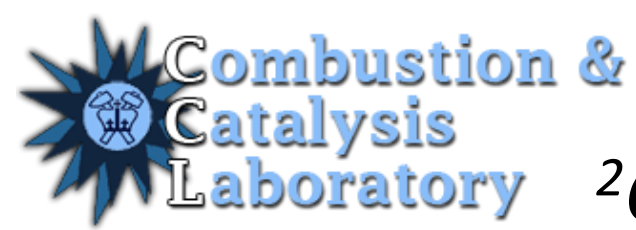


# Mitigating Chloride Corrosion in WTE Superheater Tube Alloys

Timothy Sharobem<sup>1</sup>, Marco J. Castaldi<sup>2</sup>, Nickolas J. Themelis<sup>1</sup>



<sup>1</sup>Columbia University, Department of Earth and Environmental Engineering, New York, NY

<sup>2</sup>City College of the City University of New York, Department of Chemical Engineering, New York, NY



## Project Motivation

### Chlorides Affect WTE Superheater (SH) Corrosion

MSW contains between 0.4-0.7 wt% chlorine. This fraction is liberated from waste during combustion in the form of HCl, Cl<sub>2</sub>, and metal chlorides which can react with, deteriorate heat transfer surfaces.

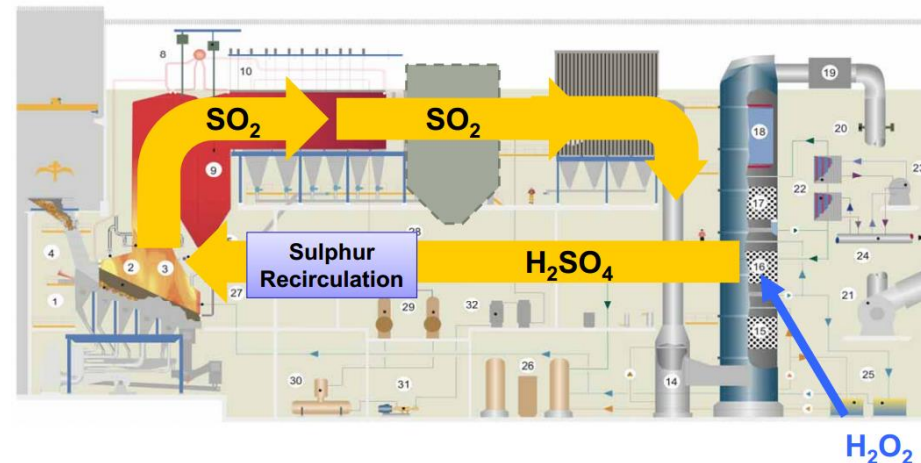
Chlorides have been largely attributed to the corrosion observed in WTE superheater tubes.

WTERT-US survey: Boiler maintenance costs WTE plants on average *\$4 per short ton combusted*<sup>1</sup> or ~6% of gate fee

### Some Potential Solutions to Reduce Cl Corrosion

- Design boilers, SH tubes with alloys, overlays, or coatings with Cl resistant materials
- Investigate sorbents to capture Cl compounds
- Additives which modify tube deposits to more corrosion resistant (e.g. sulfur- containing additives)

*Novel approach for reducing Cl corrosion via SO<sub>2</sub> recirculation, by Gotaverken Miljo<sup>2</sup>*  
[WTERT 2012 presentation]



## Corrosion Testing

### Current Research Questions

- ✓ How are SH tube alloys affected by chloride deposits? What are the probable corrosion mechanisms?
- ✓ What types of alloys provide protection against high temperature corrosion of chlorides?
- ✓ What is the effect of the SO<sub>2</sub>/HCl ratio on alloys under chloride deposits?
- ✓ What is/are the most cost effective approaches to mitigating Cl corrosion in WTE boilers?

