

Reuse applications for the fine fraction of WtE bottom ash

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Outline of Presentation

- **Introduction:**
 - Circular economy
 - Sustainable waste management
 - Waste-to-Energy in circular economy
- **Production of sintered ceramics:**
 - Material characterisation
 - Ceramic processing optimisation
 - Leaching behaviour during processing
 - Effect of ash variability
 - Cost analysis
- **Production of foamed materials:**
 - Effect of rapid sintering
- **Conclusions**

Circular economy: The concept

Linear economy

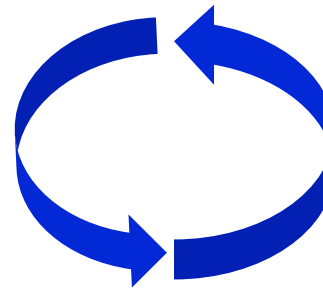


Circular economy

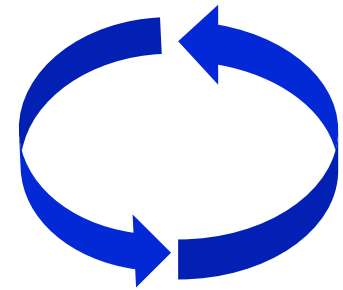
EXTRACT-> PROCESS -> MANUFACTURER ->
CONSUMER -> WASTE DISPOSAL

WASTE

Mixed technical and biological
materials

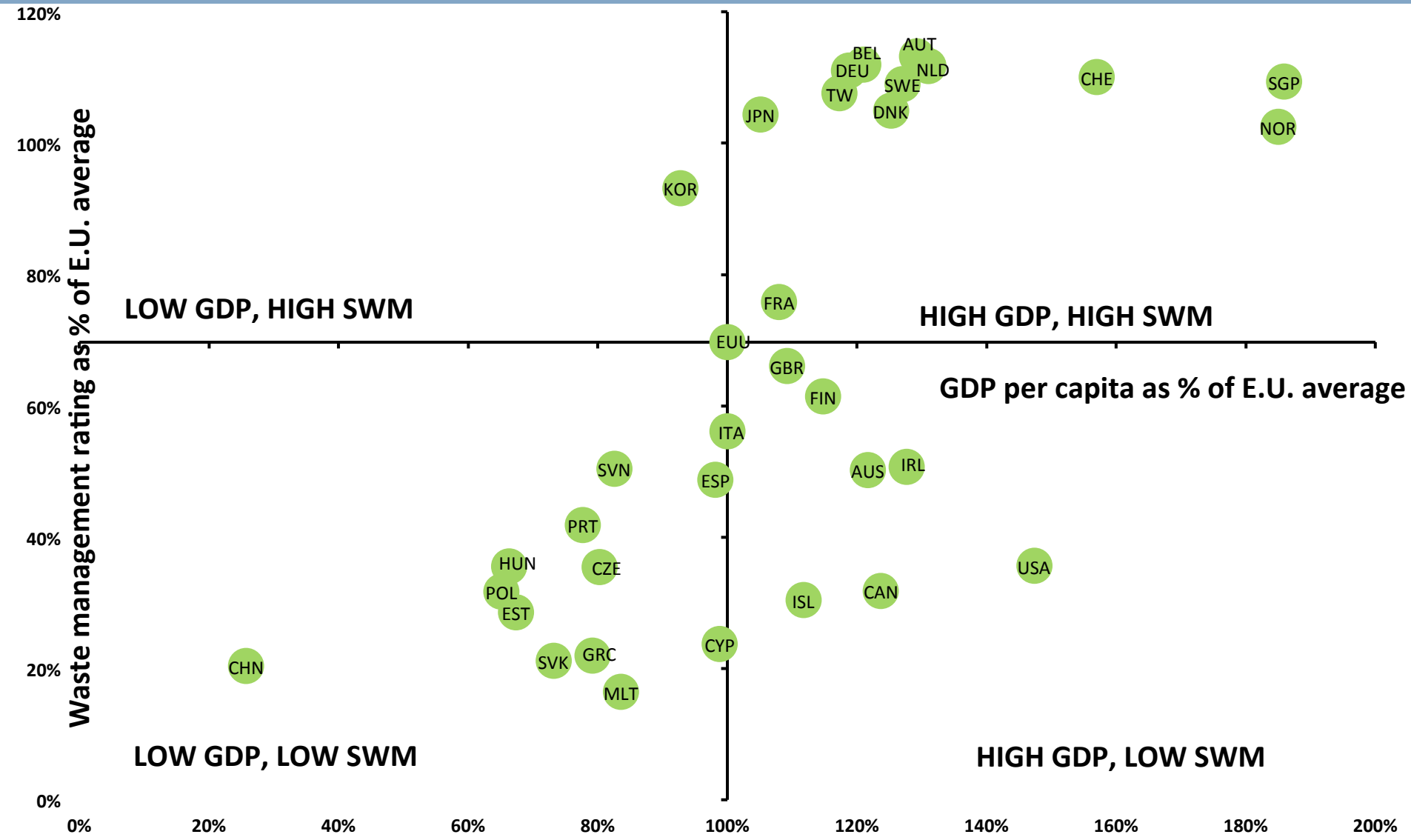


Technical nutrients Biological nutrients





Sustainable waste management (SWM) index vs per capita GDP



WtE and circular economy

Combustion



Waste to Energy

Flue Gas



Bottom Ash
150-250 kg/tonne
MSW



Air Pollution Control Residues
25-35kg/tonne MSW

Resources from Waste

WtE bottom ash recycling plant



Non-Ferrous metals (0.5-2%)



IBA Aggregate (85-95%)



Coarse fraction (10- 15%)



Medium fraction (40-70 %)

