in WtE is limited by superheater corrosion

**Biomass or waste
fired boiler**



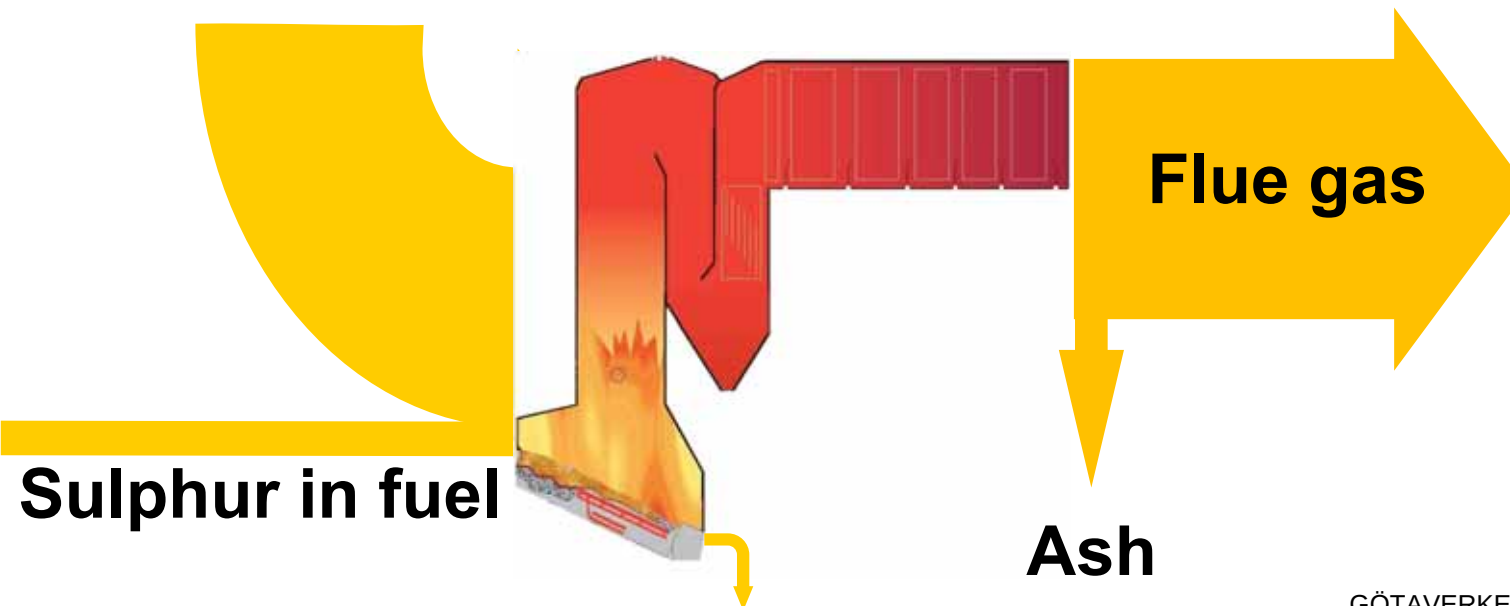
Sulphur mass balance



Sulphur dosage inhibits corrosion

Higher SO_2 concentration:
Alkali chlorides → alkali sulphates
(corrosive) (non corrosive)

Sulphur dosage



Sulphur Recirculation for High Efficiency, Low Corrosion WtE

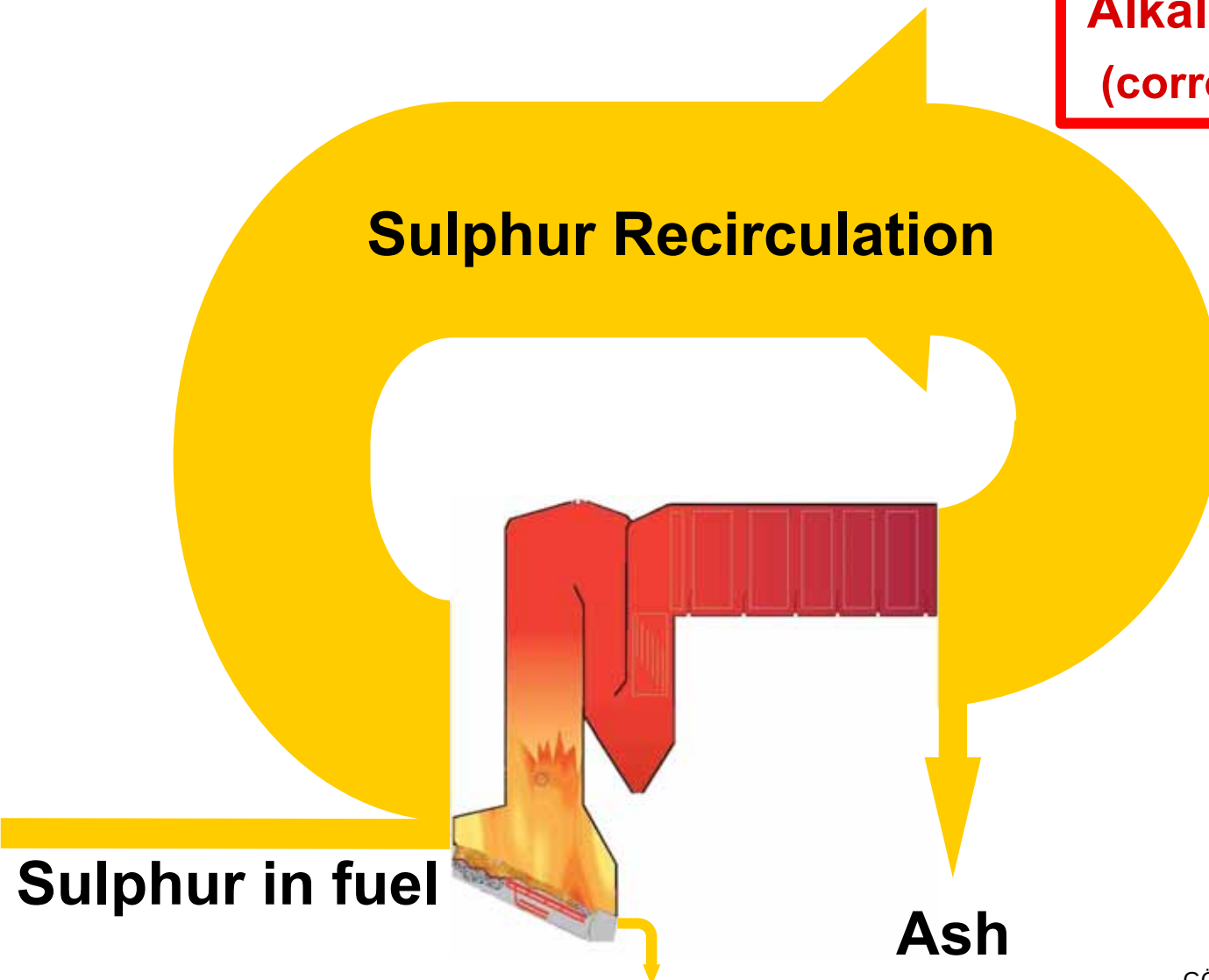


Higher SO₂ concentration:
Alkali chlorides → alkali sulphates
(corrosive) (non corrosive)

CHALMERS

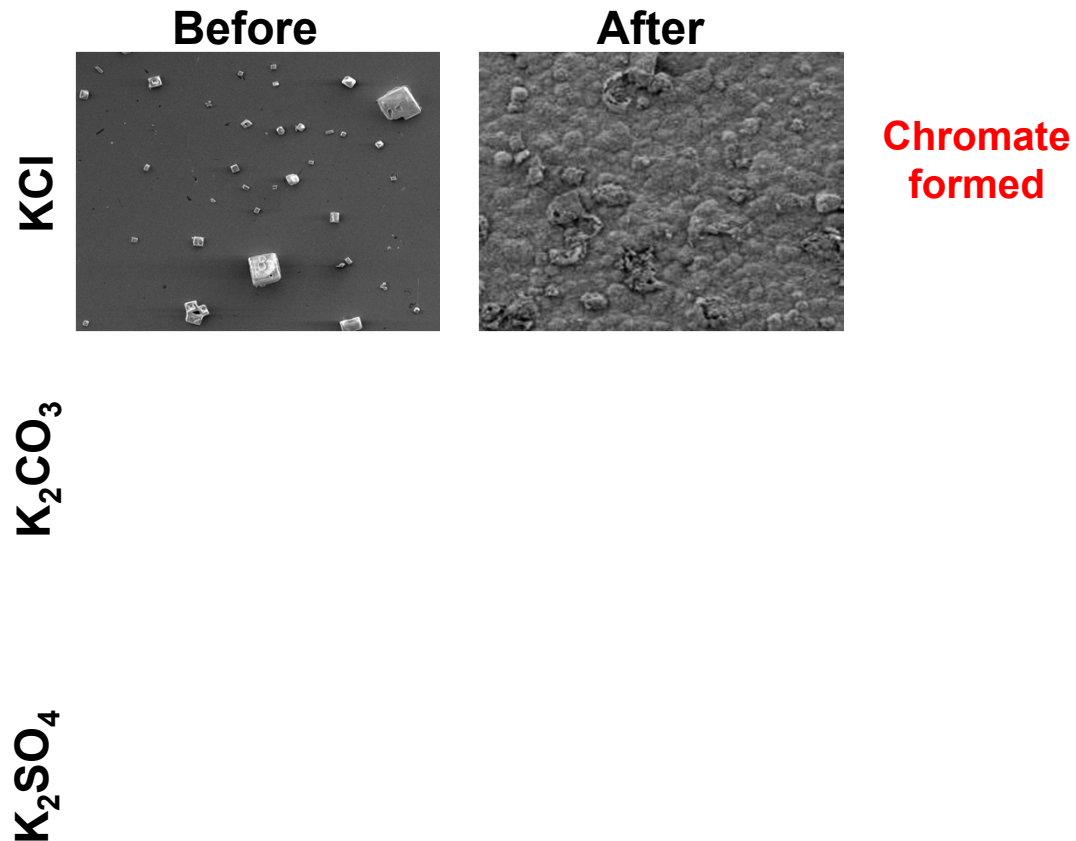
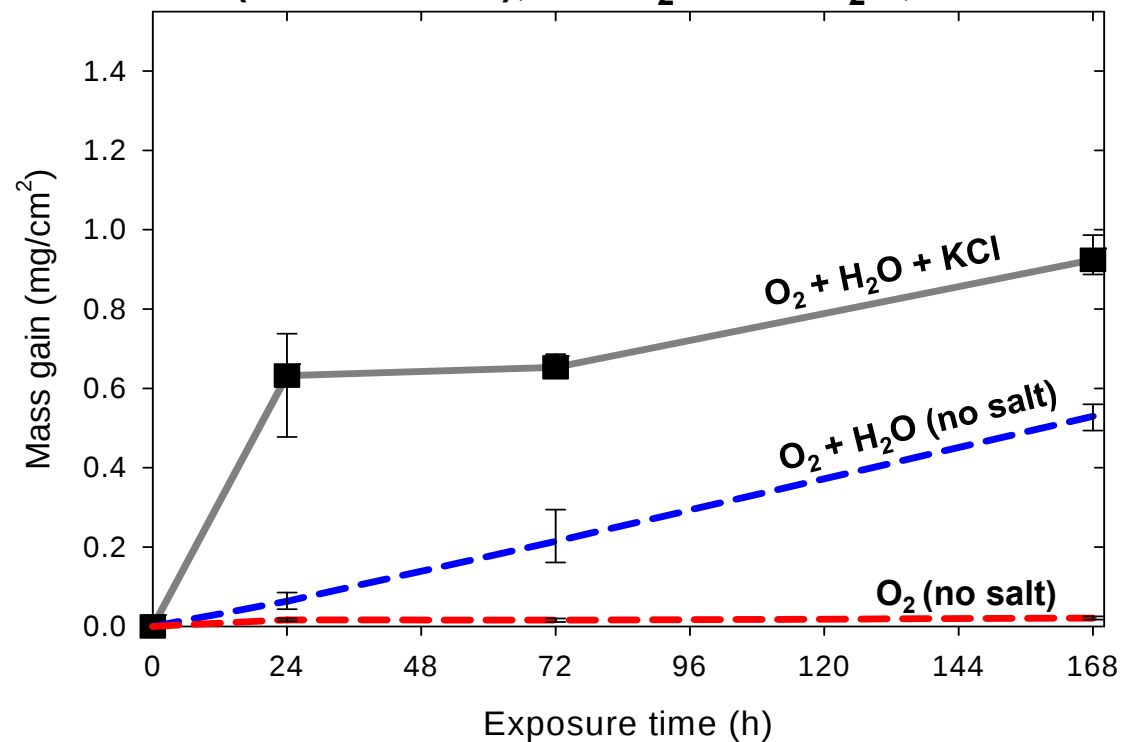


ProEnviro



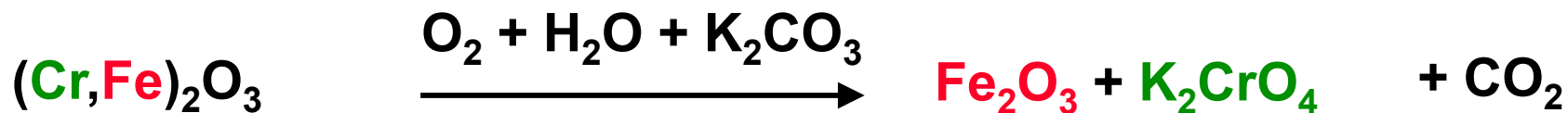
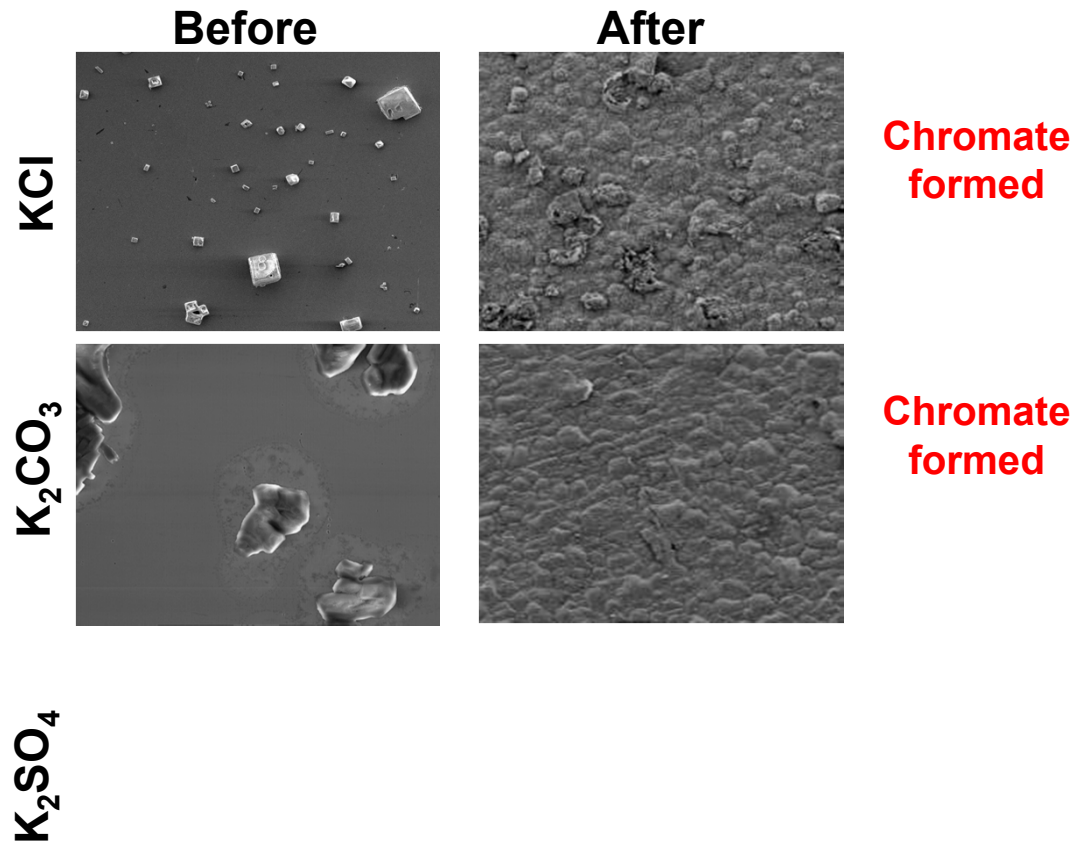
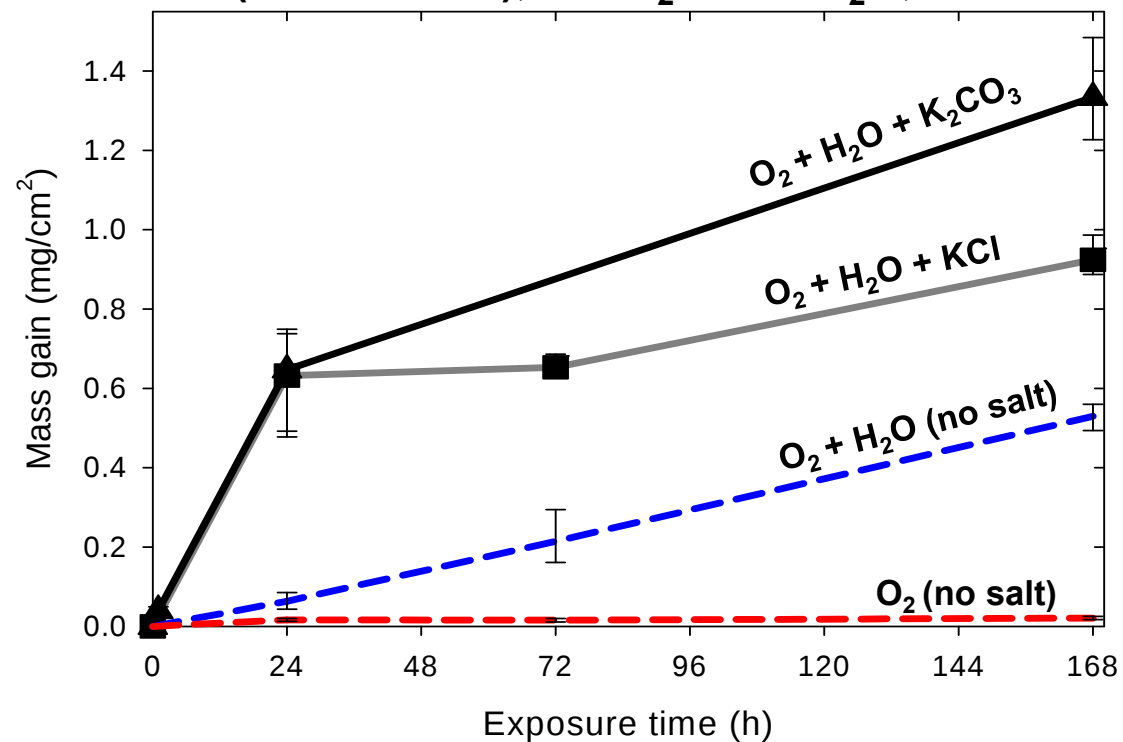
The effect of chromium depletion on chromia forming steels