### Experimental Approach

#### 1. Coupon Cutting and Cleaning



*Coupons cut from SH alloys, 3.2 cm<sup>2</sup> area*

#### 2. Furnace Tests



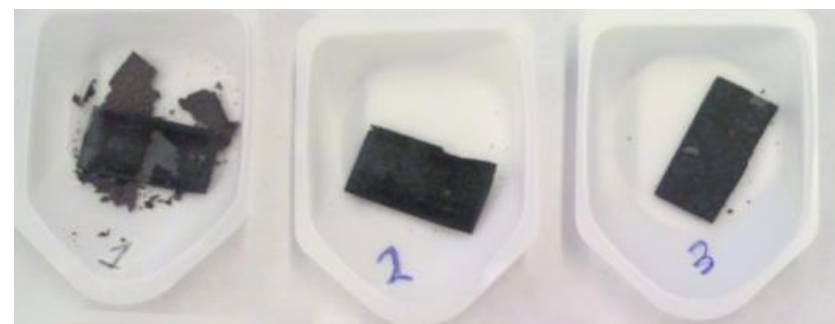
*Isothermal testing, under synthetic WTE flue gas*

#### 3. Coupon, Deposit Characterization



*XRD, SEM-EDS*

#### 4. Corrosion Rate Assessment

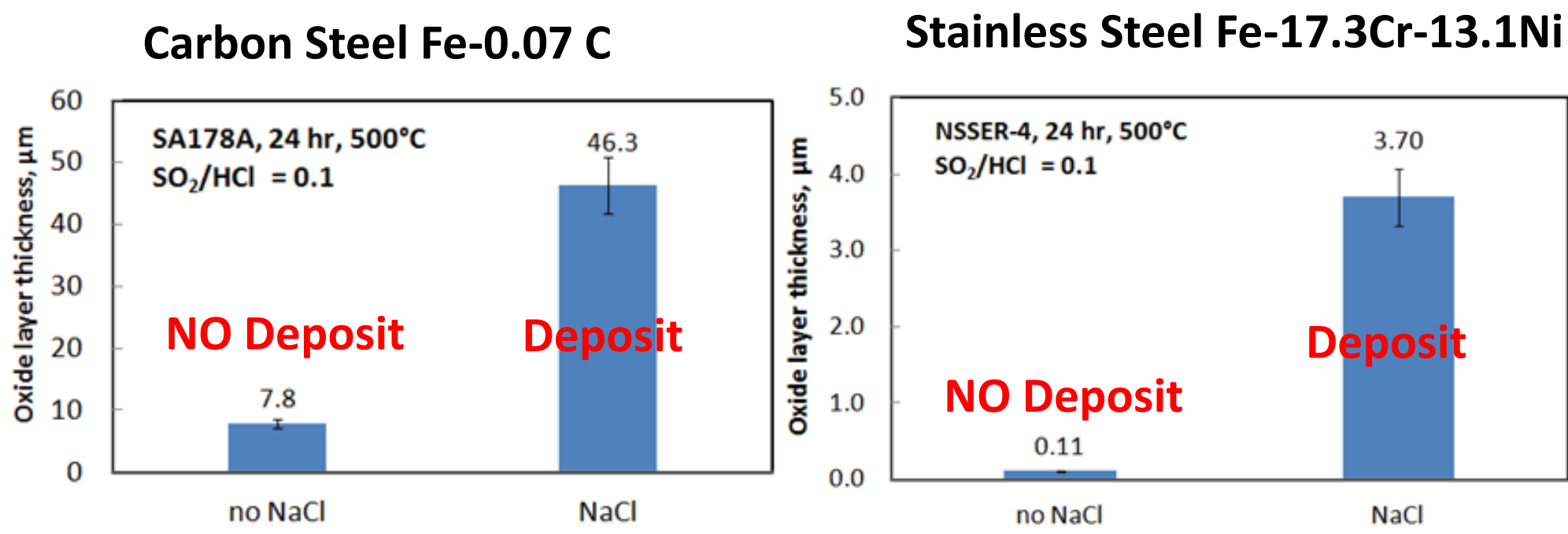


*Rate calculated from mass loss, in accordance with ASTM method G1-03*

**Testing Conditions** Metal temperatures: 450-550°C (842-1022°F); Gas Composition: 8% O<sub>2</sub>; 12% CO<sub>2</sub>; 15% H<sub>2</sub>O; 800 ppmv HCl; SO<sub>2</sub> 80-800 ppmv; N<sub>2</sub> balance, 500 SCCM, Deposit NaCl chosen as chloride surrogate, deposit on coupon of 4.0 mg/cm<sup>2</sup> ± 10%