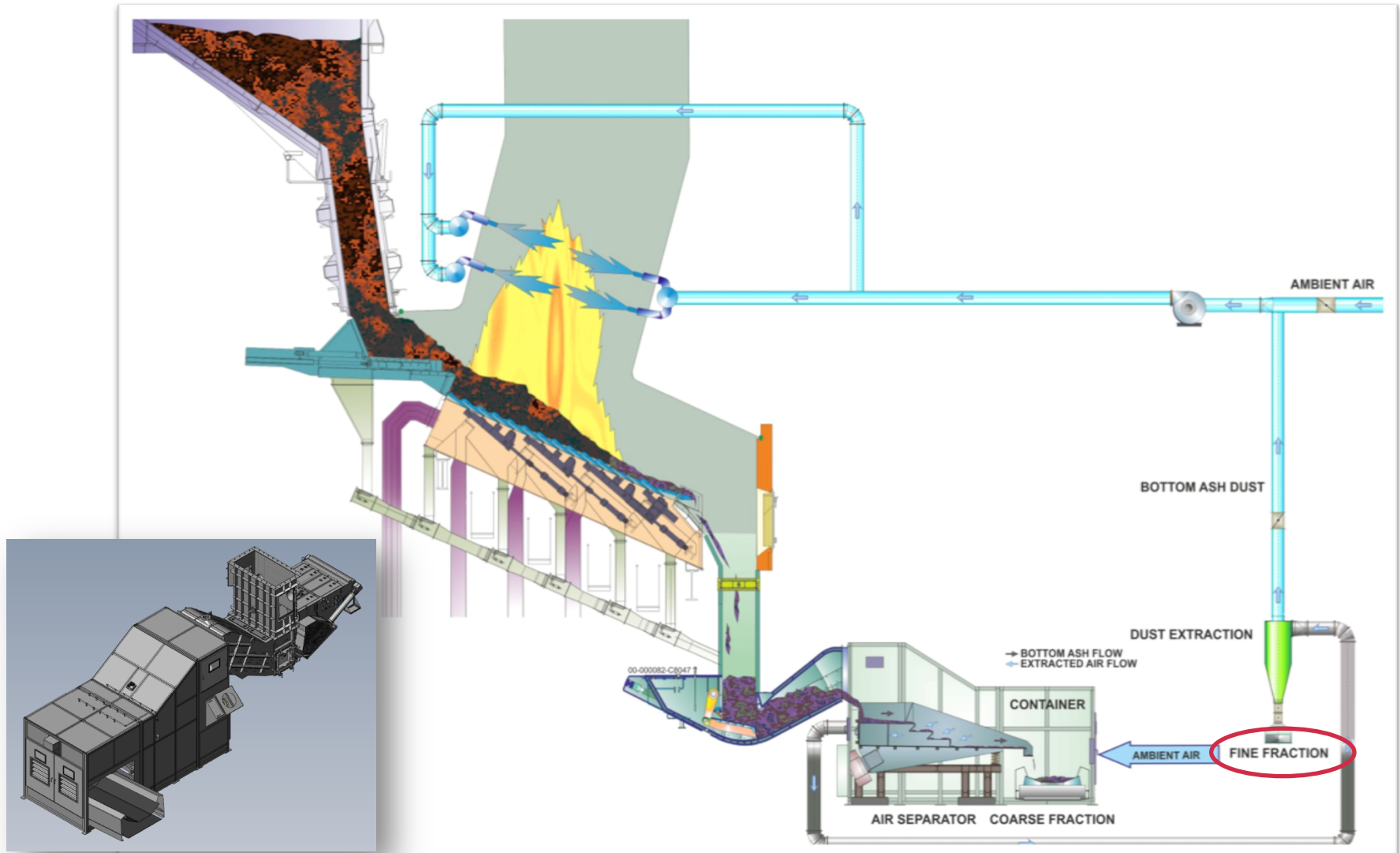


Fine fraction (11- 45 %)



Ferrous metals (5-15%)

Monthey dry discharge system- Martin development



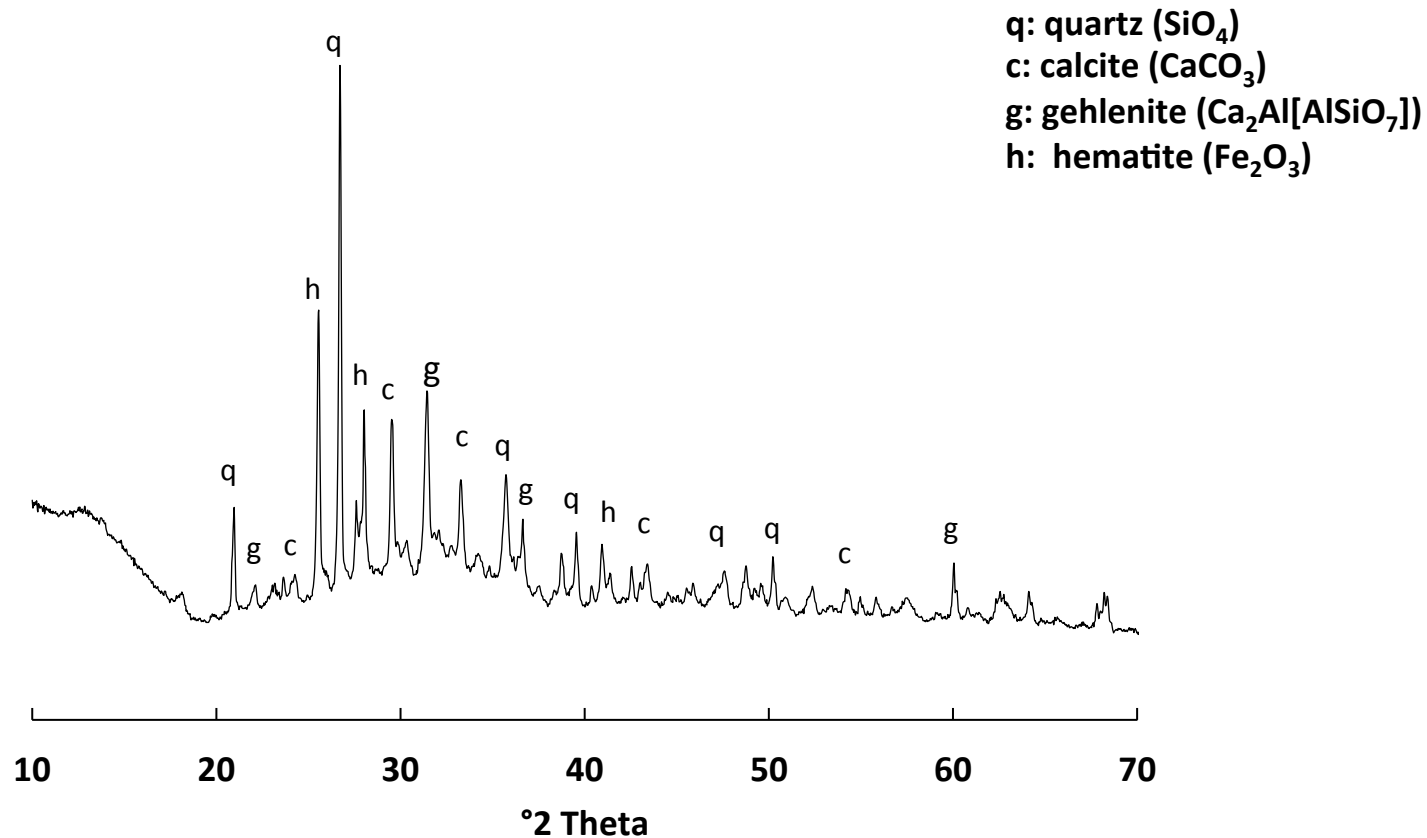
Production of sintered ceramics

Chemical composition of the <500µm IBA (oxide %)