304L (Fe20Cr10Ni), 5% O₂ + 40% H₂O, 600°C



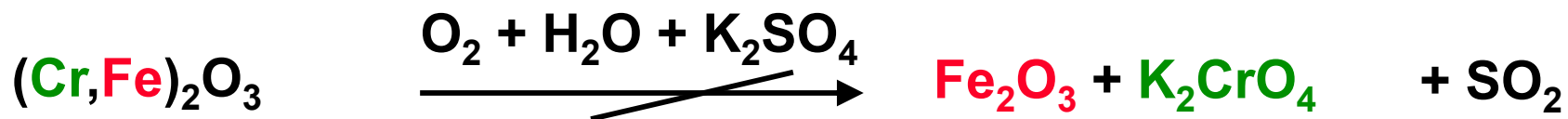
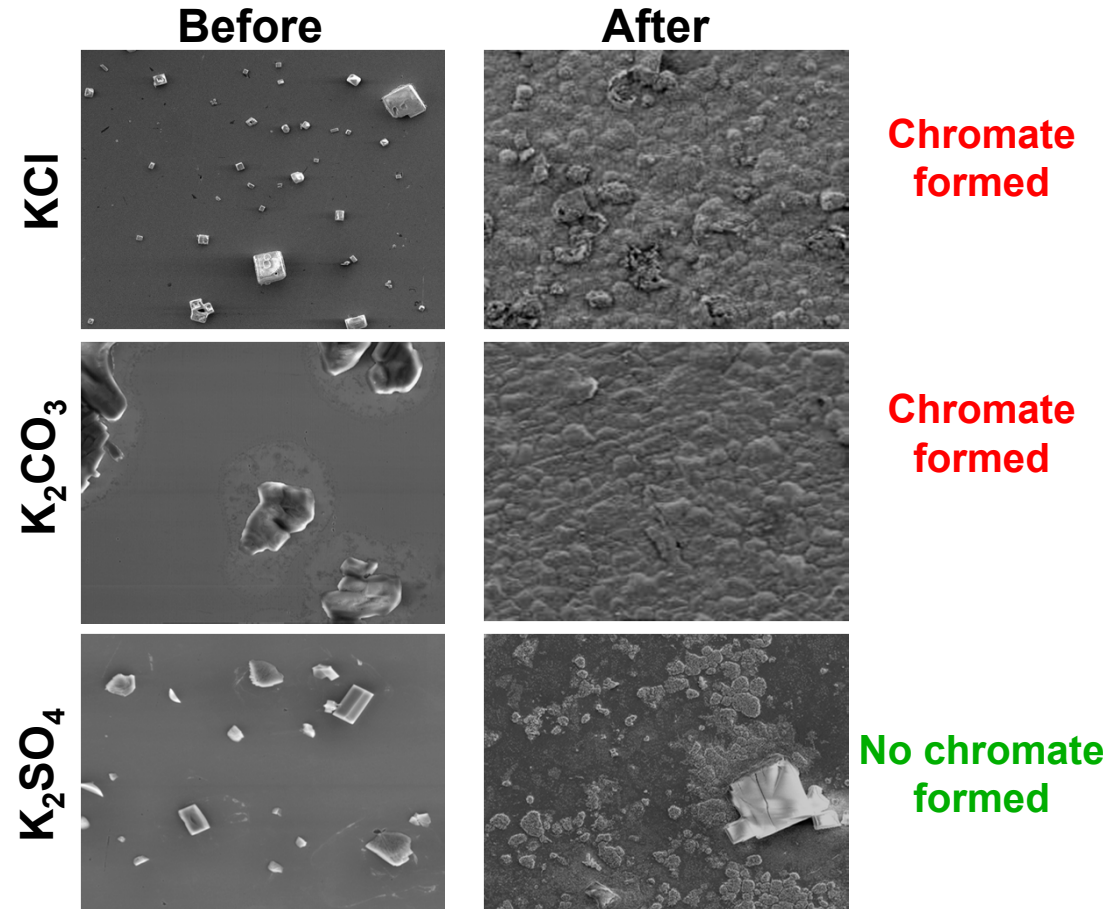
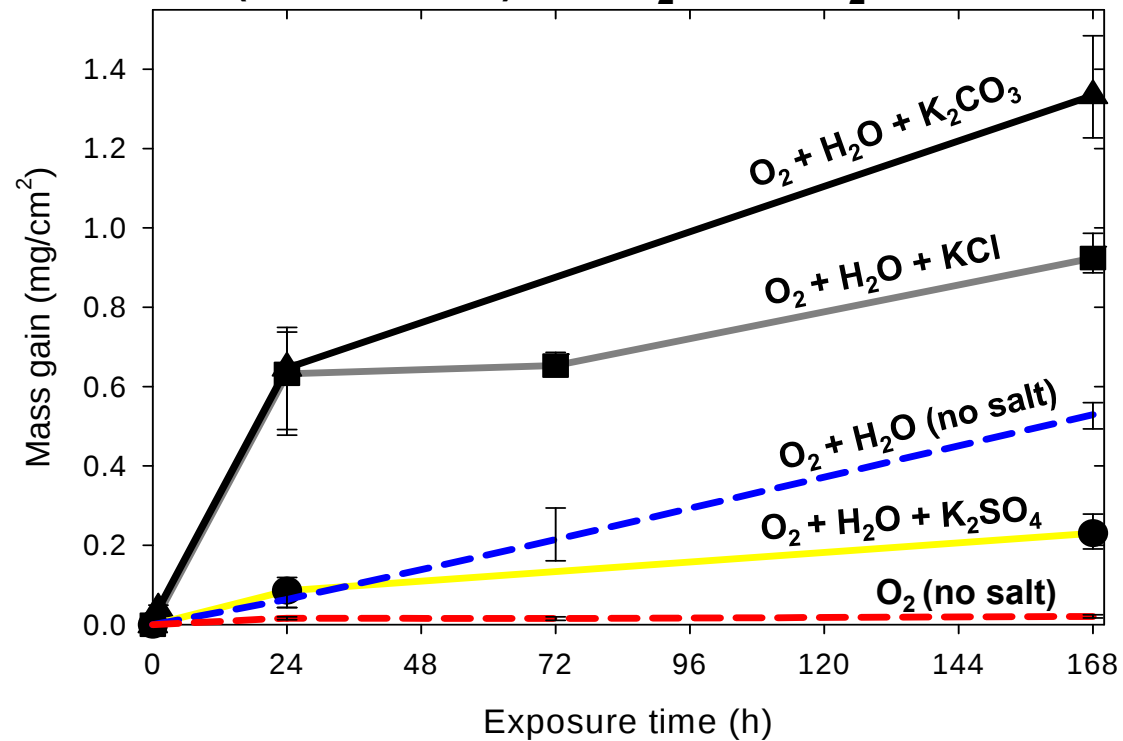
The effect of chromium depletion on chromia forming steels

304L (Fe20Cr10Ni), 5% O₂ + 40% H₂O, 600°C



The effect of chromium depletion on chromia forming steels

304L (Fe20Cr10Ni), 5% O₂ + 40% H₂O, 600°C



Super-
Heaters

SNCR

Dosage

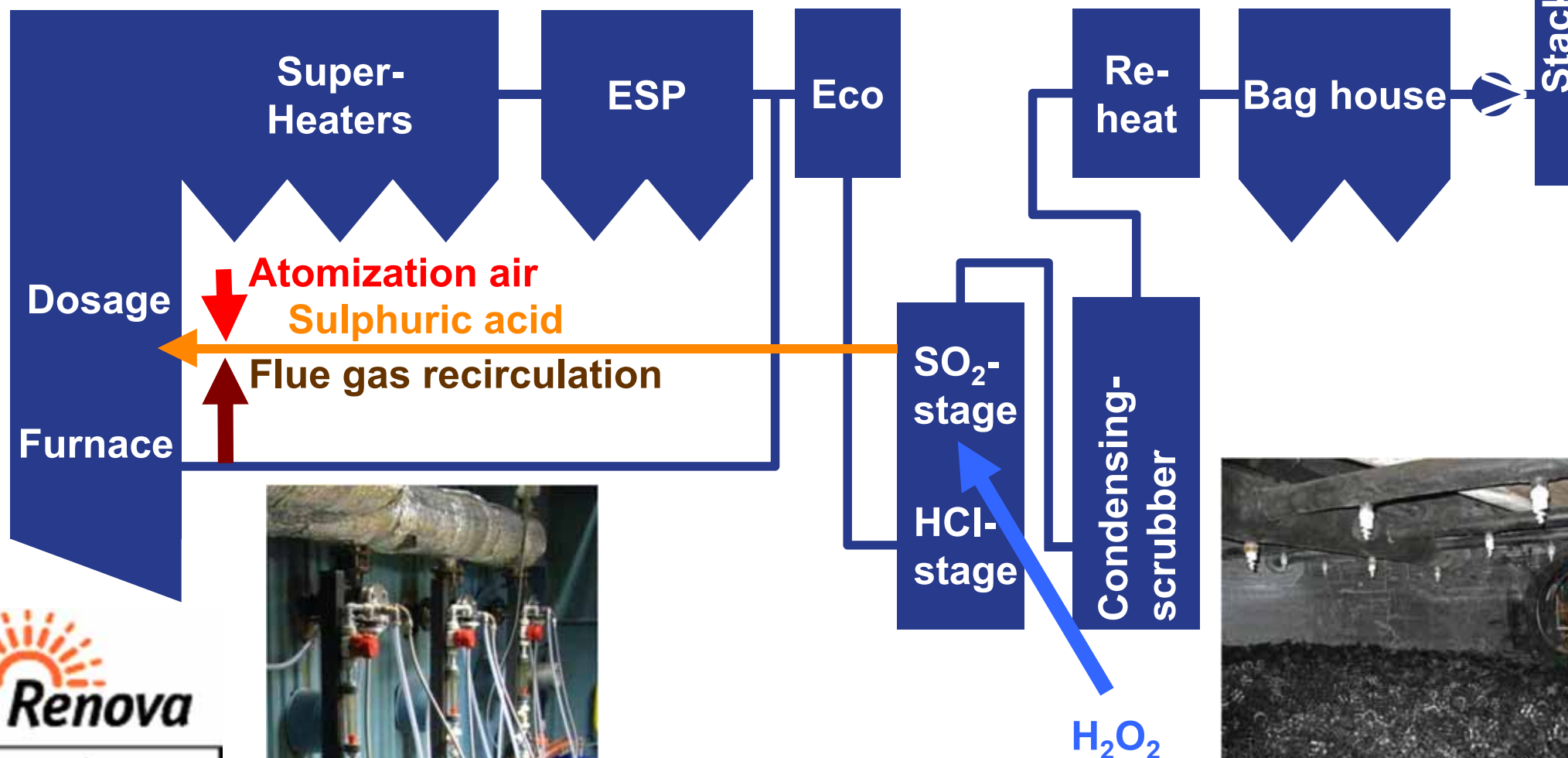
Oil burn.

Grate



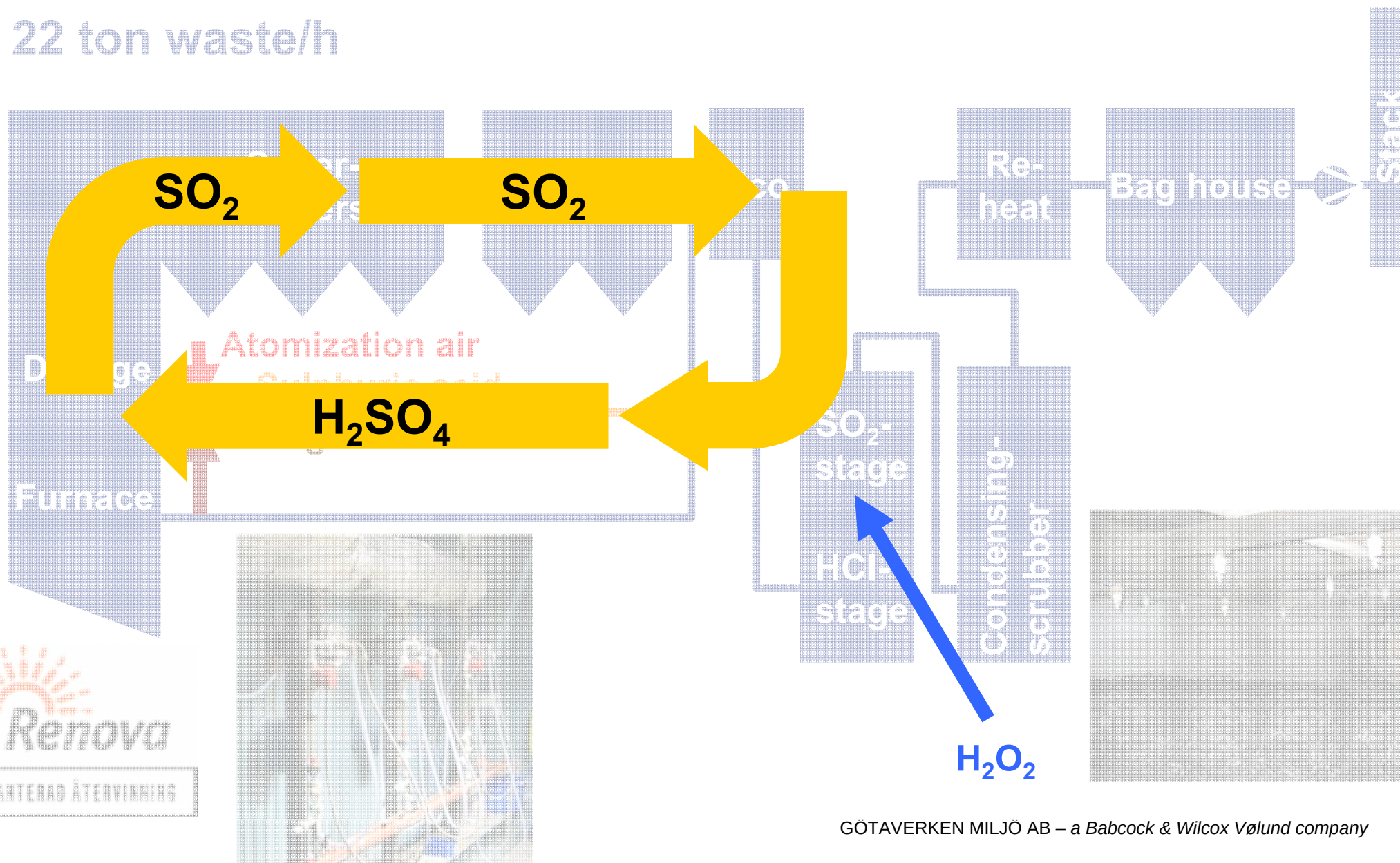
Full-scale tests at Renova P5 (Göteborg)

22 ton waste/h

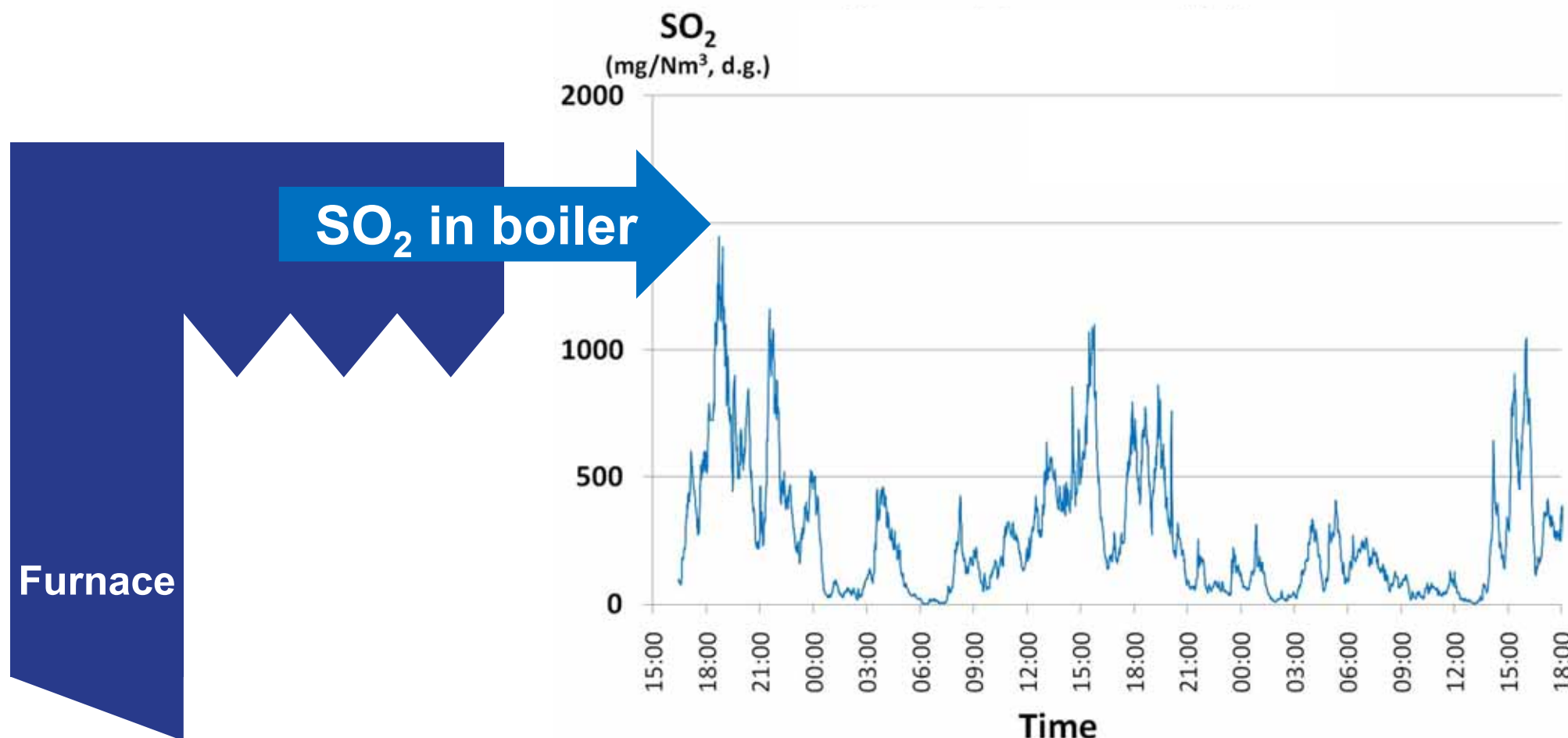


Full-scale tests at Renova P5 (Göteborg)

22 ton waste/h

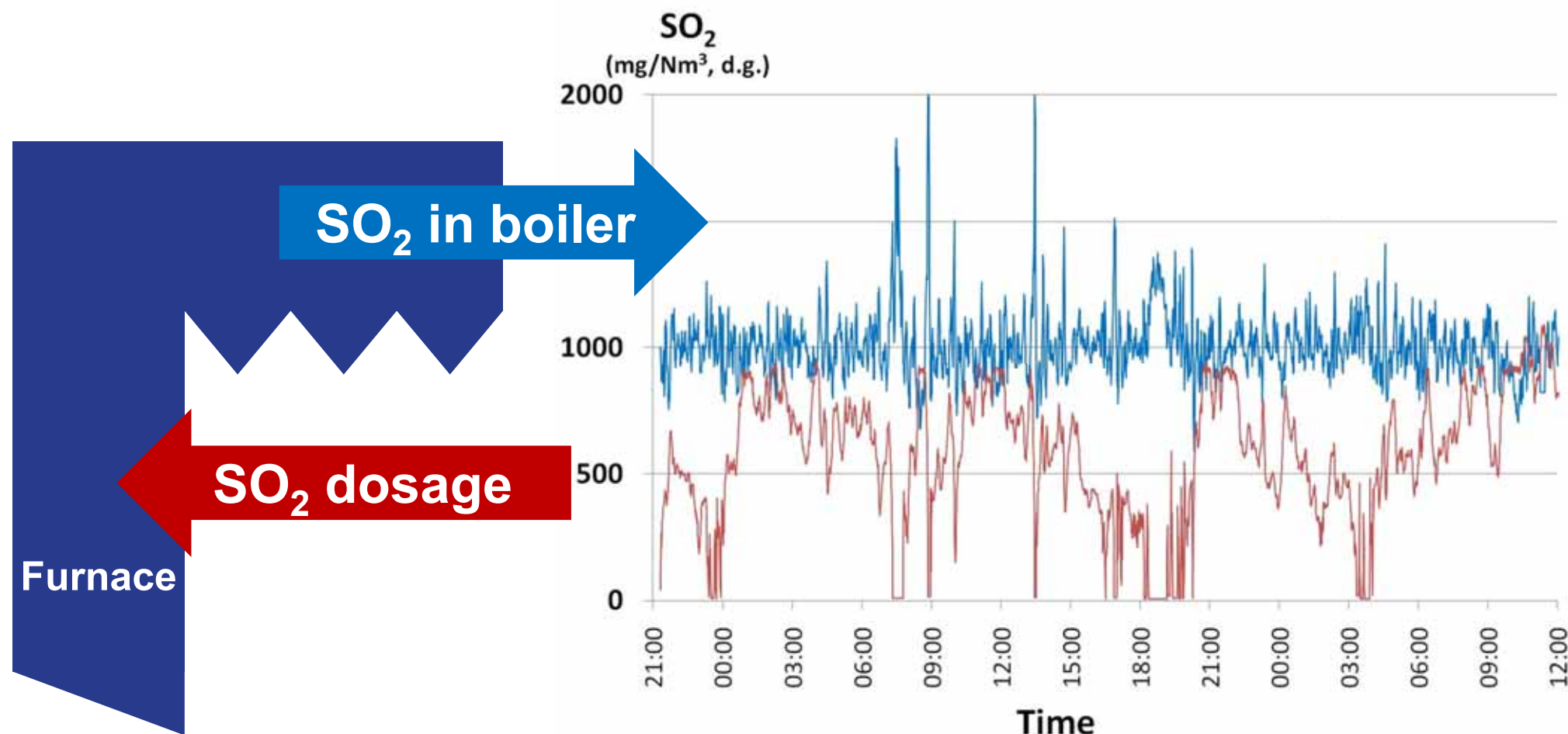


1000 h Reference (normal operation)