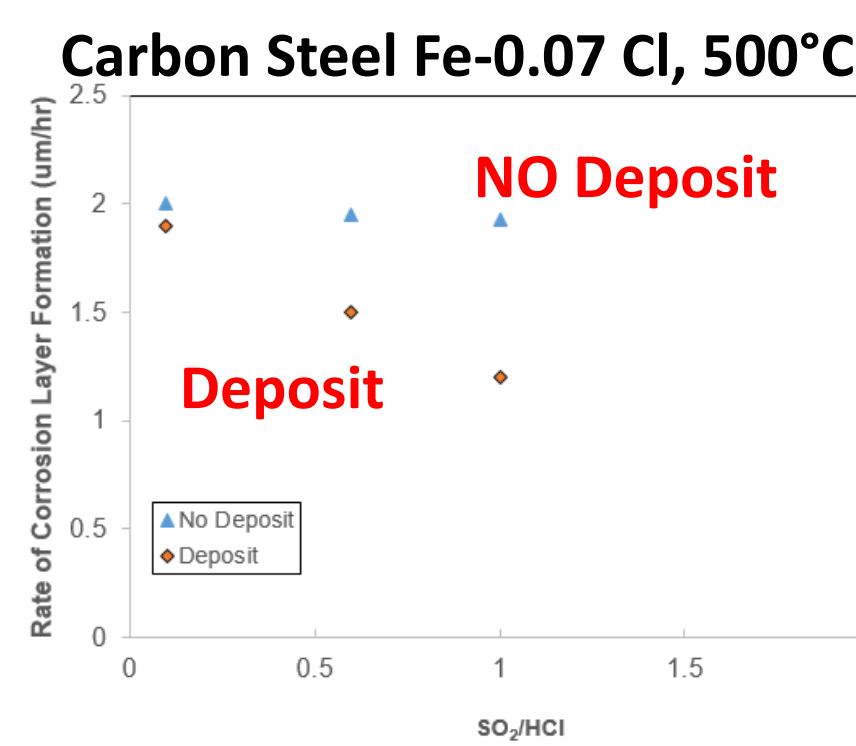
## Results and Discussion

### Effect of Chloride Deposit



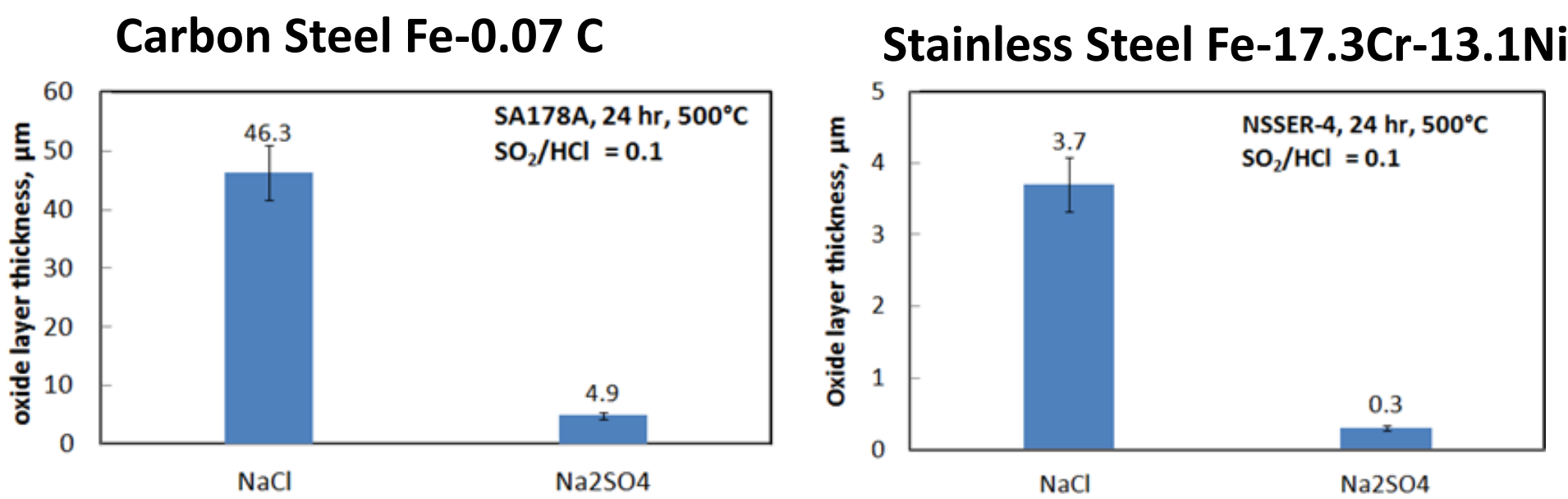
NaCl layer **significantly** accelerate corrosion layer formed onto c-steel, stainless steel over 24 hours by about an order of magnitude at 500 °C (932 F)