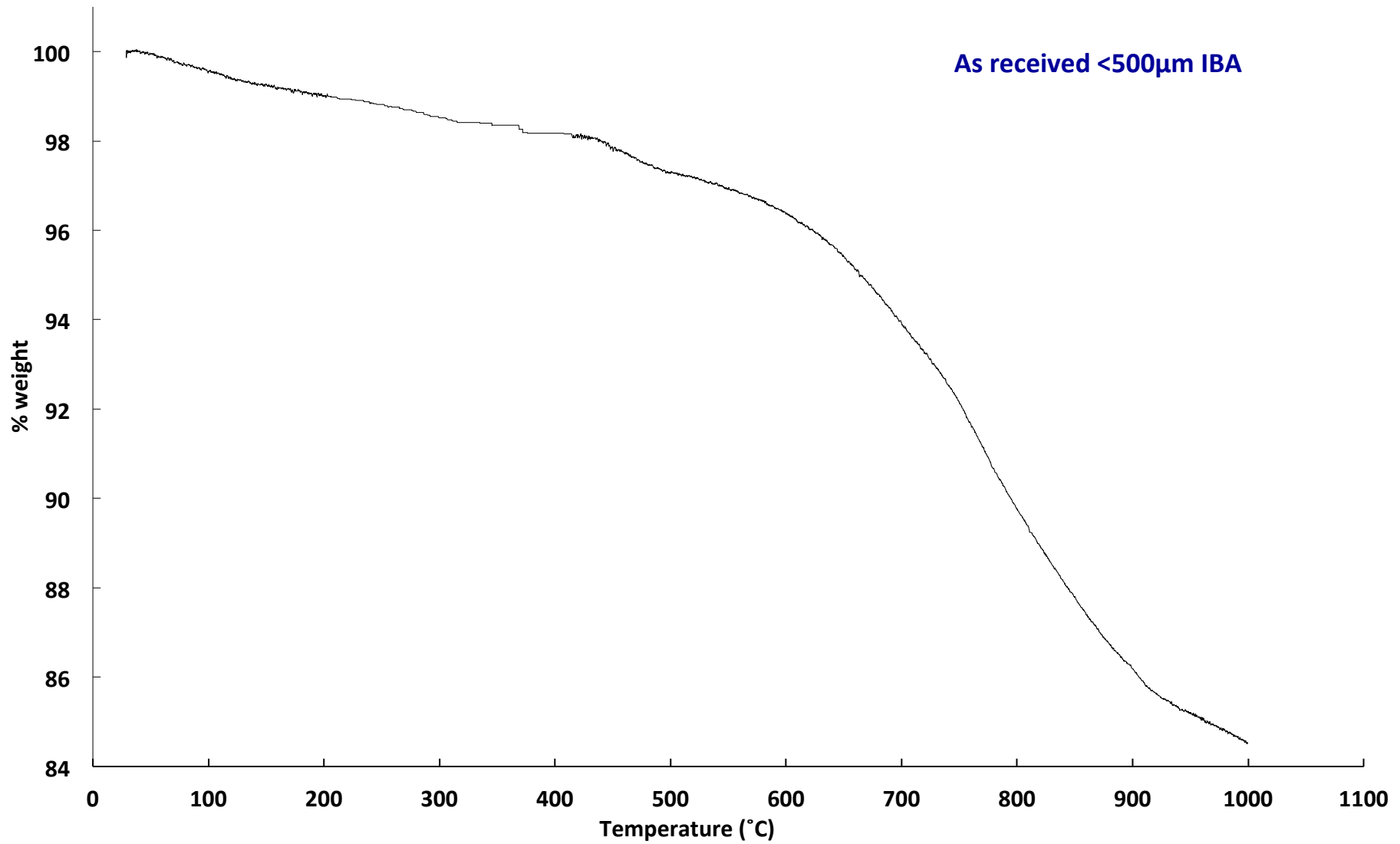
XRF analysis

Oxide	Weight percent %	Oxide	Weight percent %
SiO ₂	36.3	MgO	2.0
Fe ₂ O ₃	18.4	TiO ₂	1.9
CaO	15.7	P ₂ O ₅	1.9
Al ₂ O ₃	6.4	ZnO	1.8
SO ₃	5.7	Na ₂ O	1.5
K ₂ O	3.3	CuO	1.3
ClO ₂	2.2	Others	1.6
LOI (%)	15.0		

X-ray diffraction : <500 μ m IBA as-received

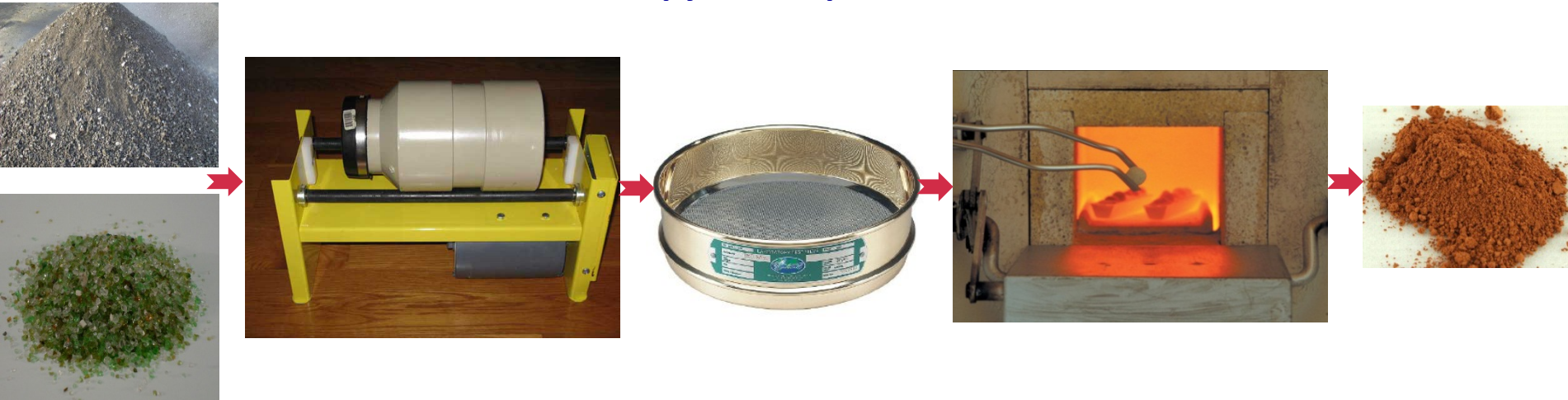


Thermogravimetric analysis (TGA)



Ceramics manufacturing process

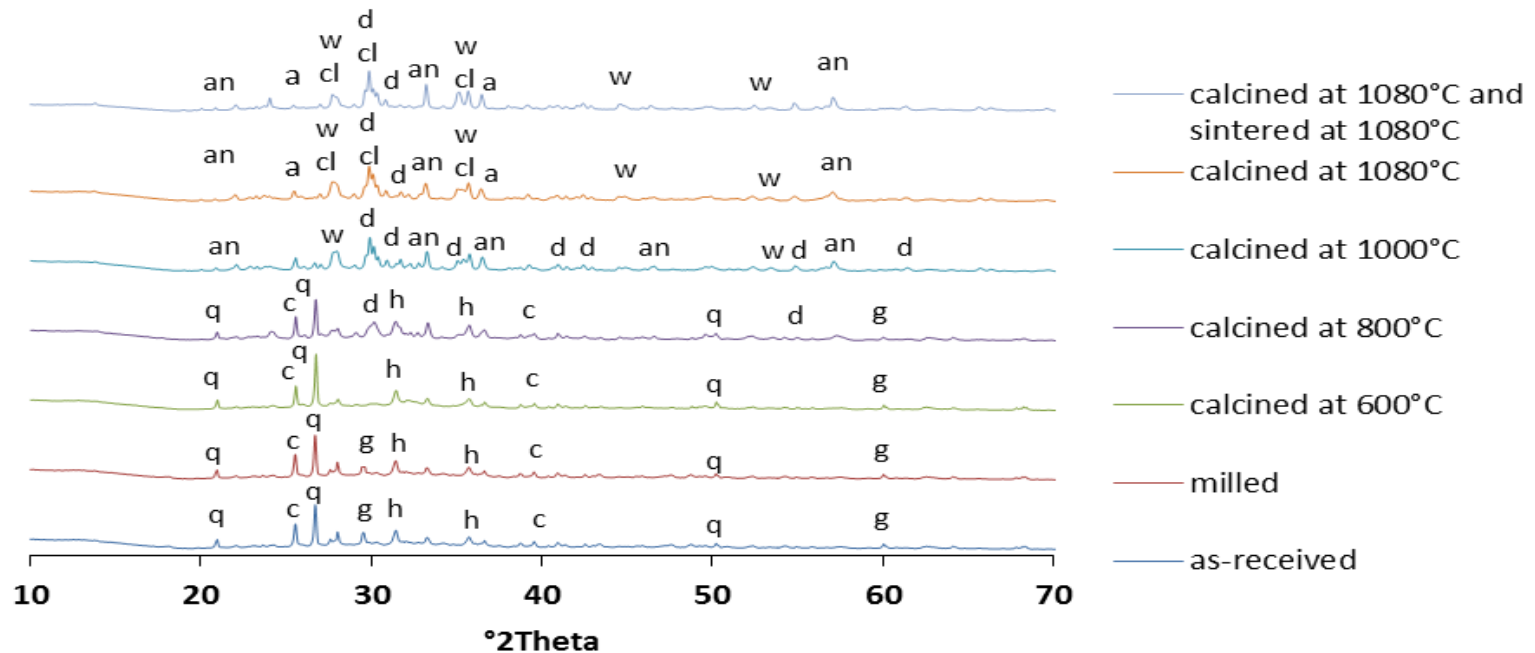
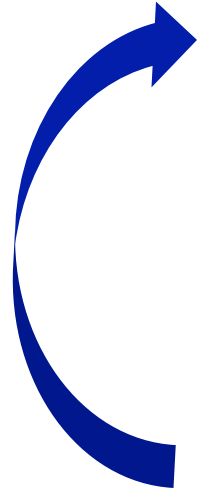
Production of pyroxene powder