1000 h Reference: SO_2 in boiler = 270 mg/m³ (n,dg)

1000 h Recirculation: SO₂-setpoint



1000 h Reference: SO₂ in boiler = 270 mg/m³ (n,dg)

1000 h Recirculation: SO₂ in boiler = 720 mg/m³ (n,dg)

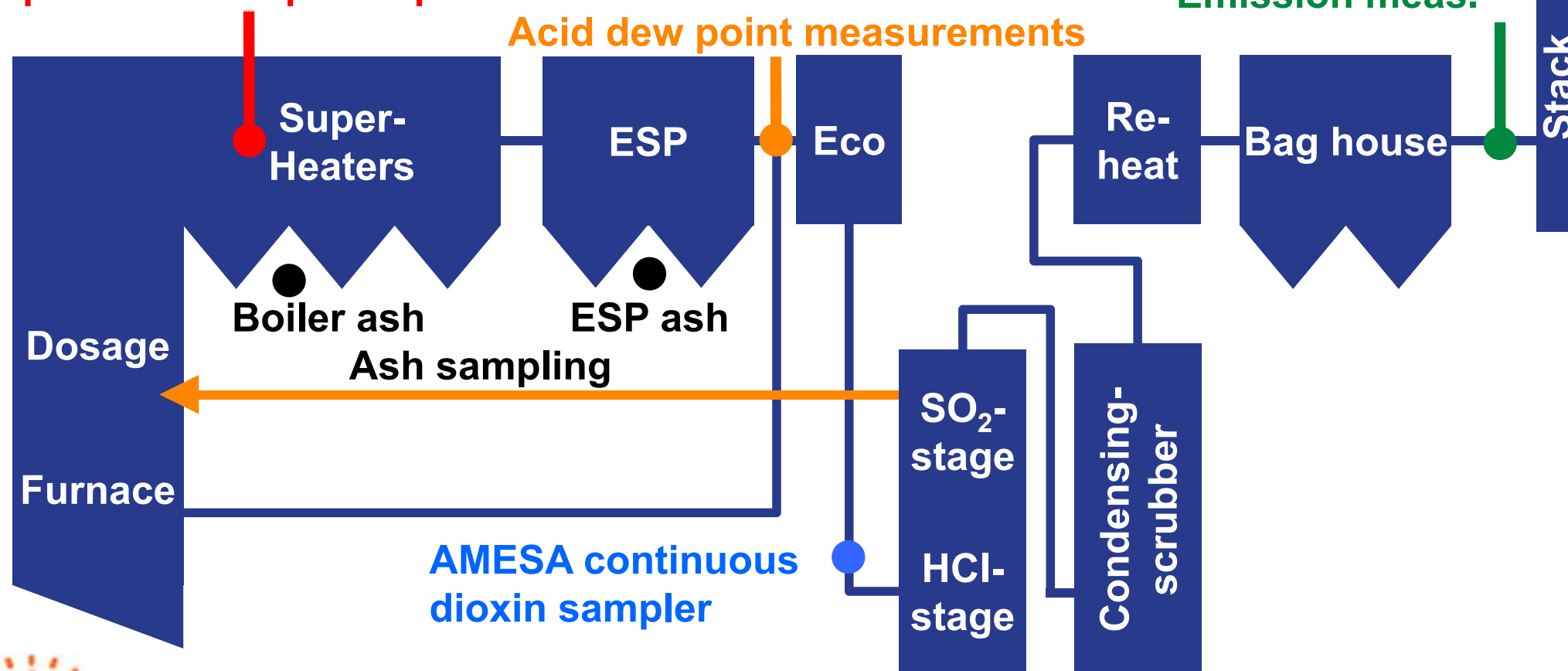
Sampling and measurements

High temp corrosion probe 24 h and 1000 h

Impactor and deposits probe

Acid dew point measurements

Emission meas.

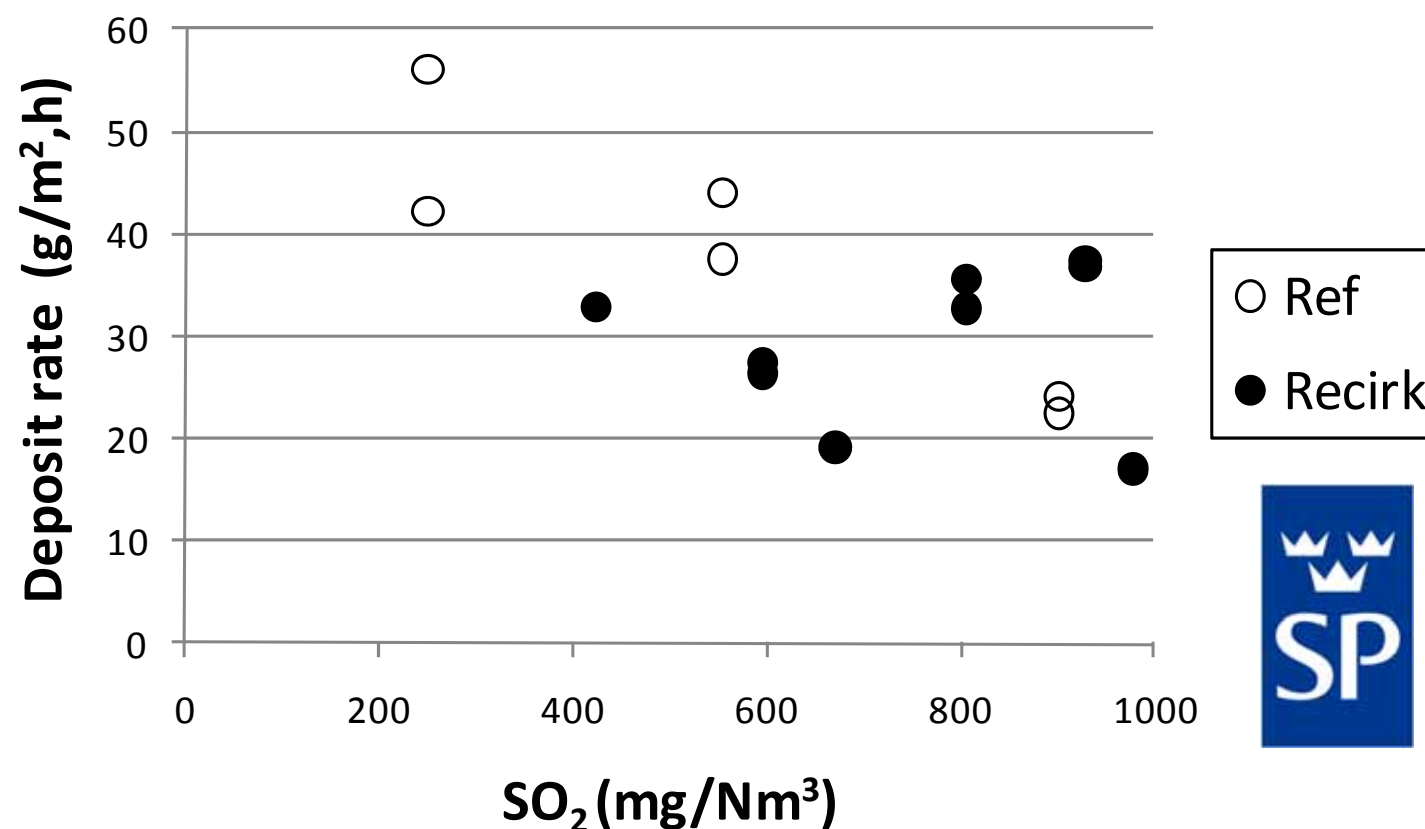
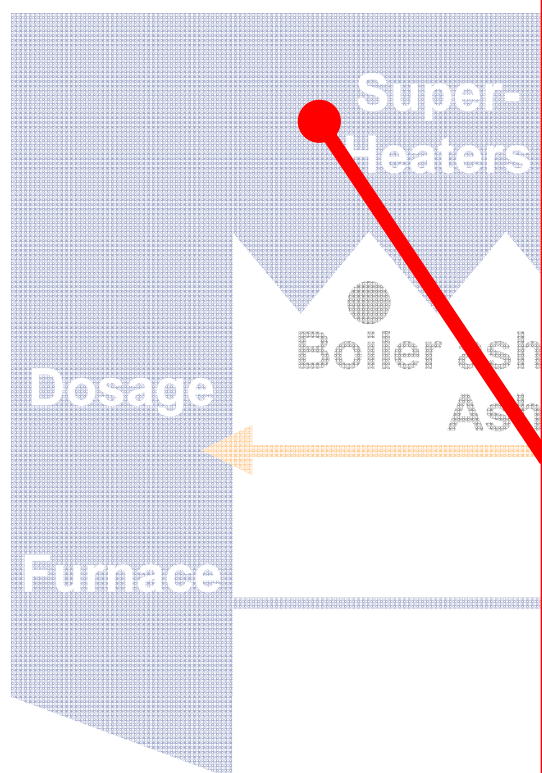


Deposit rate (g/m²,h) decreased with SO₂

High temp corrosion probe 24 h and 1000 h

Impactor and **deposits probe**

Emission meas.



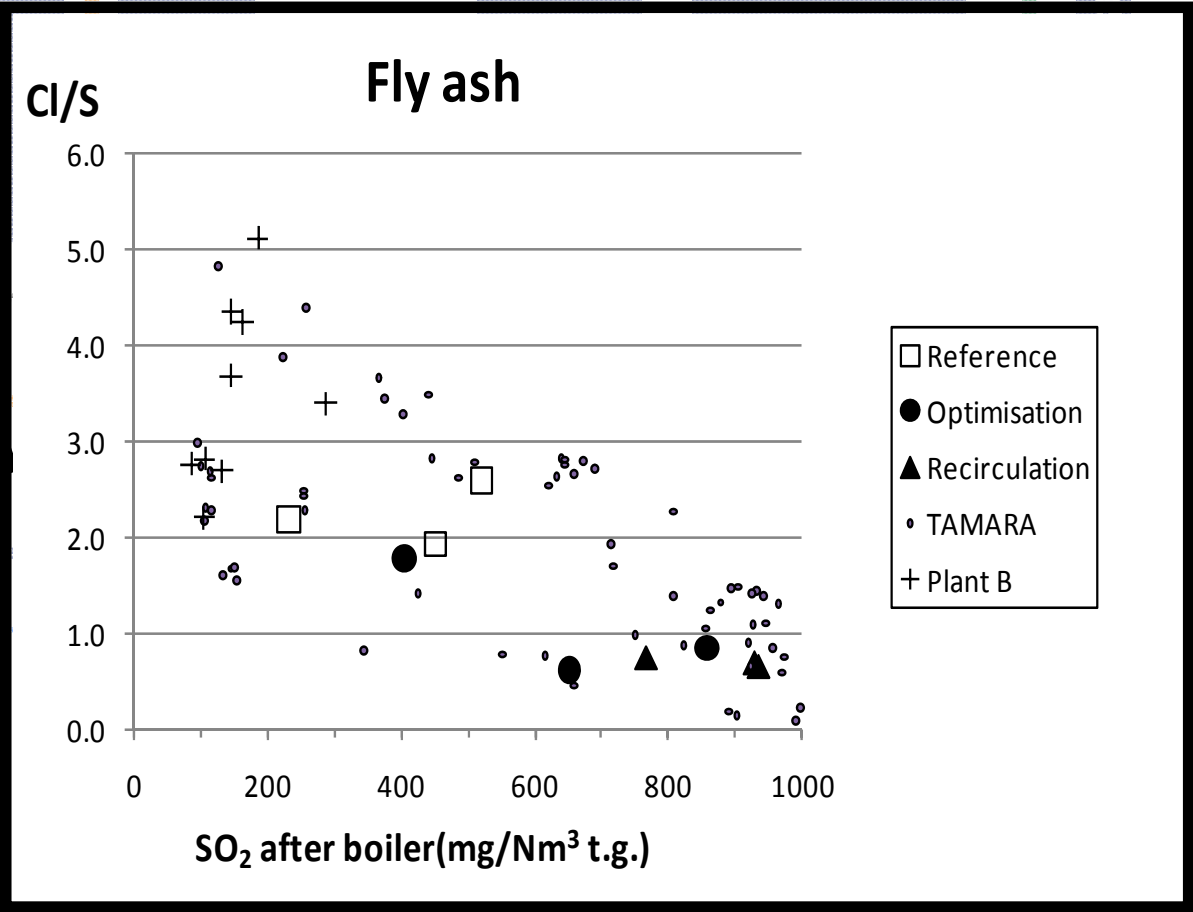
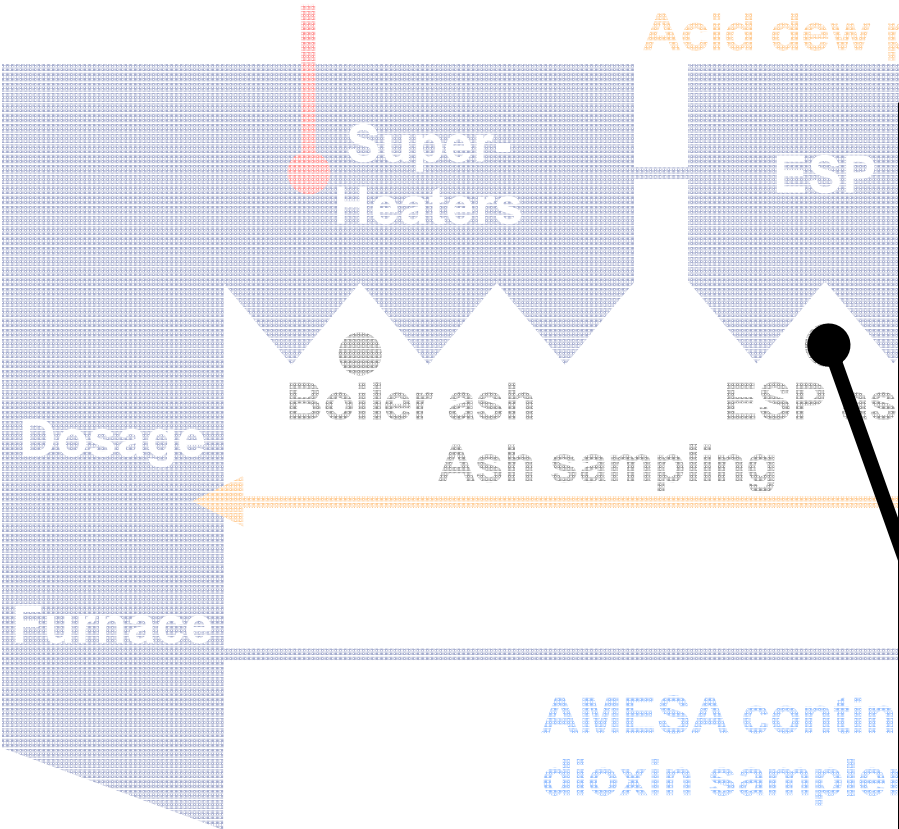


Fly ash Cl/S vs SO₂ from 3 different plants

High temp corrosion probe 24 h and 1000 h
Impactor and deposits probe

Acid dew point measurements

Emission meas.



Acid Dew point Temperature (ADT)



and 1000 h

dew point meas

ESP

Eco

SP ash

Stage

in

cor
m

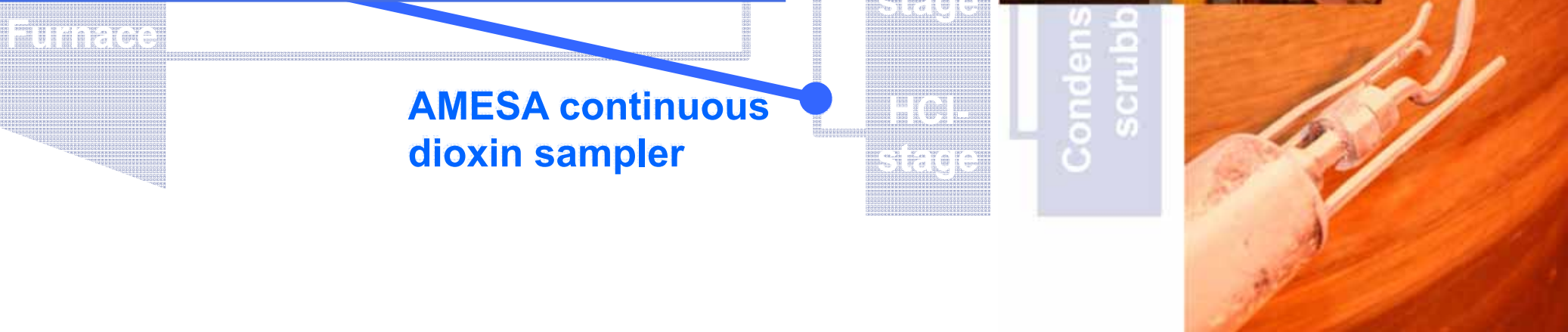
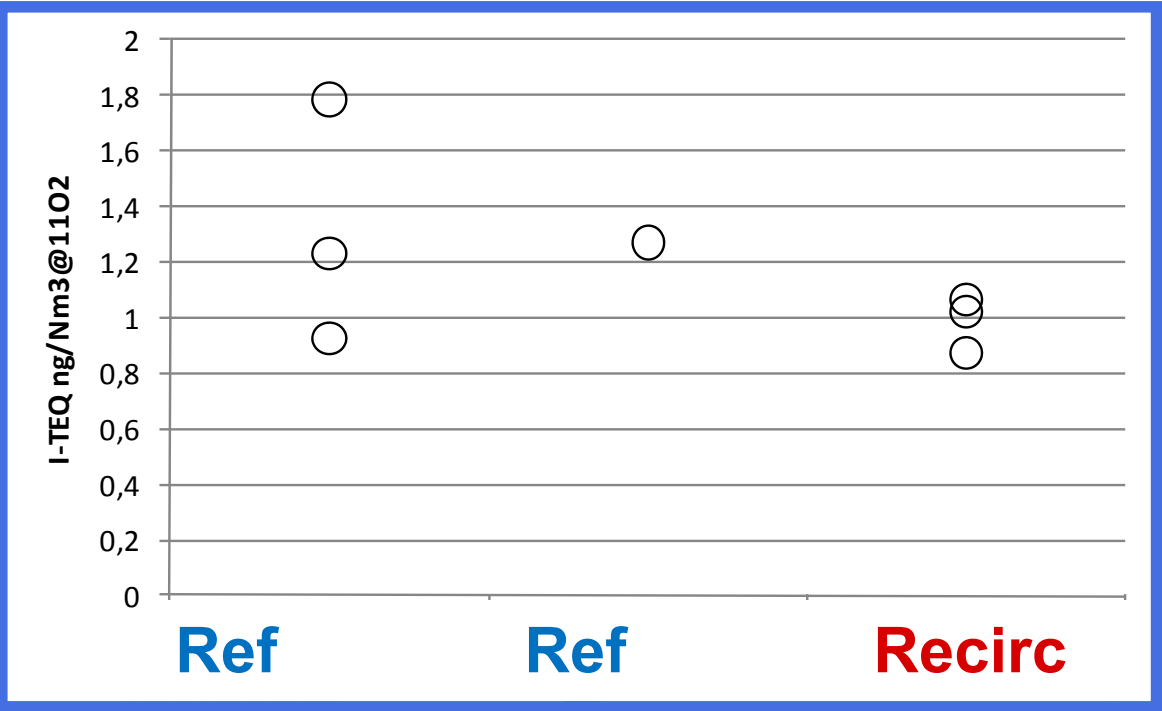