### Trends with the SO<sub>2</sub>/HCl Ratio



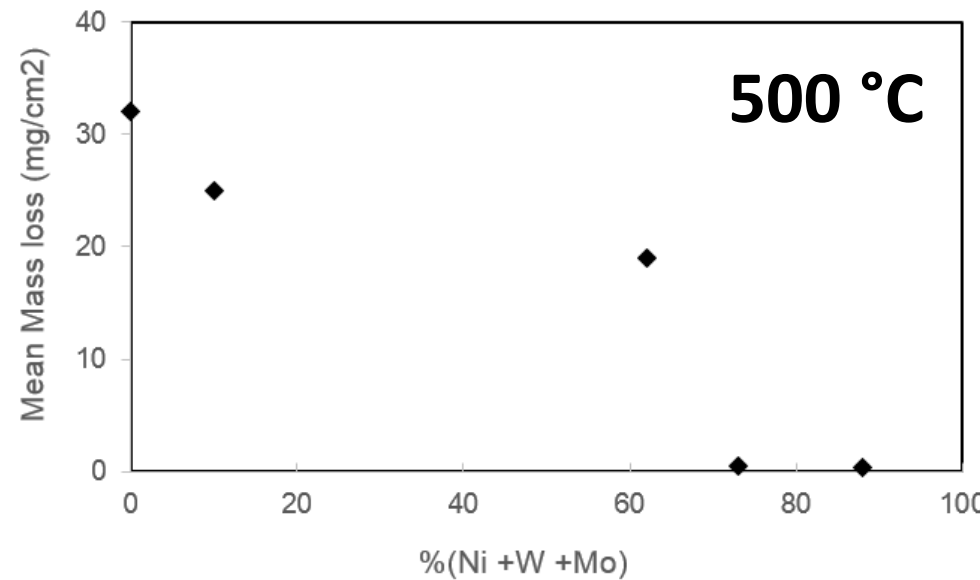
**Increasing the SO<sub>2</sub>/HCl** to elevated levels above typical operation range of 0.1-0.3 range **suppresses** formation of corrosion for c-steel at 500 °C (932 F)

### Potential Effect of Sulfating Chloride Deposits



Replacing chlorides with sulfates, **substantially** reduces corrosion layer at 500 °C (932 F)

### Effect of Alloy Composition on Chloride Resistance



Increasing concentration of **Ni+W+Mo** has shown significant improvement on material loss under NaCl deposit

## Conclusions

- ❖ Chloride deposits considerably accelerate alloy corrosion under superheater conditions versus sulfate deposits or under WTE flue gas alone
- ❖ Increasing the SO<sub>2</sub>/HCl ratio can suppress the accelerated corrosion due to chloride deposits for carbon and stainless steels
- ❖ Increasing the concentration of certain alloying elements, in particular Ni, W, Mo can achieve better SH chloride corrosion performance
- ❖ Future work will investigate economic impact of alloying choice versus additives

### References

1. PhD Thesis, Shang-Hsiu Lee
2. Sven Andersson Presentation, WTERT 2012



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