Production of sintered ceramics



XRD: changes in crystalline phases during processing

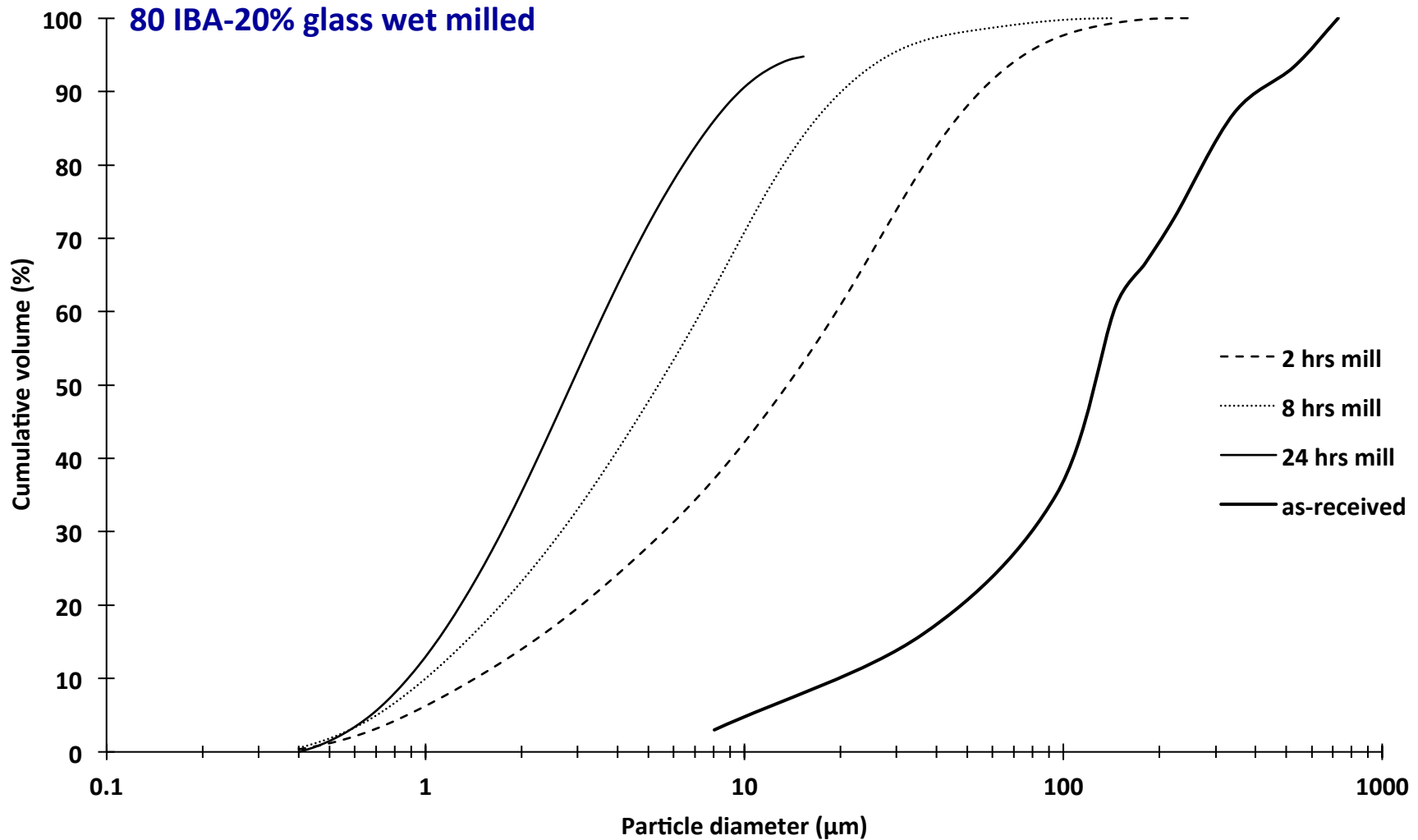


q-quartz (SiO_2); c- calcite (CaCO_3); h- hematite (Fe_2O_3); g- gehlenite ($\text{Ca}_2\text{Al}[\text{AlSiO}_7]$)

d-diopside ($\text{MgCaSi}_2\text{O}_6$) ; cl- clinoenstatite ($\text{Mg}_2\text{Si}_2\text{O}_6$); an-andradite ($\text{Ca}_3\text{Fe}_2\text{Si}_3\text{O}_{12}$)

w- wollastonite (CaSiO_3); a- albite ($\text{NaAlSi}_3\text{O}_8$)

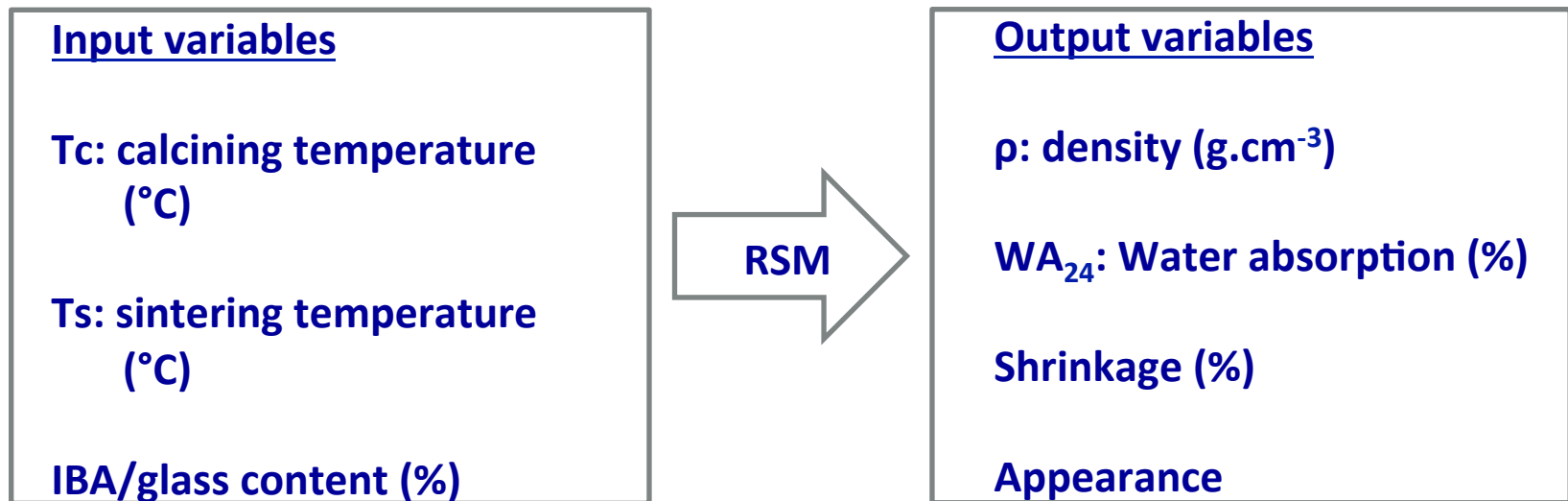
Effect of milling time: Particle size analysis