**Lancom 200
Acid Dewpoint Monitor**

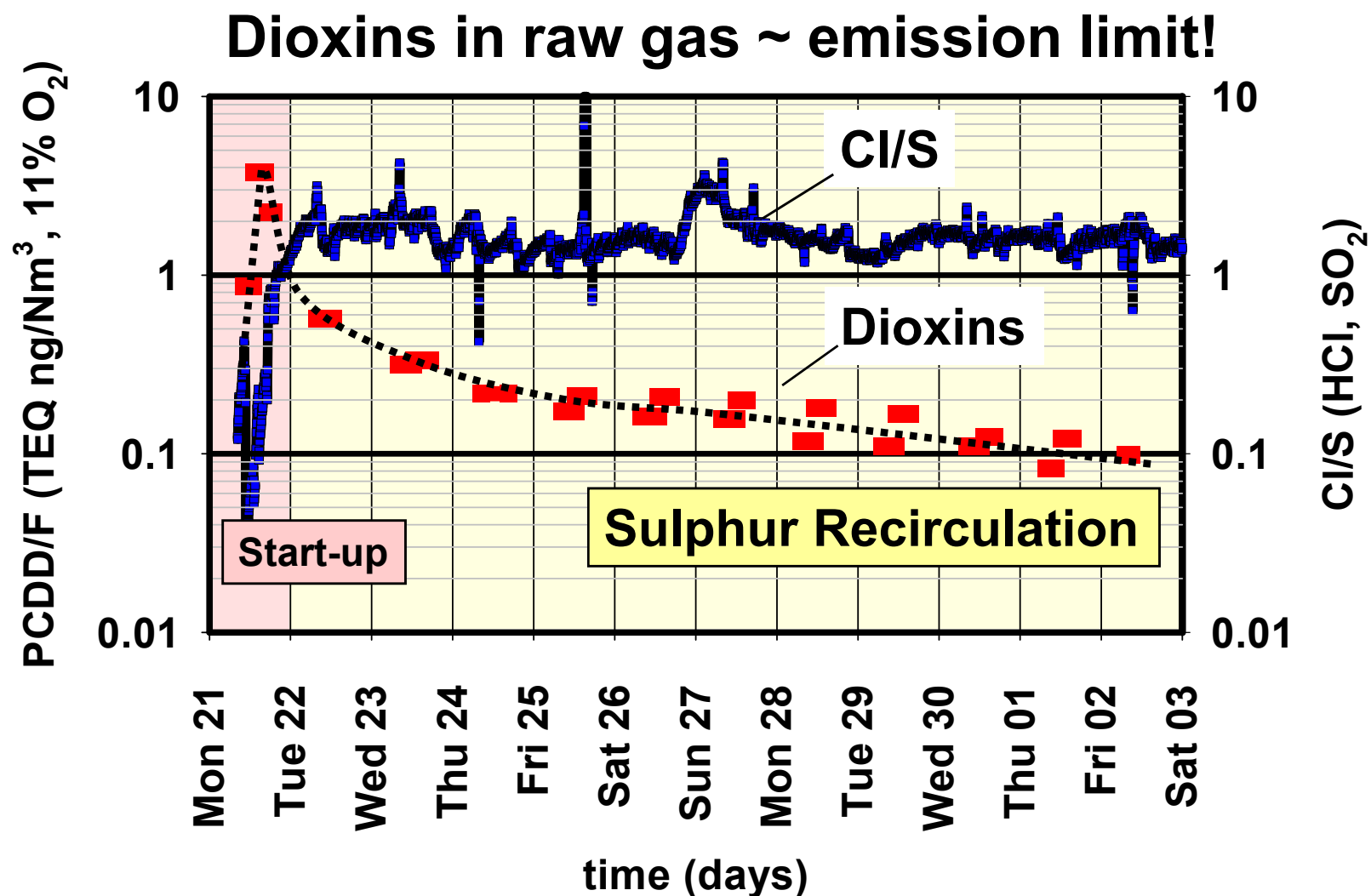
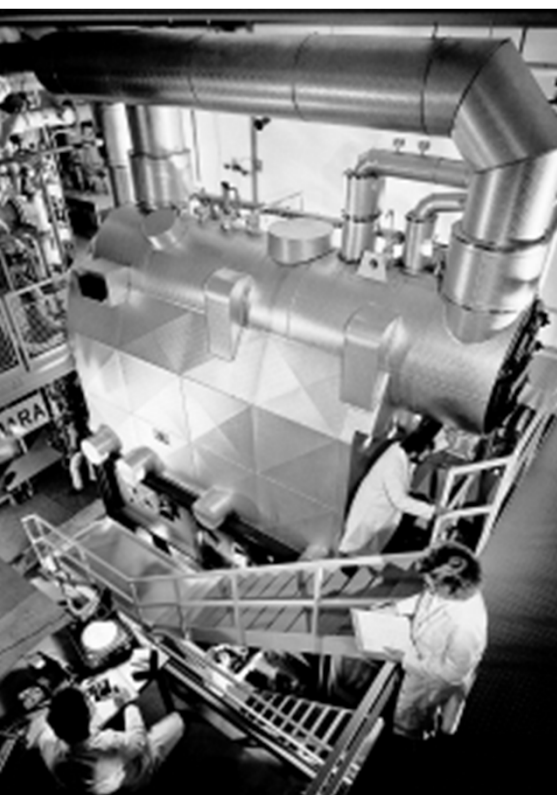
Result: No measurable ADT

Detection limit: 110-120°C

Dioxins in the flue gas: 1/4 less



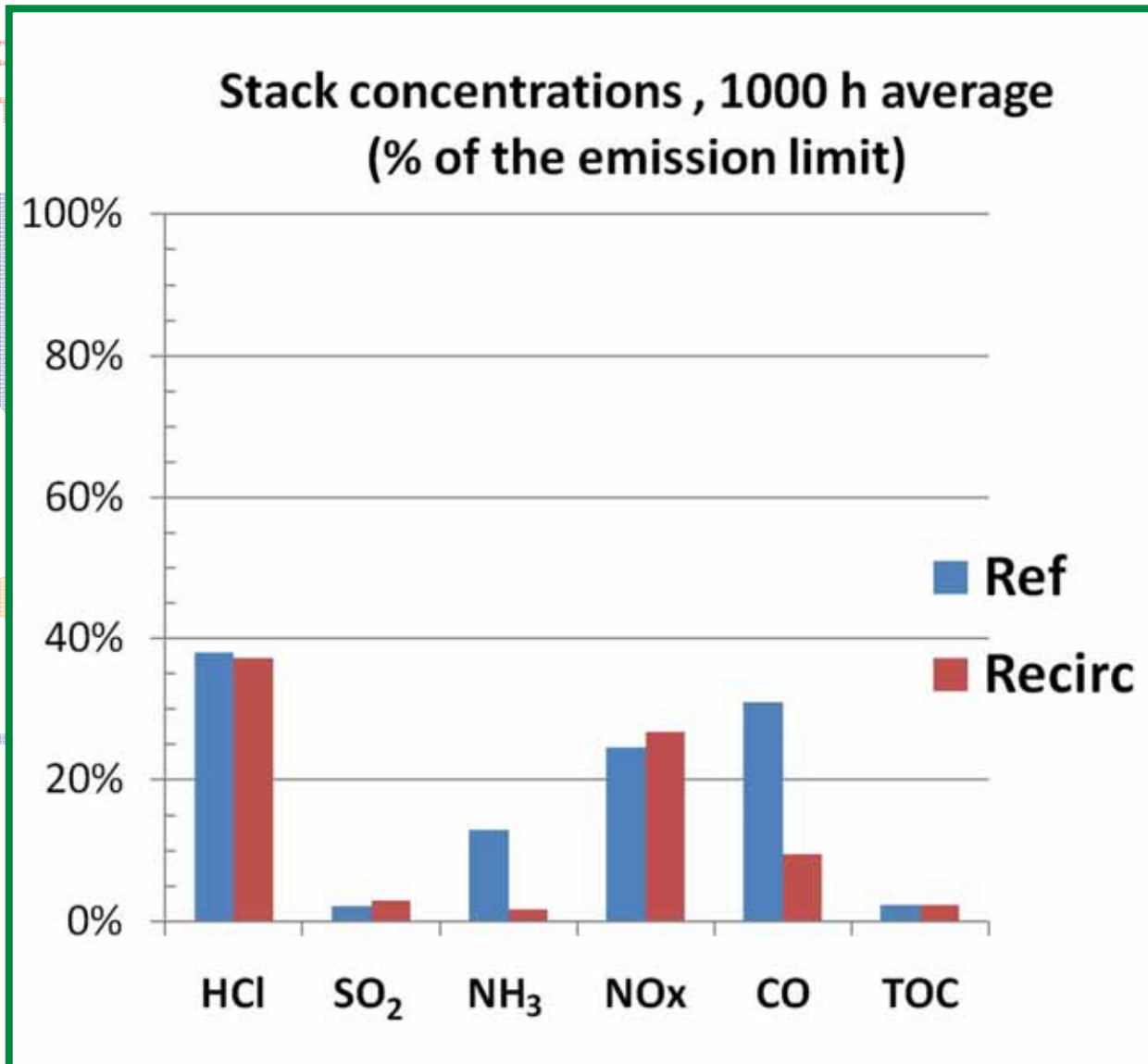
Pilot tests at KIT – Dioxin reduction



Stack values (% of Emission limit)

High temp c
Impactor an

Dosage
Furnace



Emission meas.

Bag house

Stack

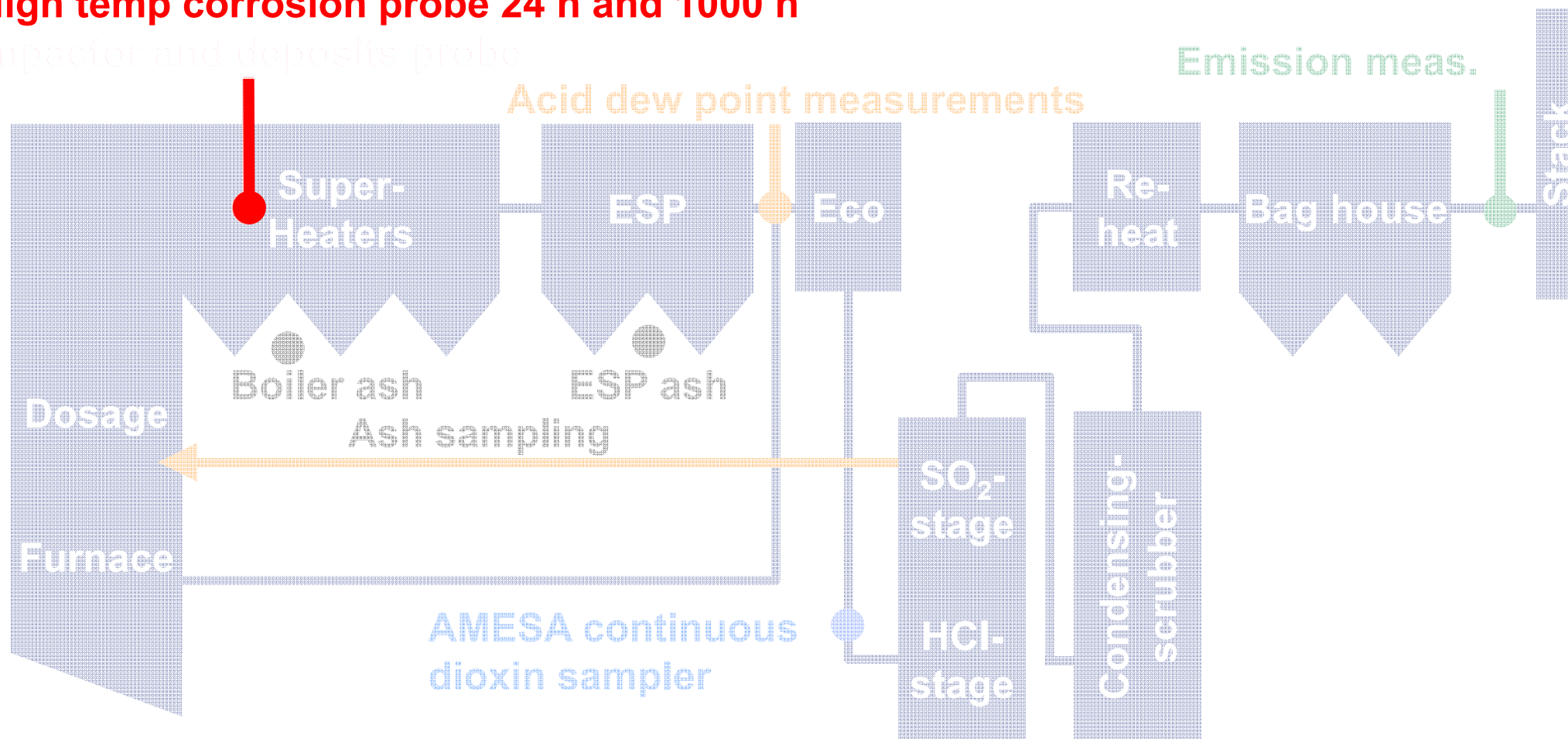
Corrosion probes in the superheater position

High temp corrosion probe 24 h and 1000 h

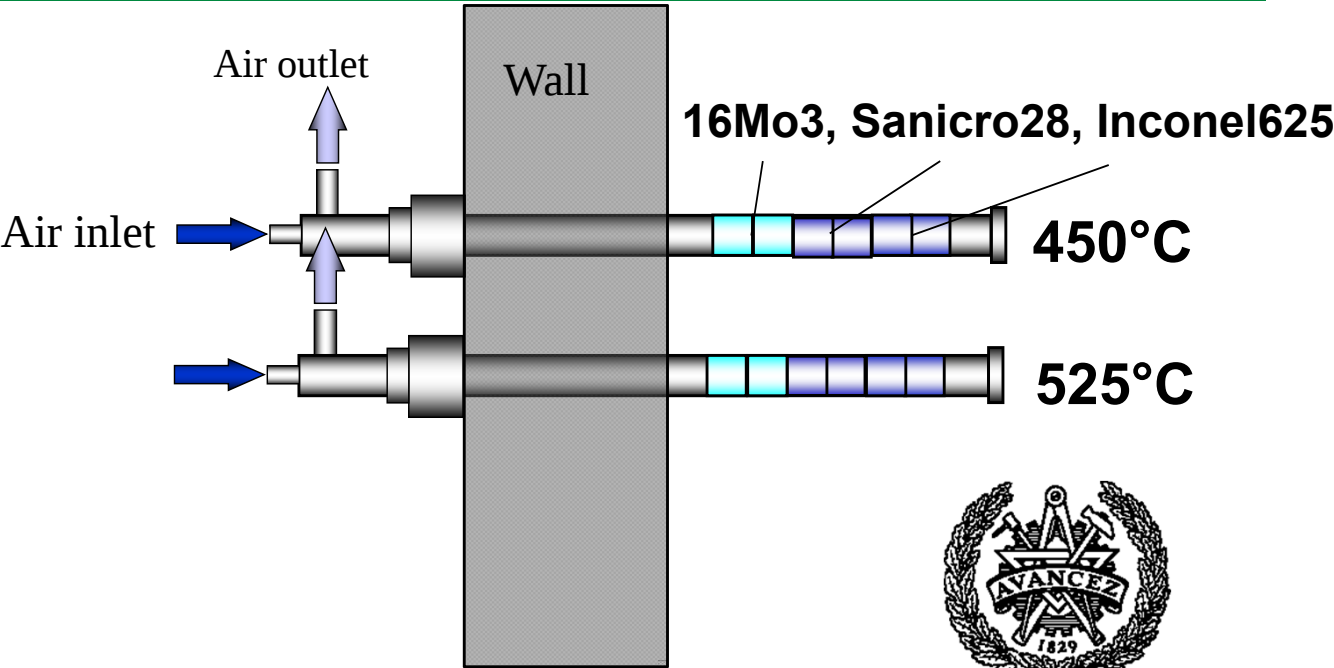
Impactor and deposits probe

Acid dew point measurements

Emission meas.