Process optimisation

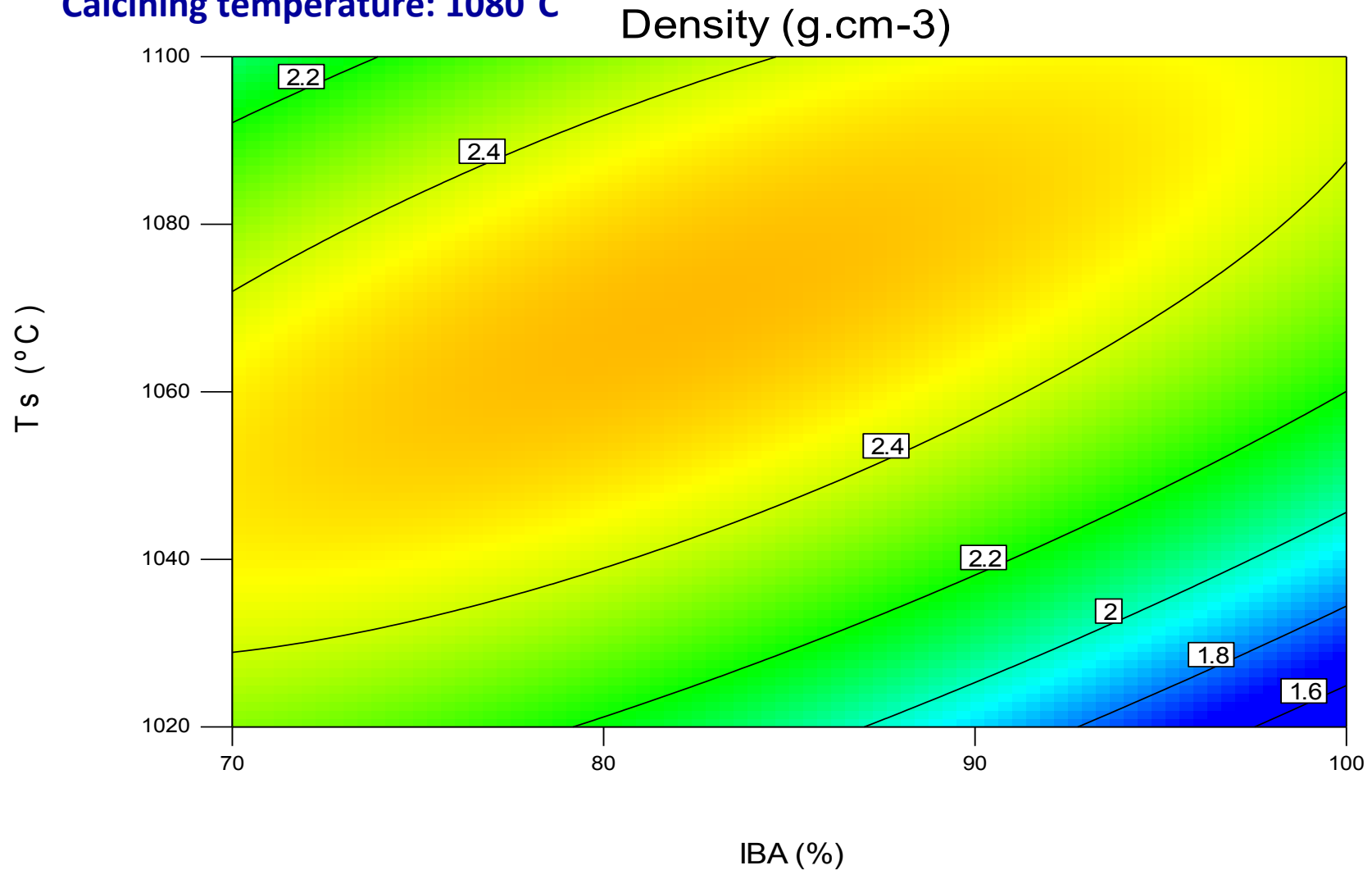
- **Response Surface Methodology (RSM) was used and the Design Expert software**
- **Describes the relationship between input variables and allows the achievement of optimum processing conditions**
- **Four steps: model fitting, validation of the model, response surface and optimization**
- **200 results from the laboratory work were use as standard points for the system**