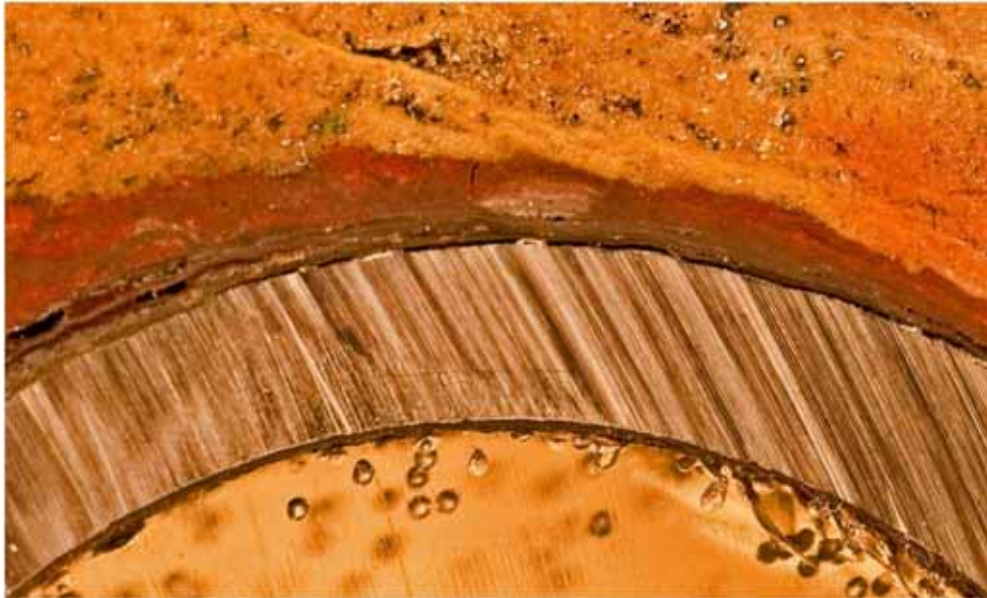
Corrosion probes in the superheater position



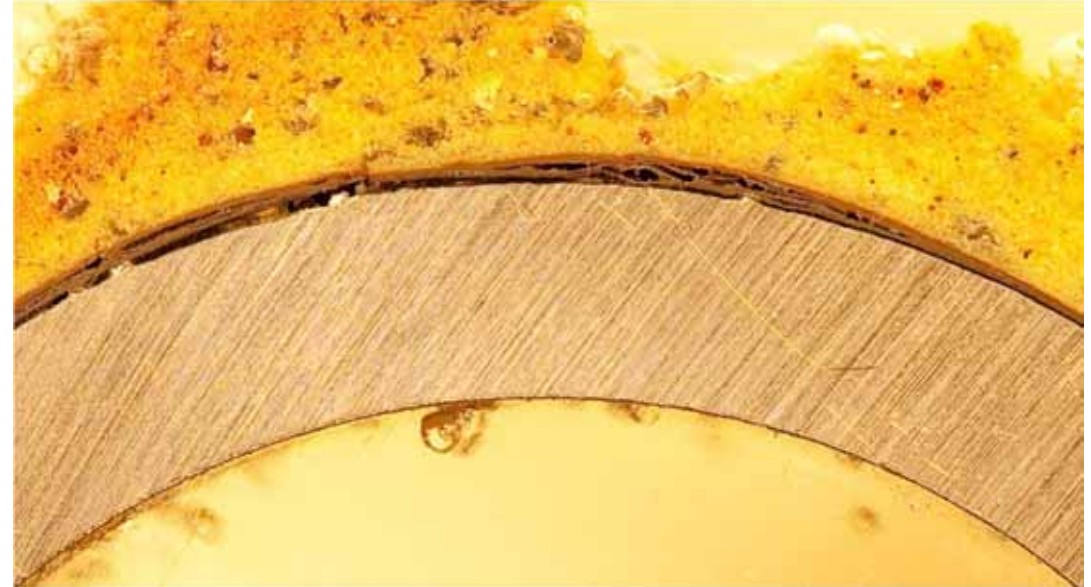
CHALMERS

(wt%)	Cr	Ni	Mn	Si	Mo	Fe	n _{Cr} /n _{Fe}	Add. elements
16Mo3	-	-	0.6	-	0.3	99.1	0	-
Sanicro 28	27.0	31.0	2.0	0.6	3.5	34.5	0.8	Cu: 1
Inconel 625	22.0	58.0	0.5	0.5	9.0	5.0	4.4	-

16Mo3 - Photograph - 525 °C

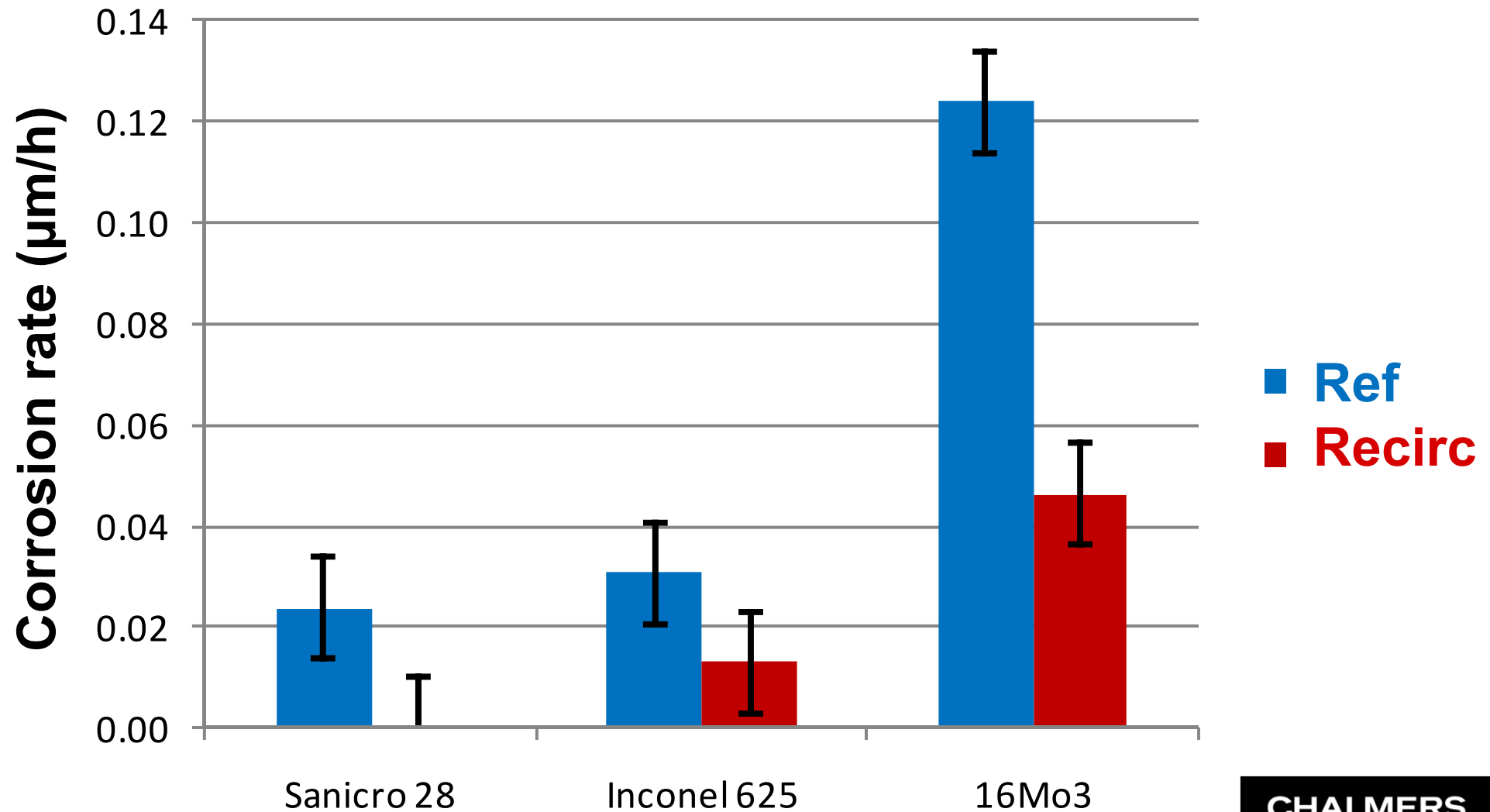


**Reference
16Mo3**

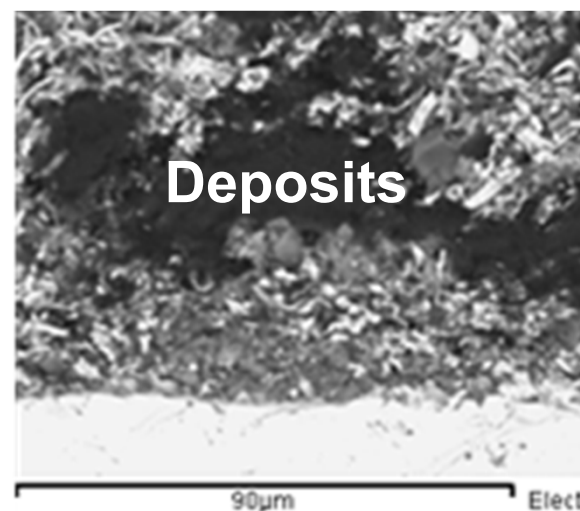
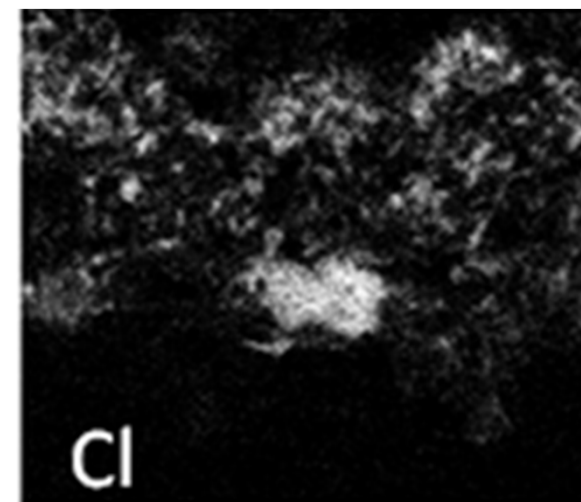
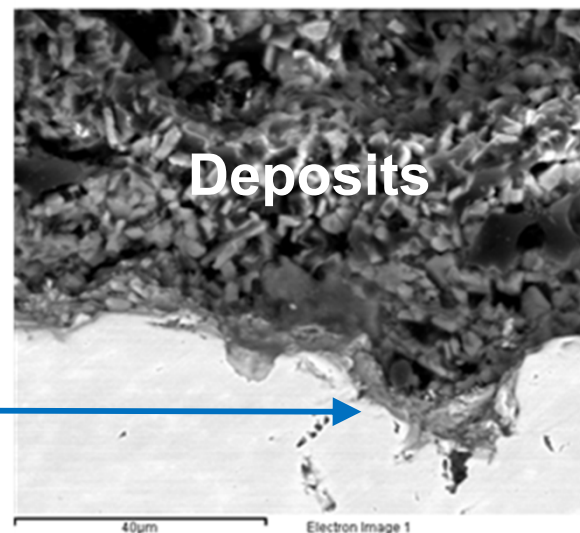


**Sulphur Recirculation
16Mo3**

Corrosion rate at material temp 450°C (1000 h)

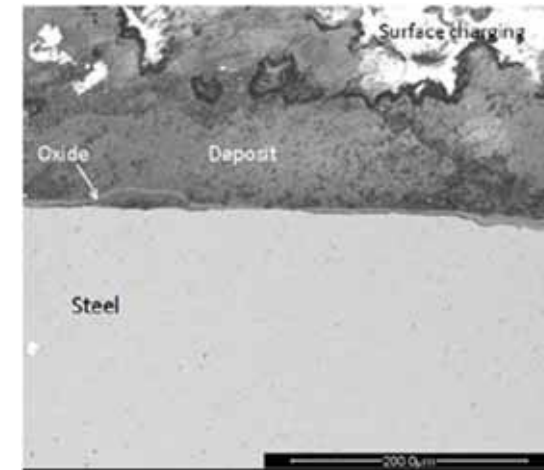
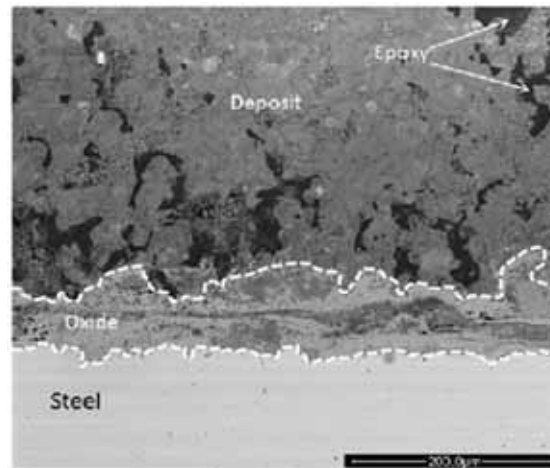


Inconel 625 - SEM/EDX images - 450°C

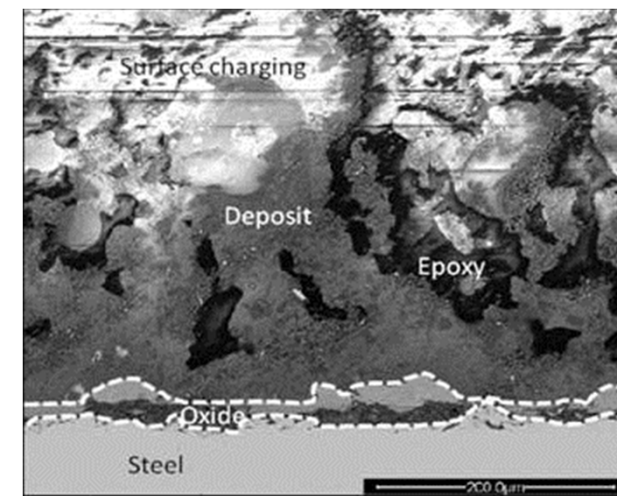
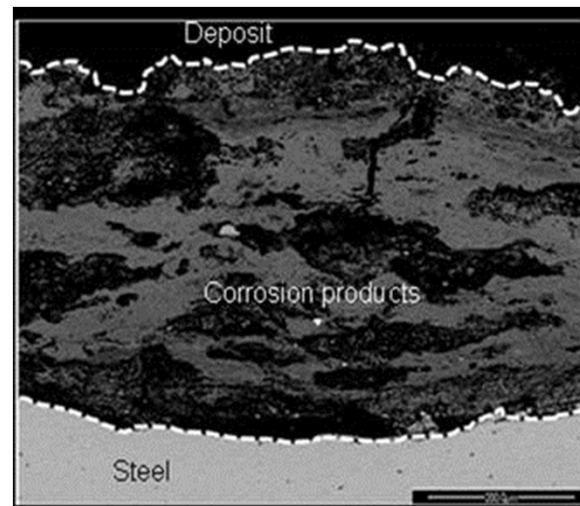
SEM**EDX map for chlorine**

Sanicro 28 - 1000h

450°C



525°C

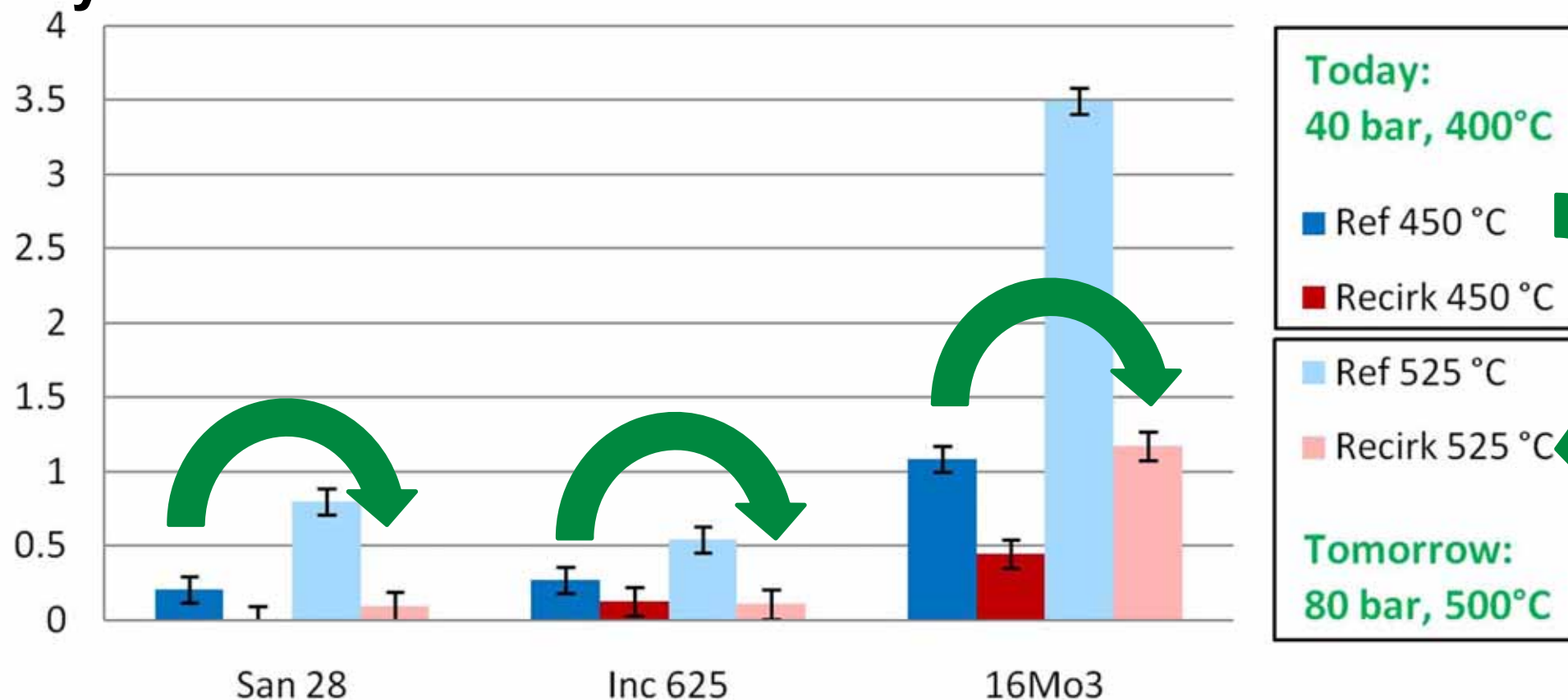


1000 h Reference

1000 h Recirculation

1000 h Corrosion rate measurements

mm/year



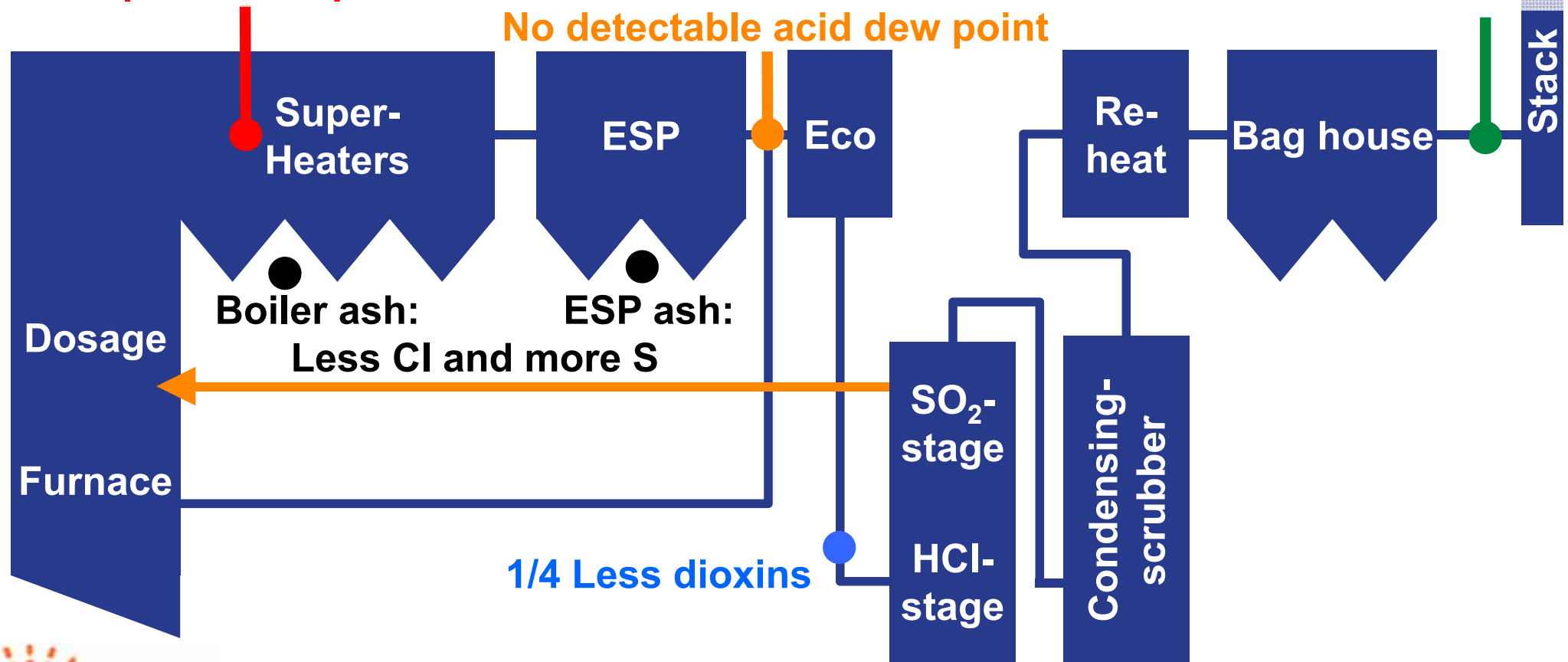
**Sulphur recirculation enables
higher steam data**