Process optimisation: Inputs and outputs



Response Surface for density

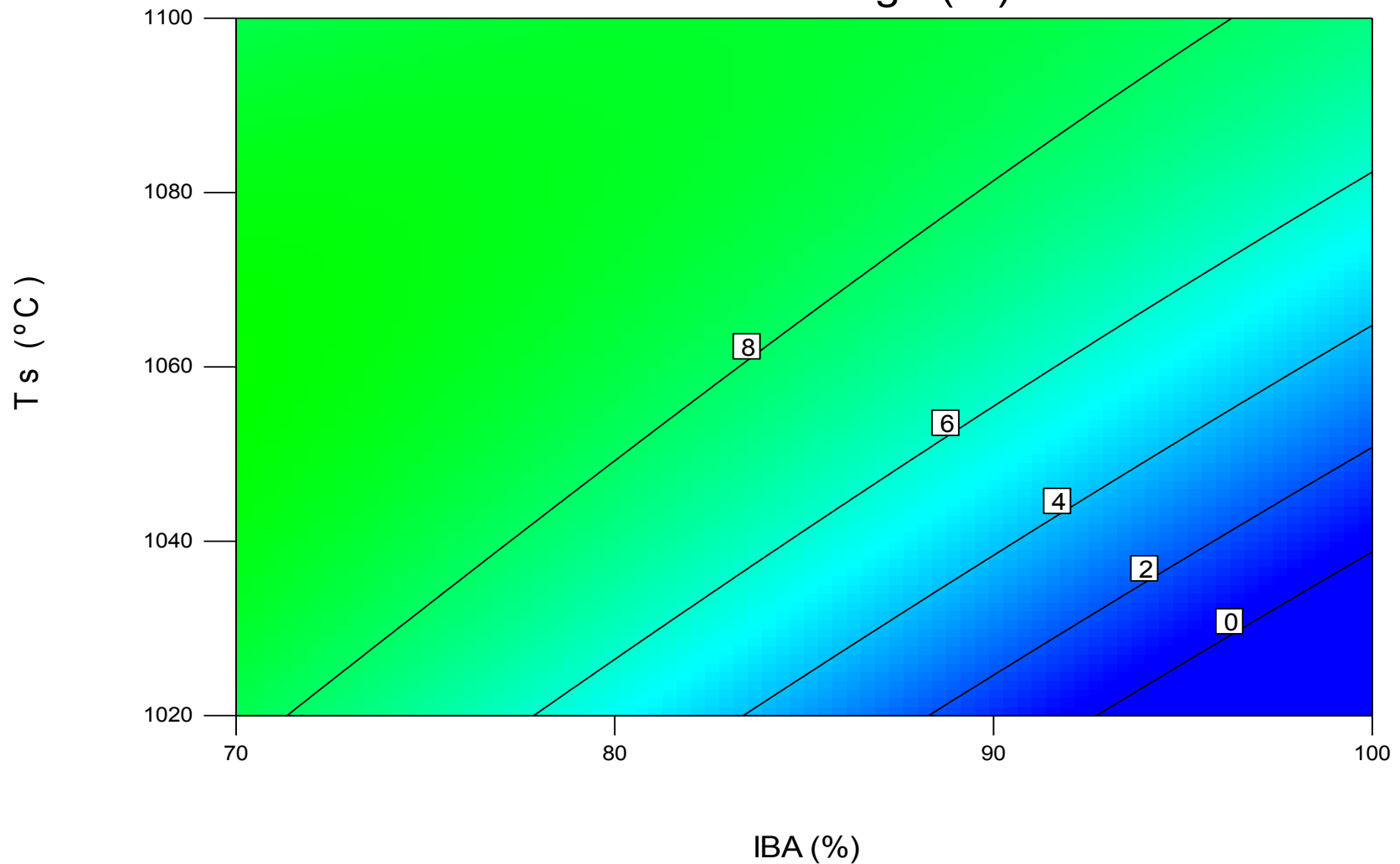
Calcining temperature: 1080°C



Response Surface for shrinkage

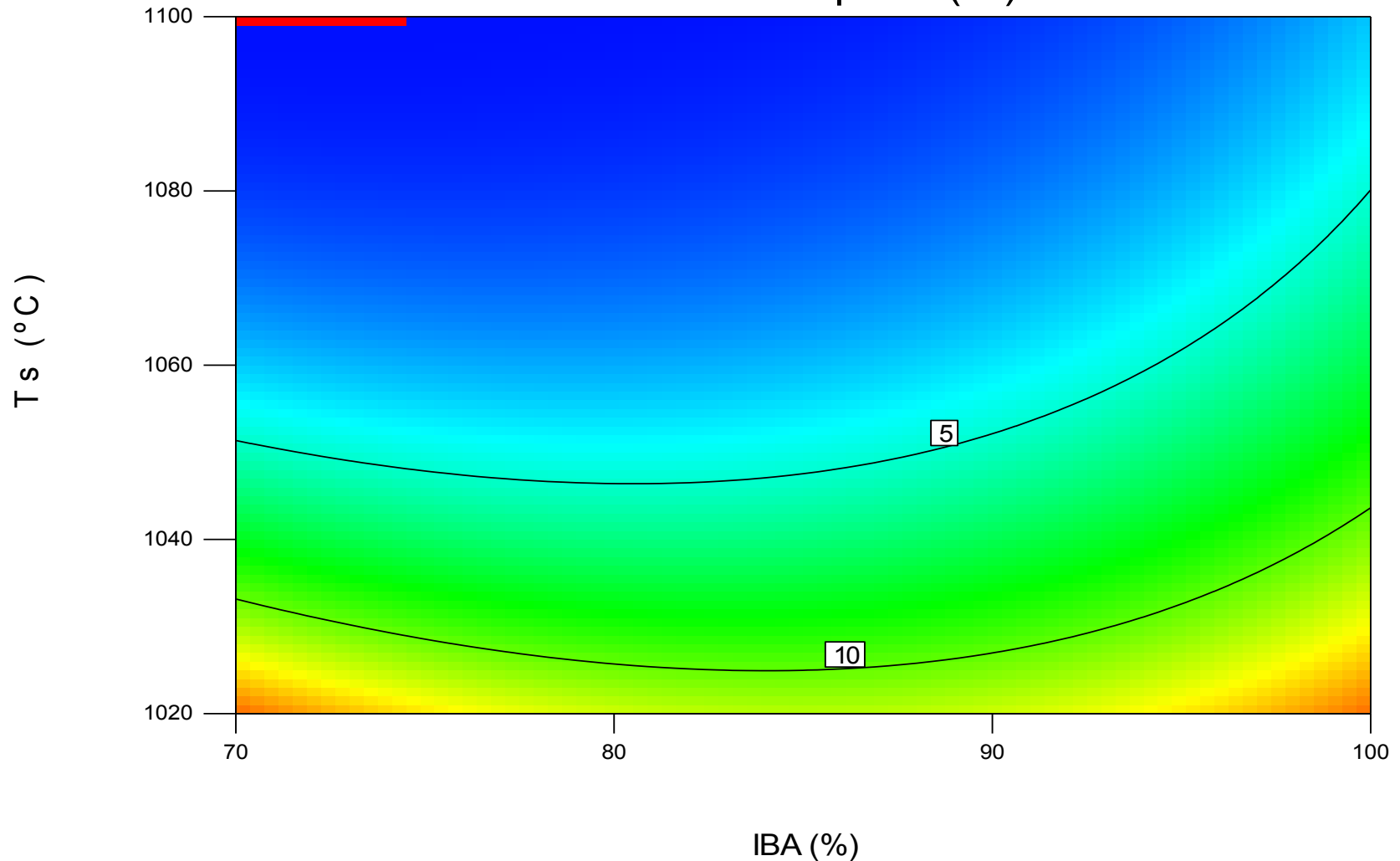
Calcining temperature: 1080°C

Linear shrinkage (%)



Response Surface for water absorption

Calcining temperature: 1080°C Water absorption (%)

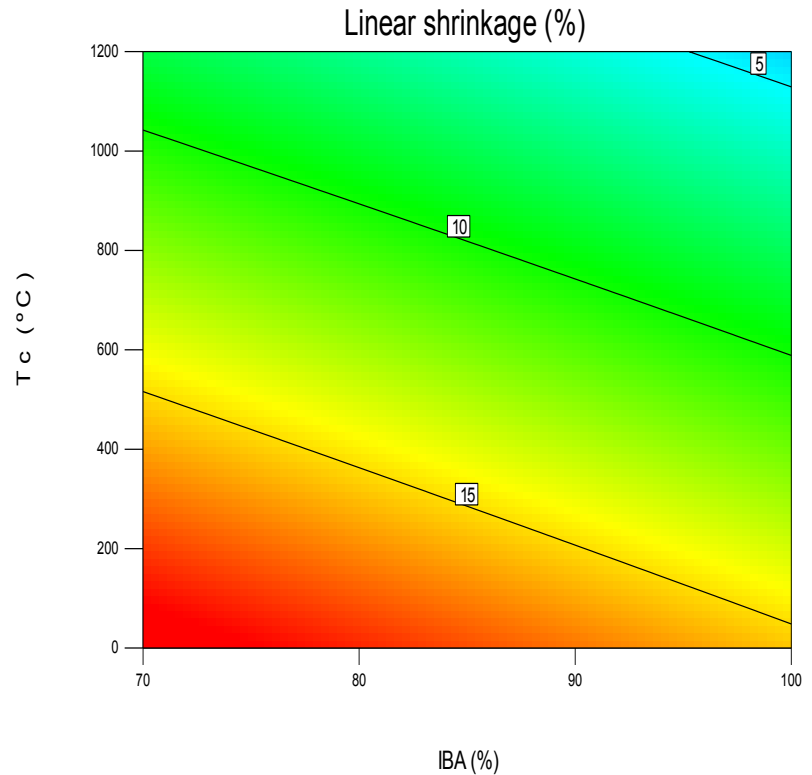
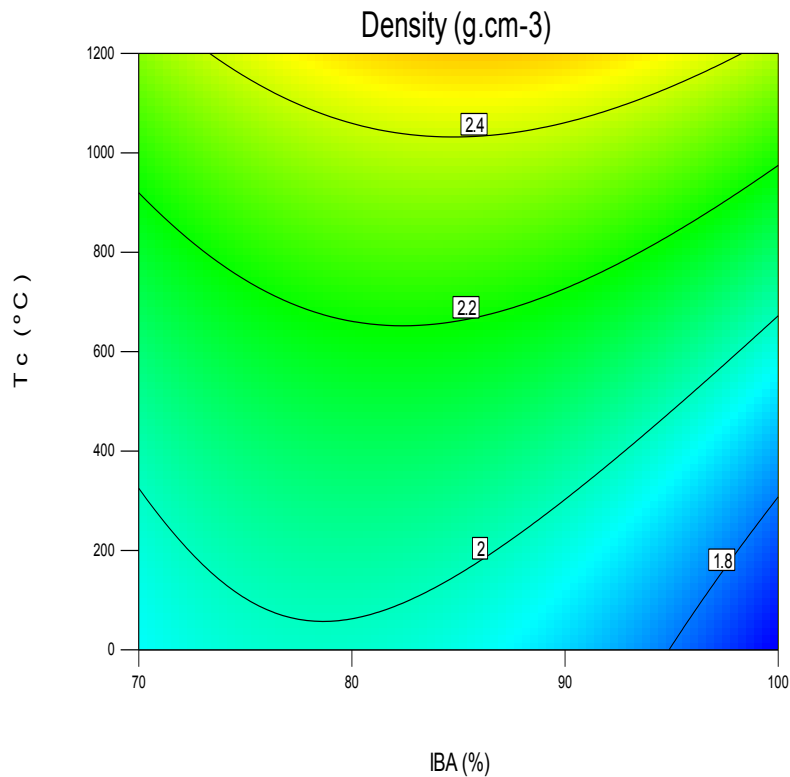


Effect of calcining on density and shrinkage of sintered ceramics

Density

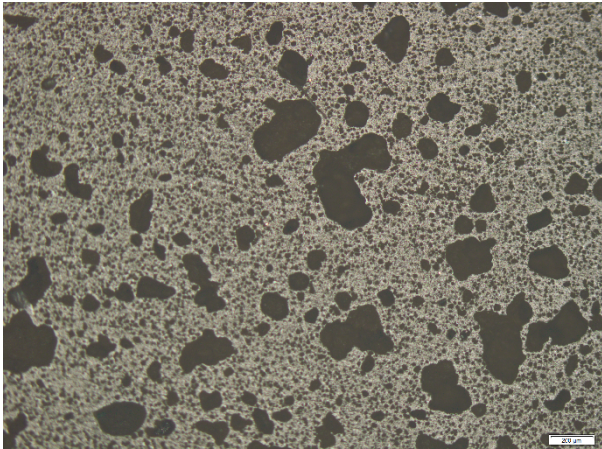
Firing temperature:
1080°C

Shrinkage

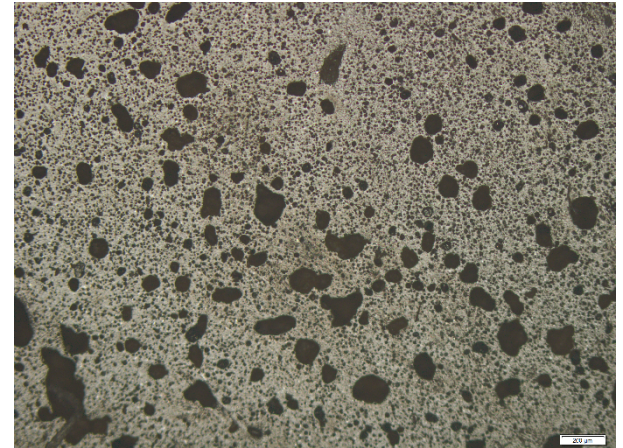


Effect of calcining on microstructure of sintered ceramics

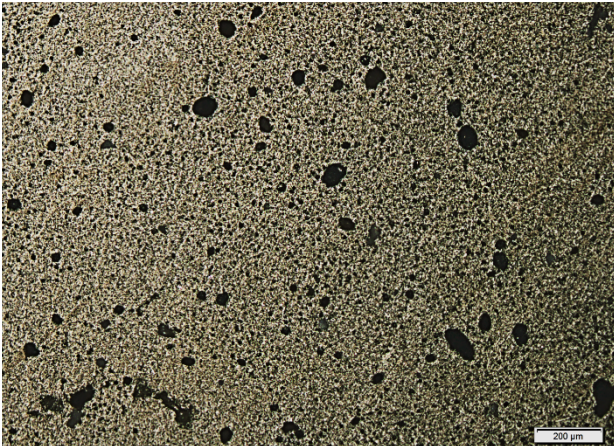
600 °C



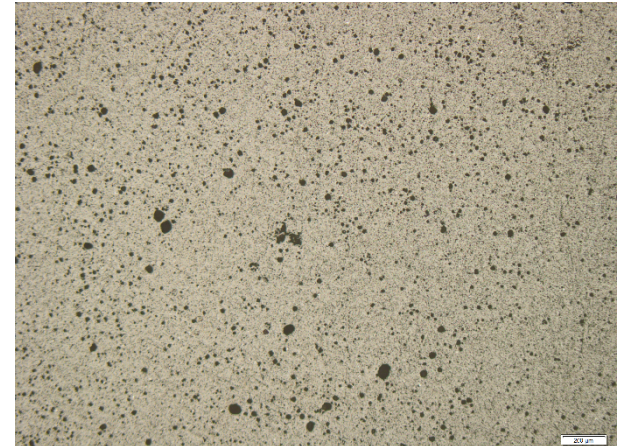
800 °C



1000 °C



1080 °C

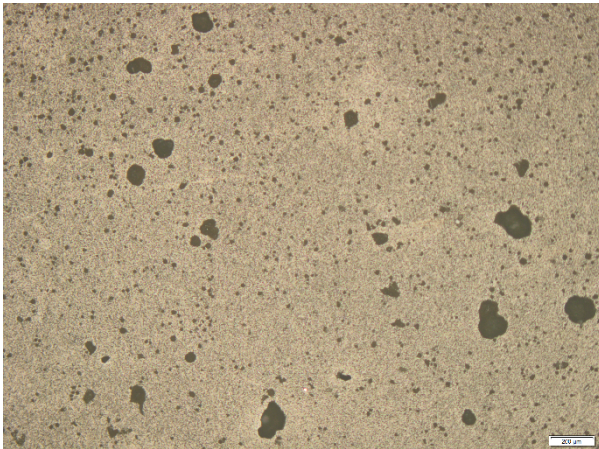


Optimum processing conditions

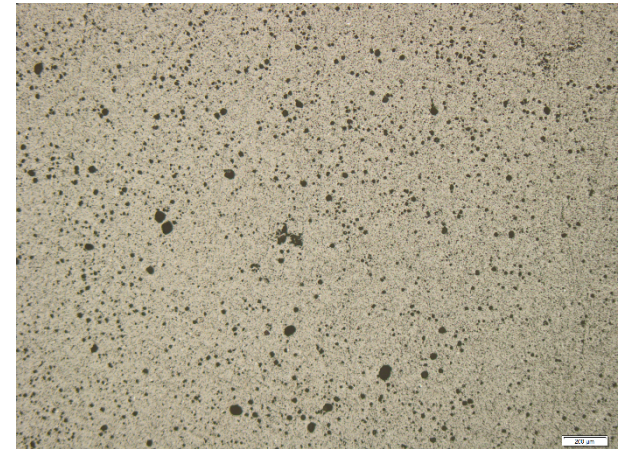
IBA (%)	T _c (°C)	T _s (°C)	Density* (g/cm ³)	Water absorption* (%)	Shrinkage* (%)	Appearance*
100	1200	1130	2.40	0.9	5.1	5.1
90	1100	1100	2.52	0.1	5.3	5.3
80	1080	1080	2.72	0	5.4	5.5
70	1060	1040	2.74	0	5.5	5.3
Clay Ceramics			2.1-2.3	0-5	7-12	