CHALMERS

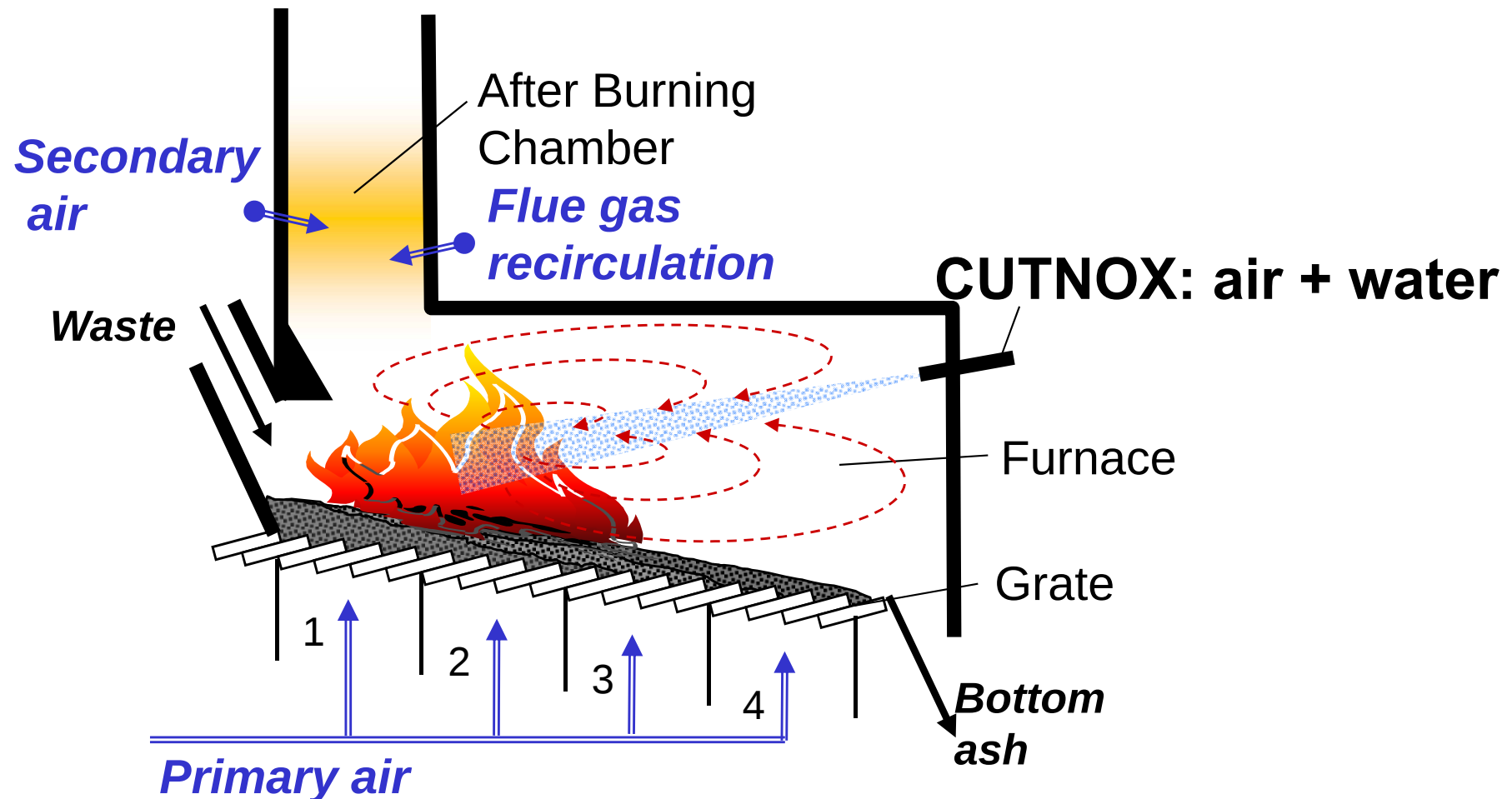
Summary

Lower high temp corrosion at 450 and 525 °C material temp
Less deposits and particles

Emissions unchanged
(lower CO and NH₃)

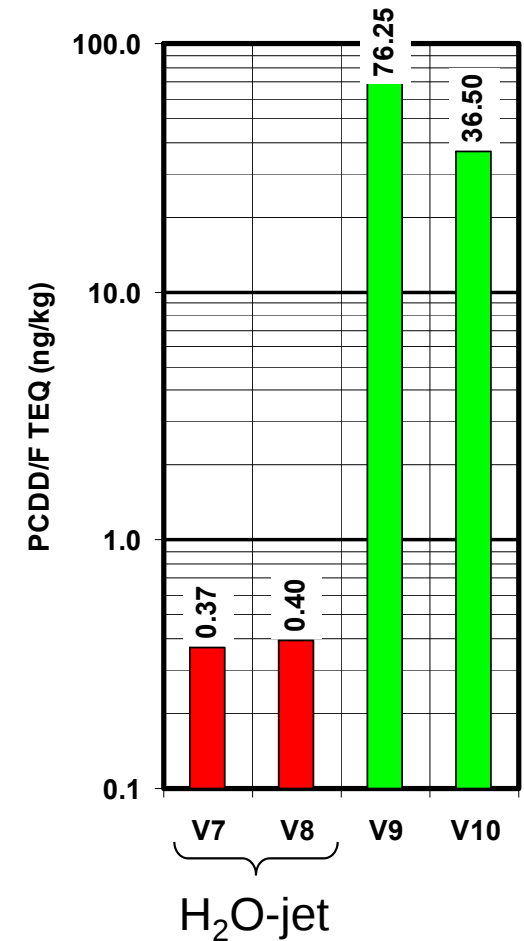
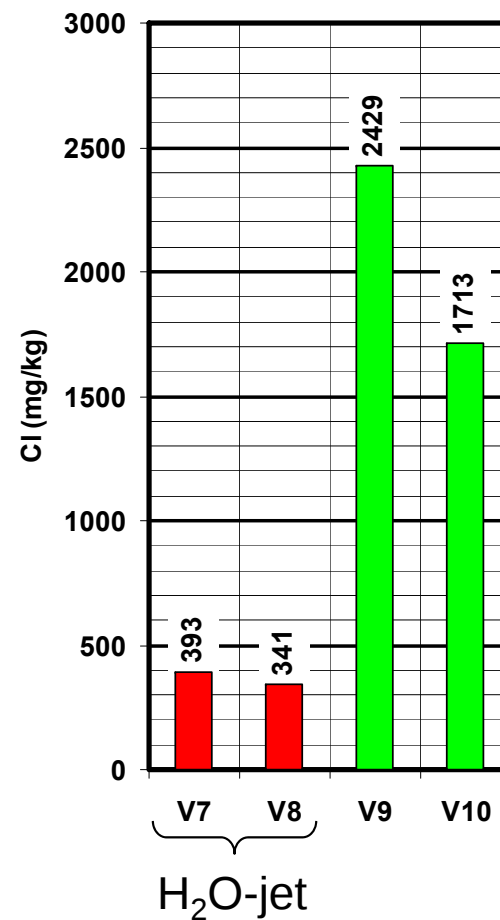
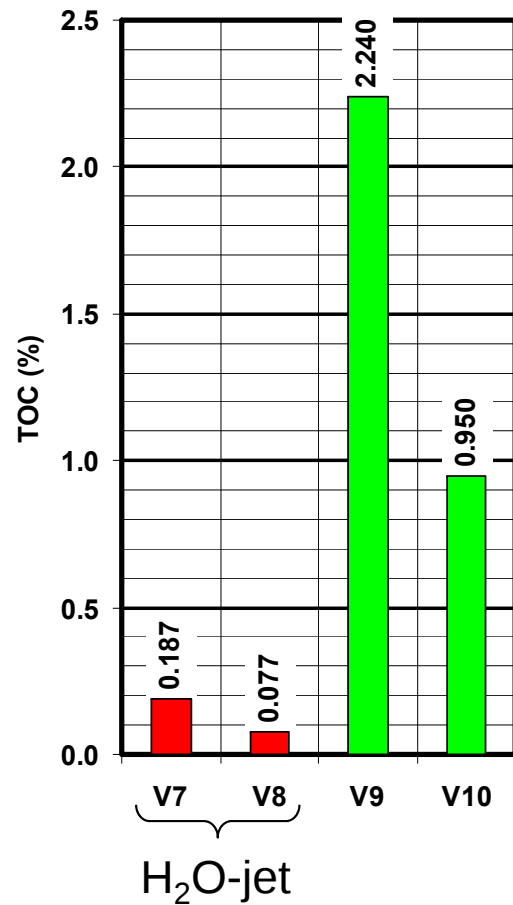


NO_x primary measure: CUTNOX



**Lower temp. and increased mixing at $\lambda < 1$
promote formation of N₂ and reduce formation of NO**

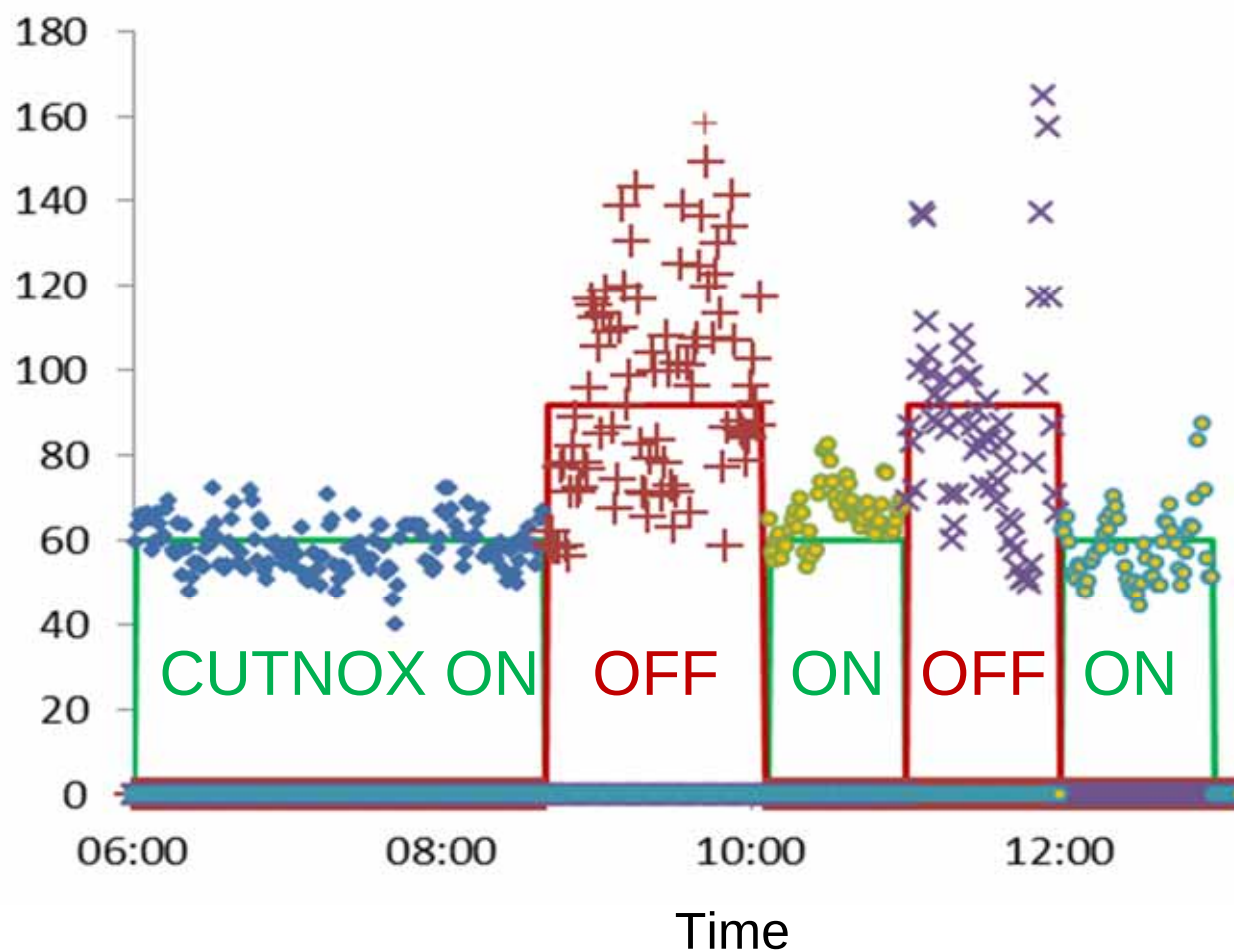
Test at TAMARA: Pilot grate fired furnace (0,5 MW_{th})



NO_x: First commercial CUTNOX at Renova (SE)

Preliminary results from CUTNOX ON/OFF tests:
Optimisation in progress

NO_x mg/Nm³ (dg, 11% O₂)



OFF = 92
(mg/Nm³ d.g.)

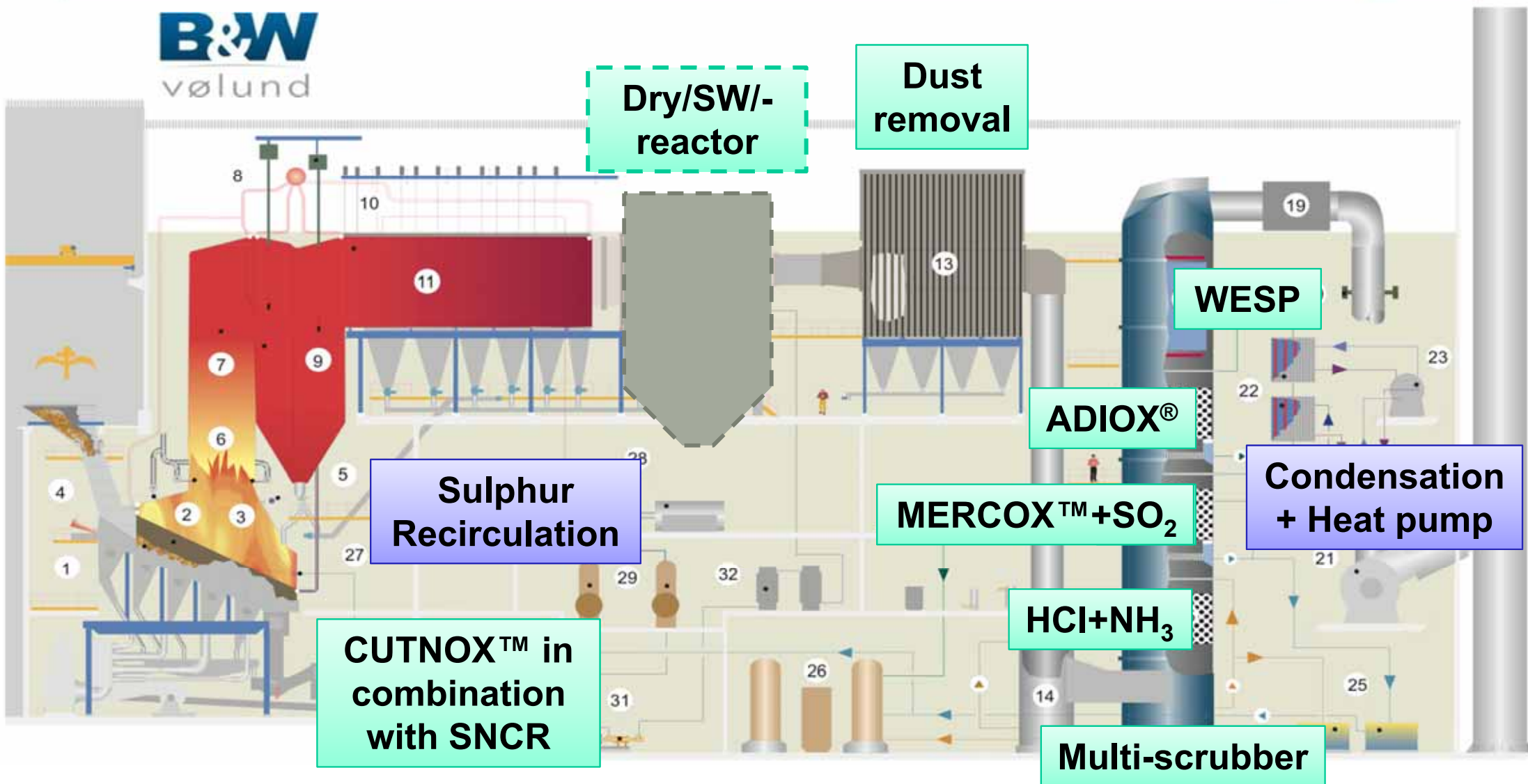
ON = 60
(mg/Nm³ d.g.)

Corresponding to
34% NO_x reduction



NextBAT® flue gas treatment

B&W
vølund

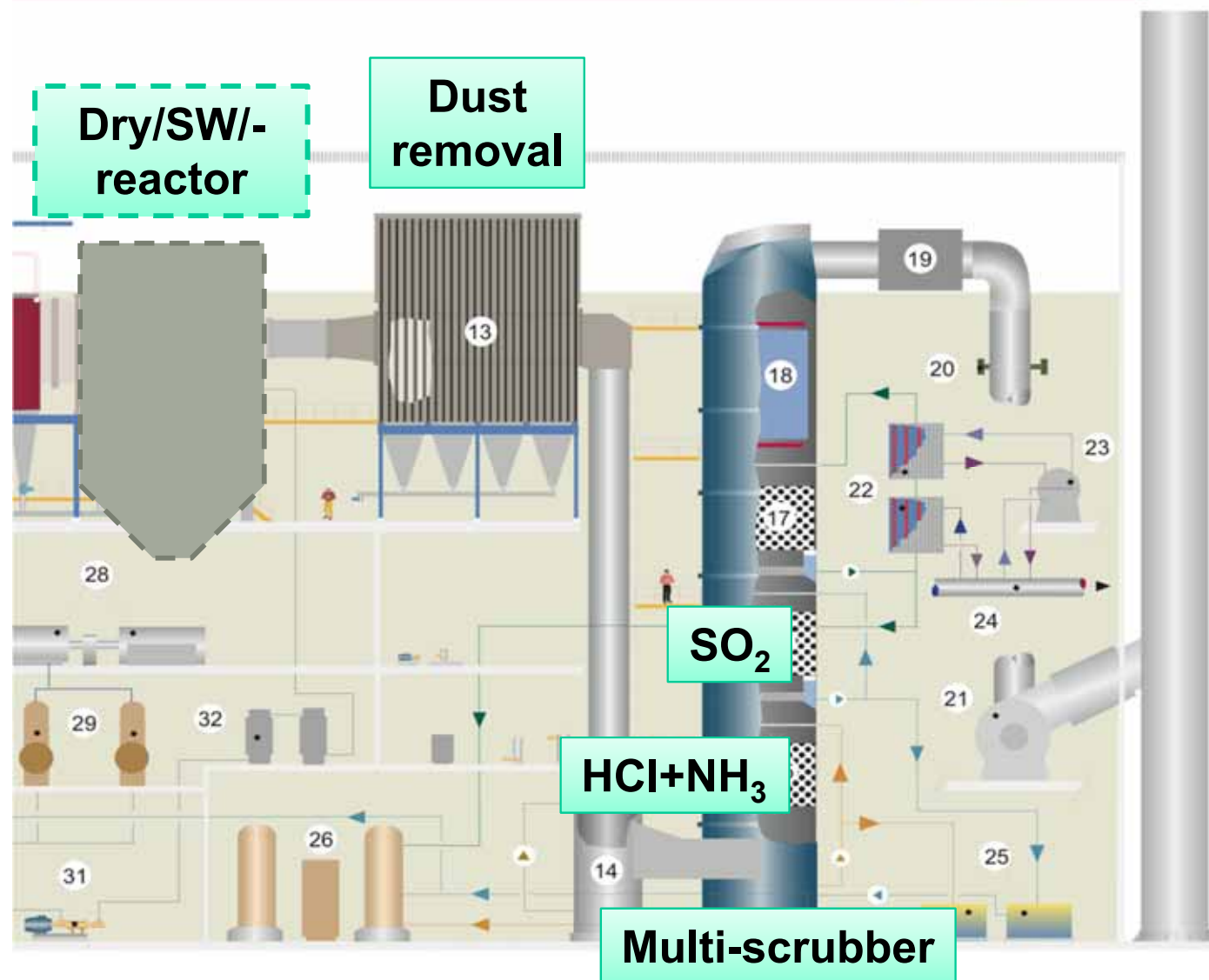


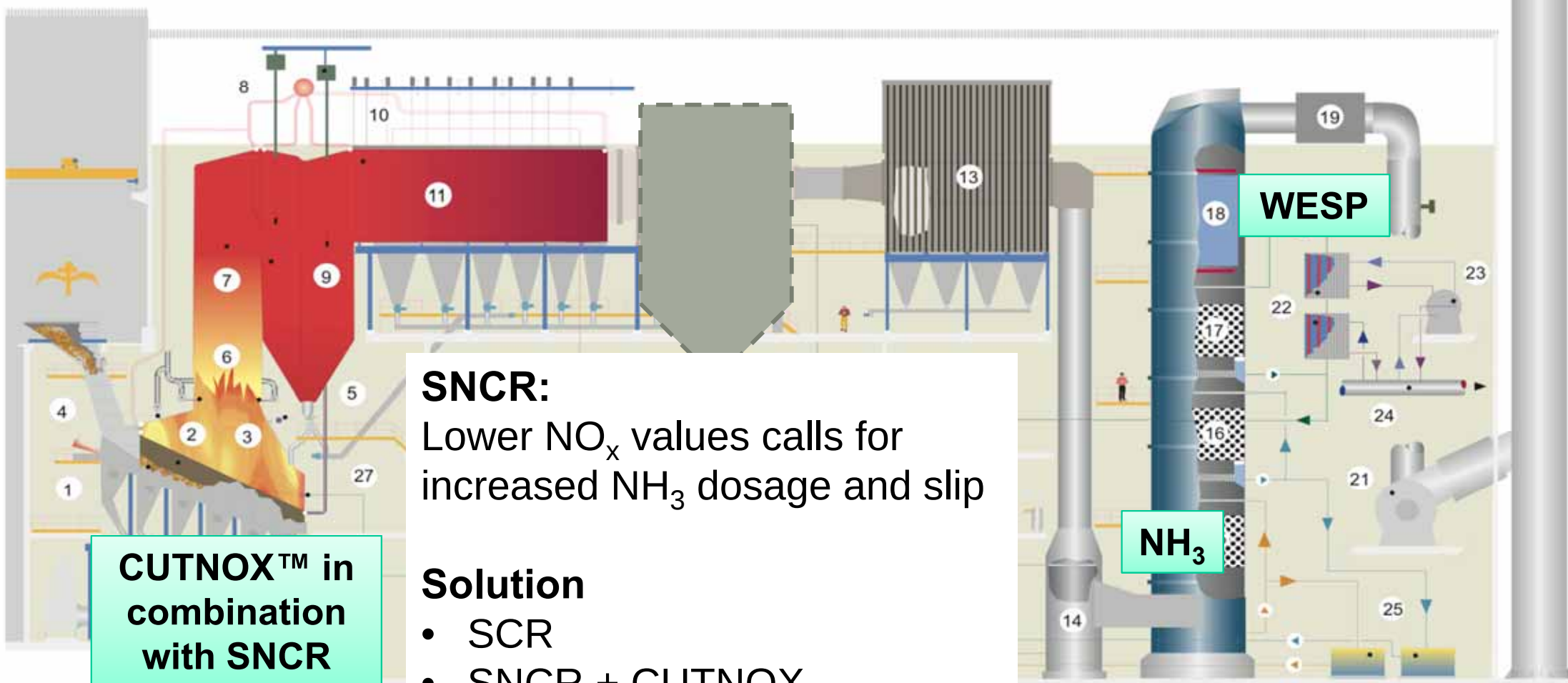
HCl+SO₂ removal

Wet scrubbers yield extremely low emission values: Insensitive to HCl/SO₂ ratio

Waste water free:
Dry or semi-wet
+ slip scrubber

**Cl⁻ + SO₄²⁻
to water recipient:**
Wet scrubber





Dust / fine particles

Problem

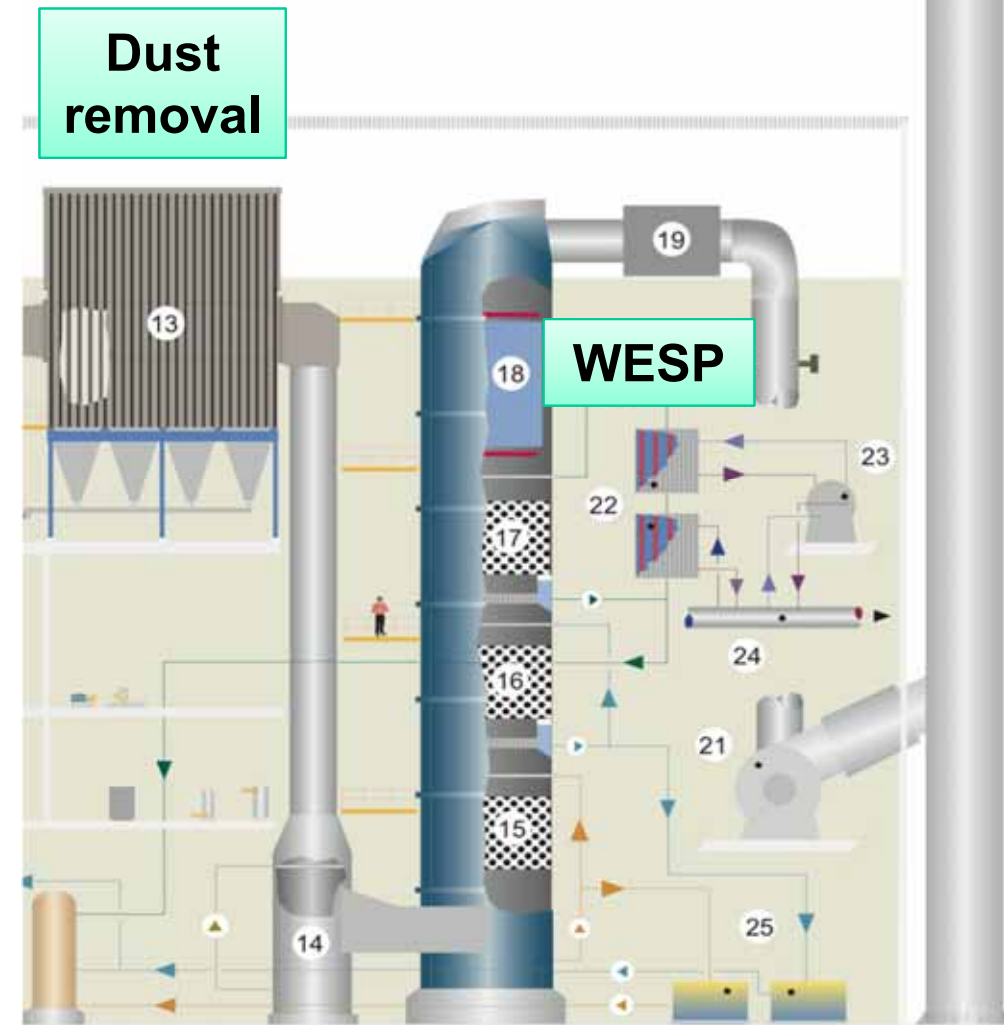
PM_{2.5} in ambient air causes premature death of 350 000 EU citizens per year.

In many urban environments, the ambient air levels of PM_{2.5} are higher than stipulated by EU directives.

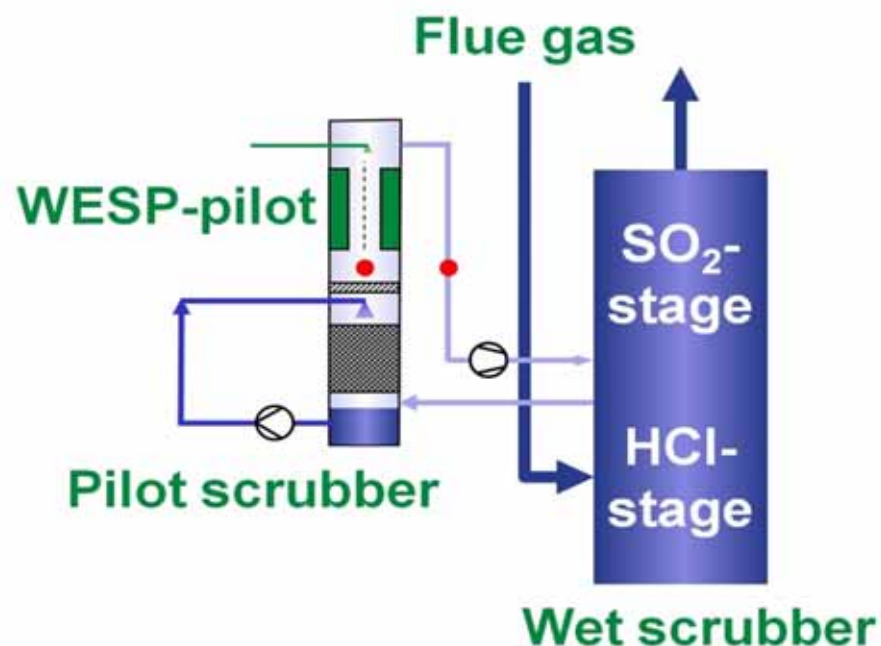
Solution

Dust concentrations $< 1 \text{ mg/Nm}^3$ (10% of emission limit) can be reached by:

- Bag house filter
- ESP + scrubber integrated WESP



Dust: Scrubber Integrated WESP

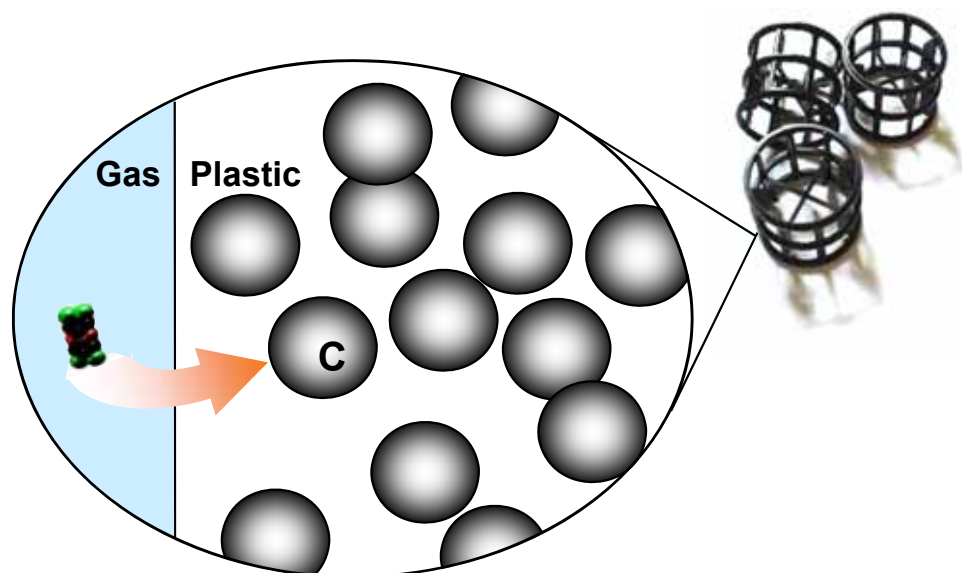


- New scrubber integrated WESP (Wet Electro Static Precipitator) developed by Götaverken Miljö and AWS Corp (IT).
- Fabricated in corrosion resistant conductive FRP
- Cooled condensing collector

- All clean gas dust measurements **<0,3 mg/Nm³ dg.**
- **Mean removal efficiency >99%**

PCDD/F removal

- **Bag house filter + carbon injection + ADIOX** for Memory Effect minimisation
- **ESP + ADIOX**
ADIOX can be incinerated after use – thereby taking dioxins out of the eco-cycle



PCDD/F removal: ADIOX®

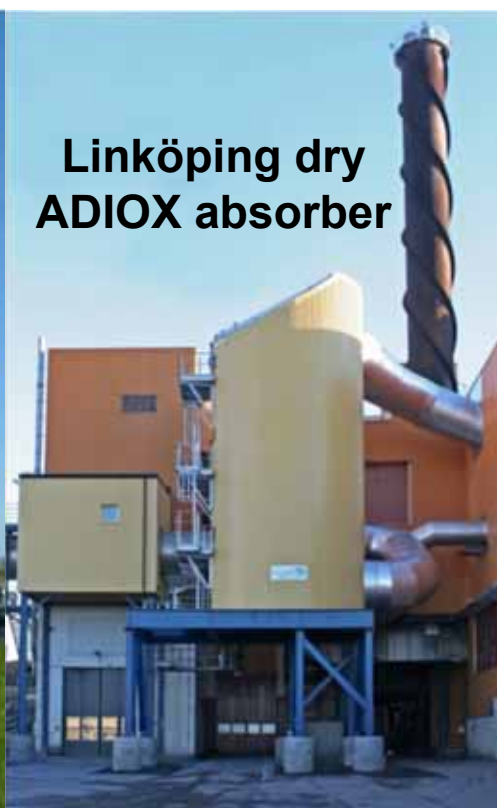
- Dioxin absorption in carbon filled polymer
- ADIOX material in packings and demisters
- If required a separate ADIOX absorber unit
- Always on-line to absorb dioxin
- Efficient also during plant start-up



Scrubber interior



ESP+ADIOX



**Linköping dry
ADIOX absorber**



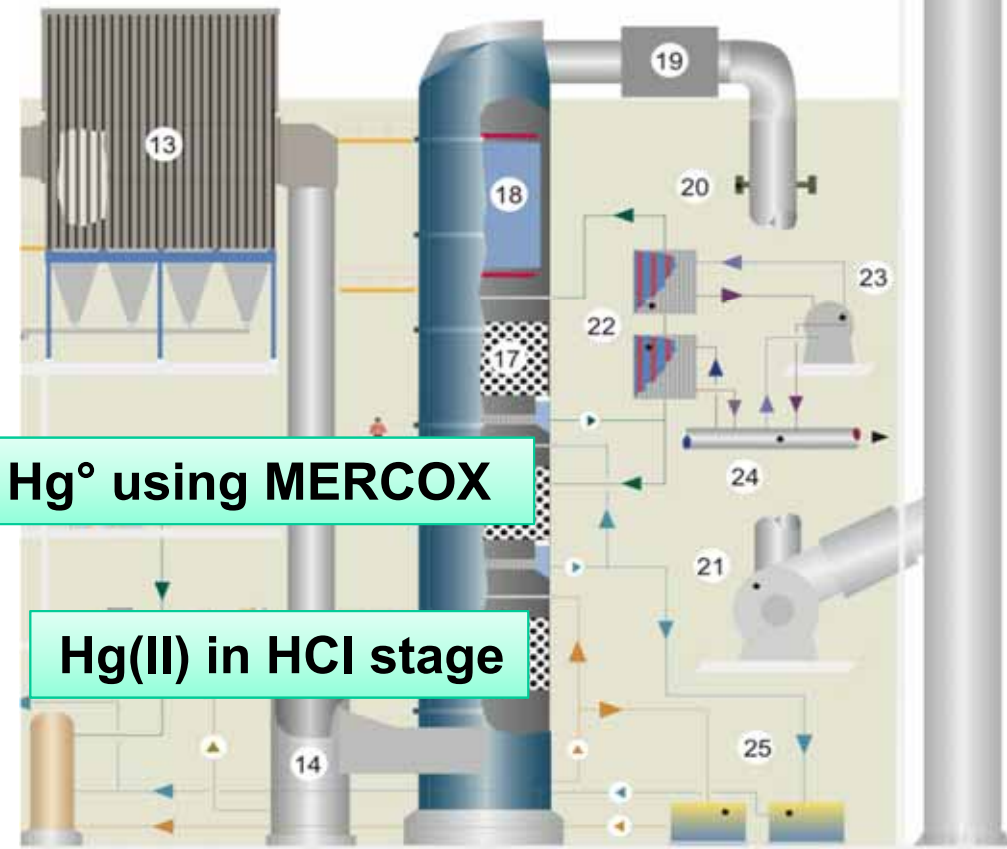
Hg

- **Bag house filter + carbon injection** is normally sufficient for Hg removal
- **MERCOX** in case of very high Hg loads or very low emission values

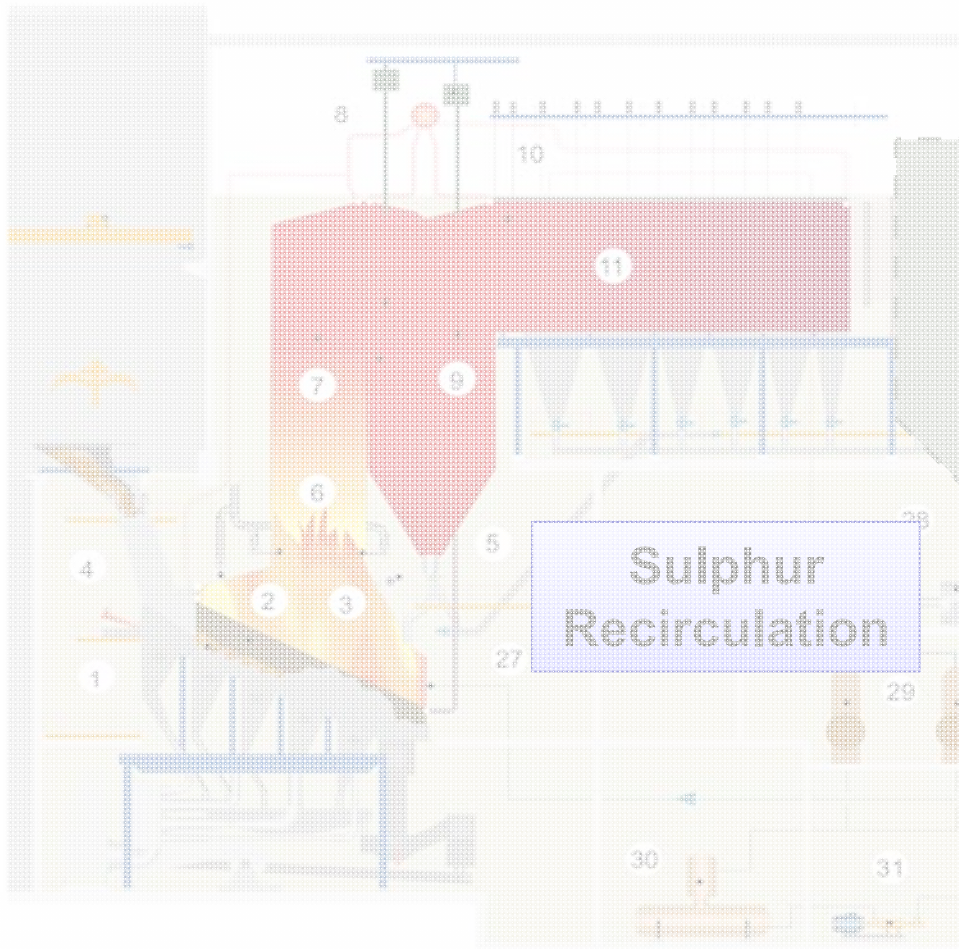
$\text{Hg}^{\circ} + \text{Hg}(\text{II})$
using activated
carbon

Hg° using MERCOX

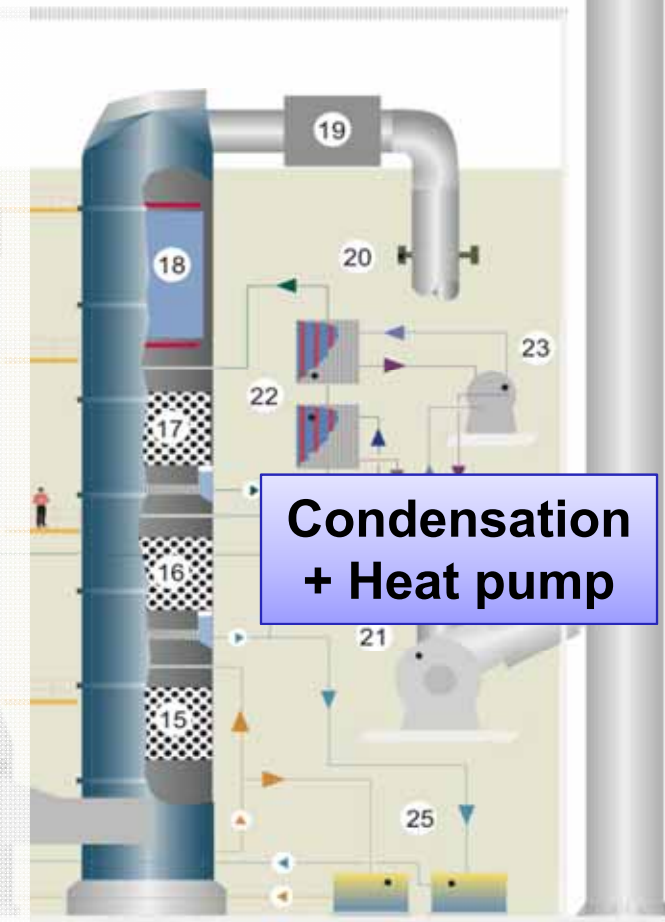
$\text{Hg}(\text{II})$ in HCl stage



Energy recovery

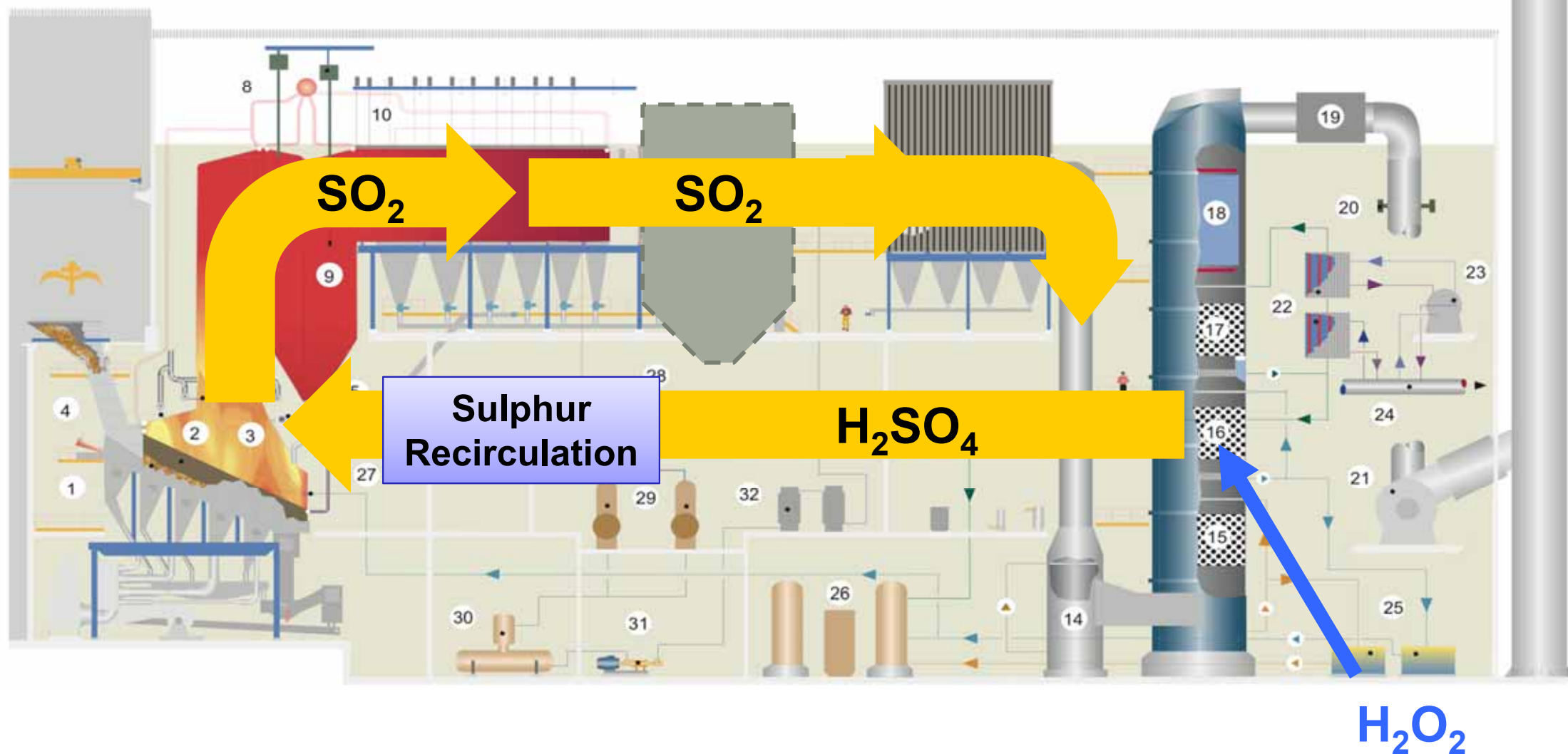


Vestforbraending
absorption heat pump



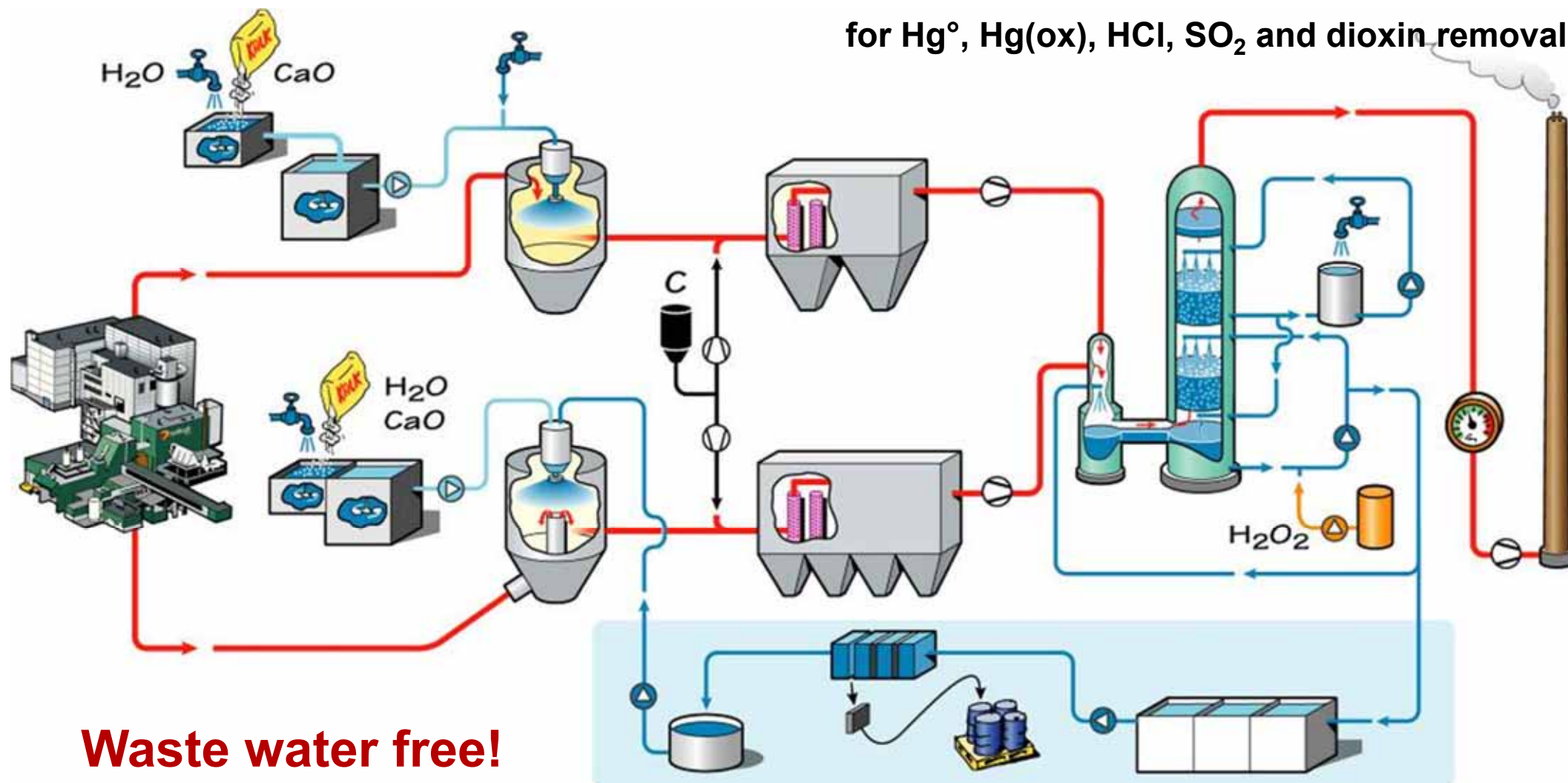
- Increased energy recovery by some 20-25 % by condensation with heat pumps

Energy efficiency: Sulphur Recirculation



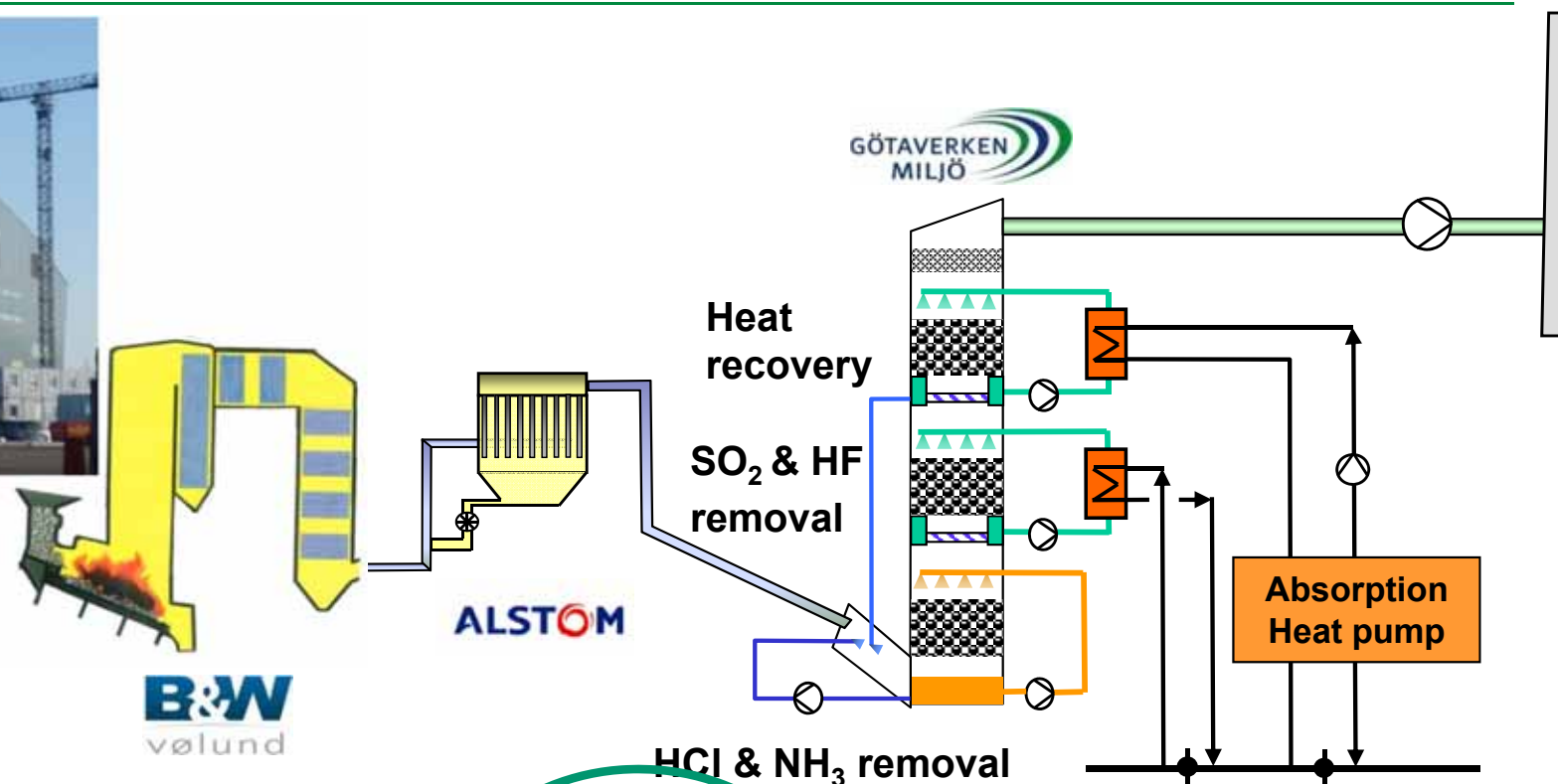
Hg: Sakab Hazardous waste incinerator, Sweden

Multifunctional MercOx- and ADIOX scrubber for Hg^0 , $\text{Hg}(\text{ox})$, HCl , SO_2 and dioxin removal



Waste water free!

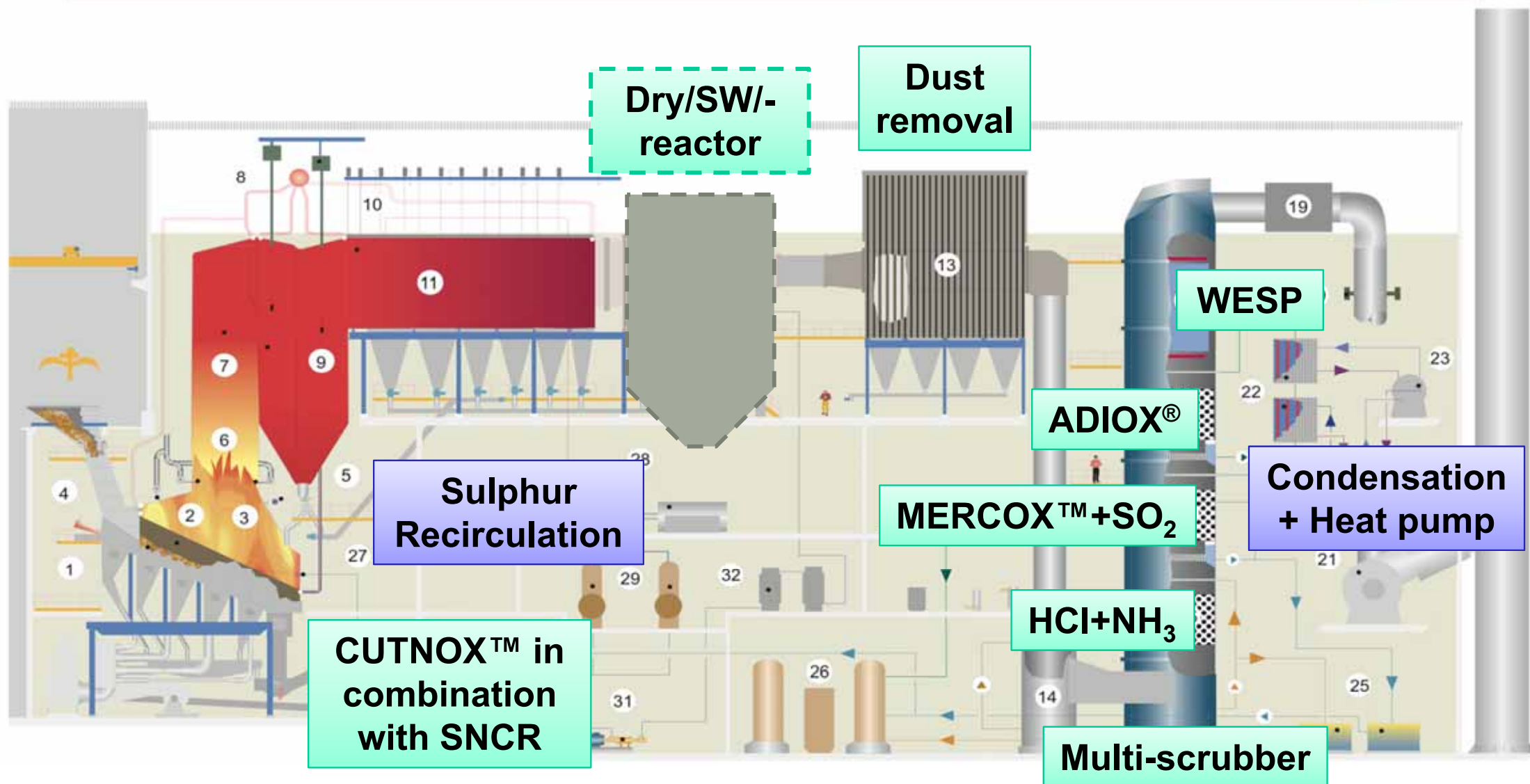
Filborna, Helsingborg (SE)



Emissions:

	Units	After boiler	Before scrubber	Emission guarantee	Emission expected
HCl	mg/Nm ³	2000	45	5	~ 1
SO ₂	mg/Nm ³	1000	50	25	~ 1
HF	mg/Nm ³	30	1	0.5	~ 0.1
PCDD/Fs	ng/Nm ³	10	0,05	0,05	~ 0.02

Conclusions



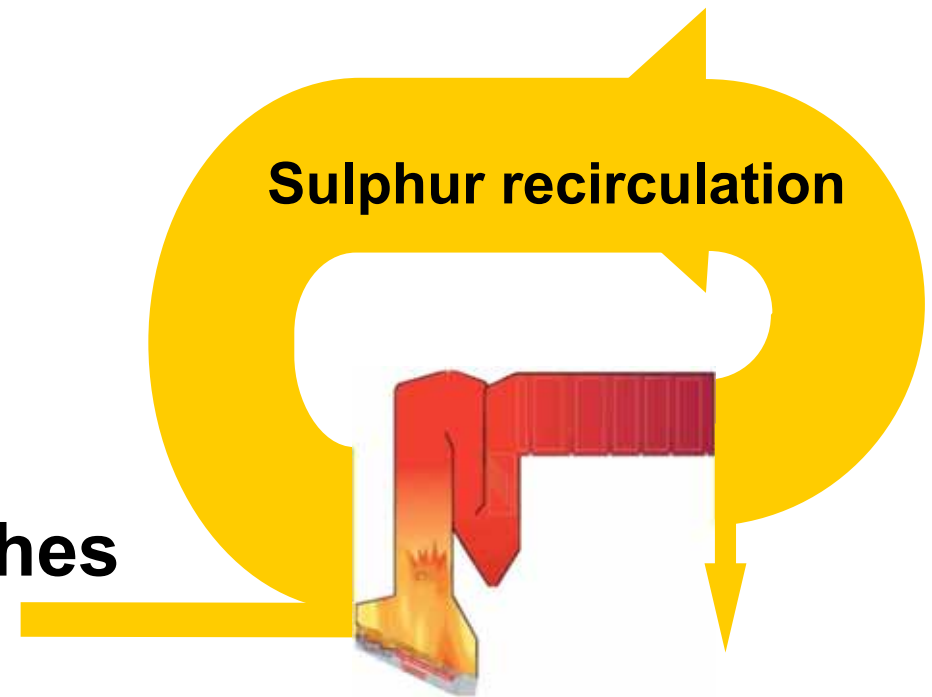
Conclusions

- Reduced NO_x concentration / NH₃ consumption
- Less TOC, Cl and PCDD/Fs in the bottom ash
- Smaller variations in temperature and steam flow



Conclusions

- **Potential for sulphate waste water free operation**
- **Less dioxins, deposits and ashes**
- **More electricity production or less corrosion**



sven.andersson@gmab.se