Microstructure of optimum samples

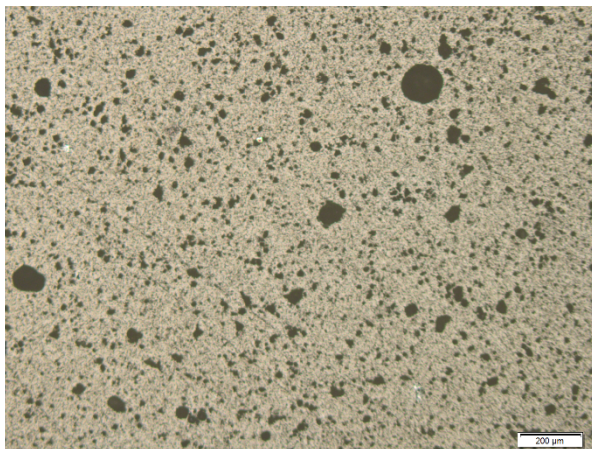
70wt.% IBA



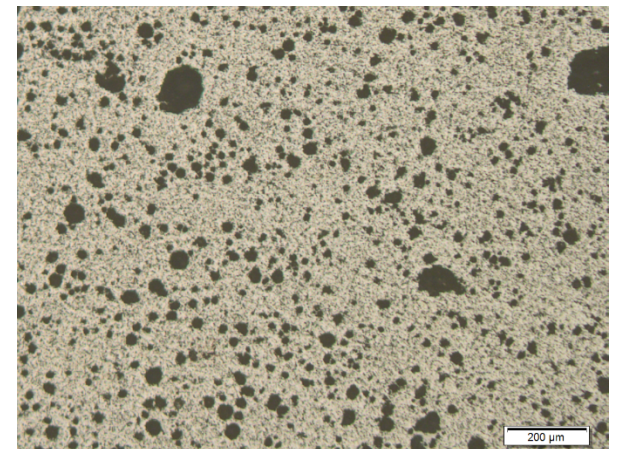
80wt.% IBA



90wt.% IBA



100wt.% IBA



Metals: IBA as received, pyroxene powder and sintered ceramic

		Amount leached (leachate pH 3)				
	Concentration in IBA	IBA as received	Pyroxene powder		Sintered ceramic	
	mg/kg	mg/kg	mg/kg	% reduction	mg/kg	% reduction
Cr	163	17.9	0.75	95.8	0.6	96.7
Cu	3200	887.6	21.8	97.5	19.5	97.8
Ni	197.5	9.3	0.13	98.6	0.05	99.5
Cd	63	4.6	0.16	96.5	0.09	98.1
Zn	3100	1139.4	9.4	99.2	8.2	99.3
Pb	350	133.1	0.15	99.9	0.07	99.7
Al	11500	1742	57.9	96.7	53.1	96.9
Fe	4600	1013	6.12	99.4	4.5	99.6

Comparison of mechanical properties of sintered ceramics

Mechanical property	Sintered ceramics	Clay ceramics	Alumina ceramics
Density (g/cm ³)	2.7	2.3	3.8
Young's modulus (GPa)	76.2	71	300
3-point bending strength (MPa)	80.9	78.2	400
Vickers microhardness (GPa)	4.4	3.1	20
Thermal conductivity (W/m*K)	0.6	0.6	3

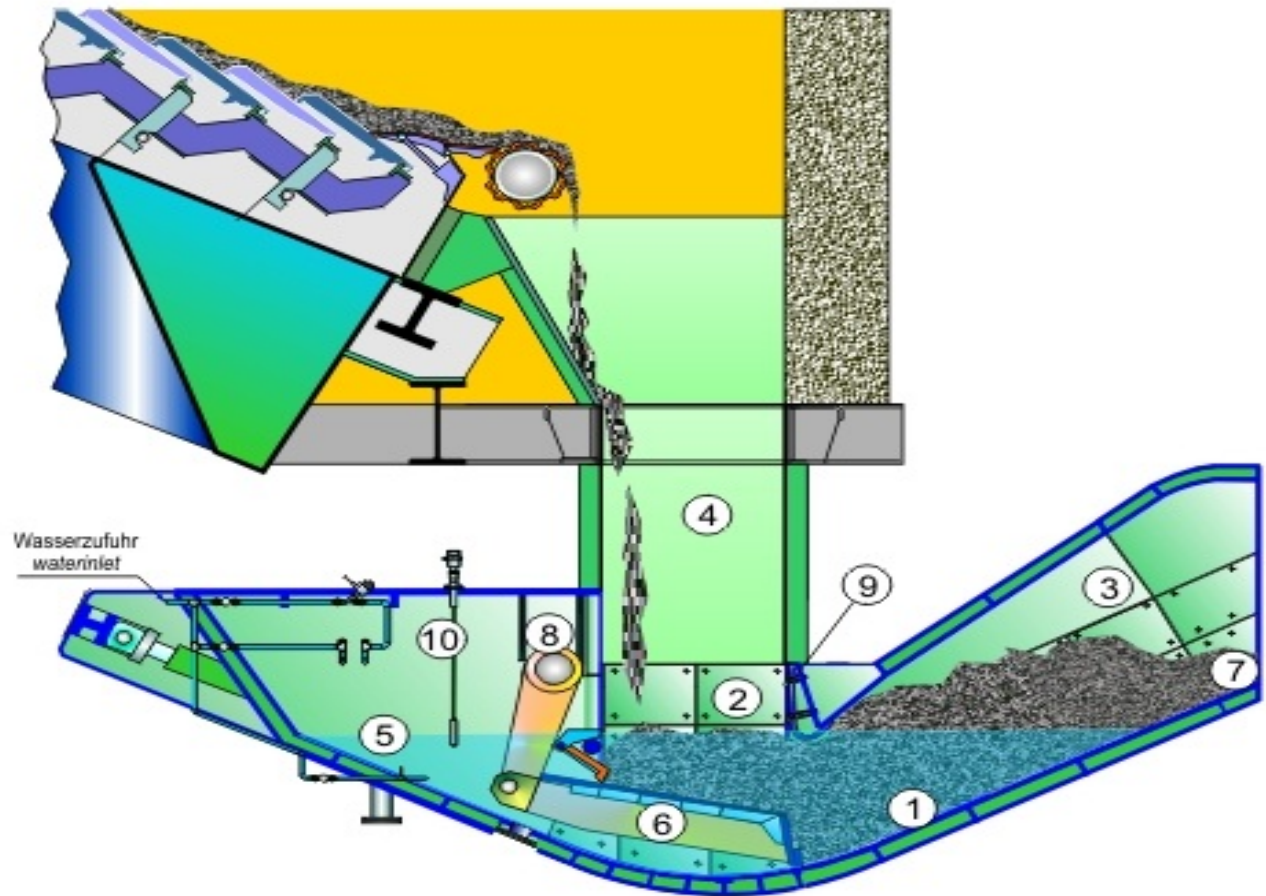
Sintered ceramic derived from Martins' dry discharged fine IBA



Effect of ash variability: The less than 4 mm wet discharged IBA

Wet discharged IBA: traditional process

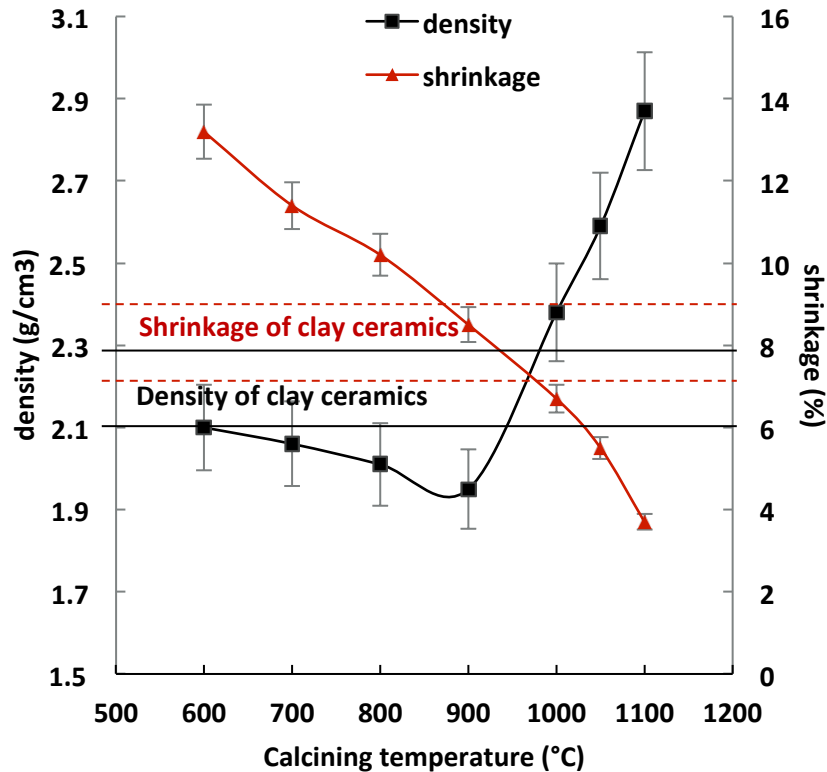
- 1 Discharger tub
- 2 Inlet section
- 3 Outlet chute
- 4 Connecting piece
- 5 Water level
- 6 Discharge ram
- 7 Drop-off edge
- 8 Drive shaft
- 9 Air sealing wall
- 10 Electrically-controlled level metering system



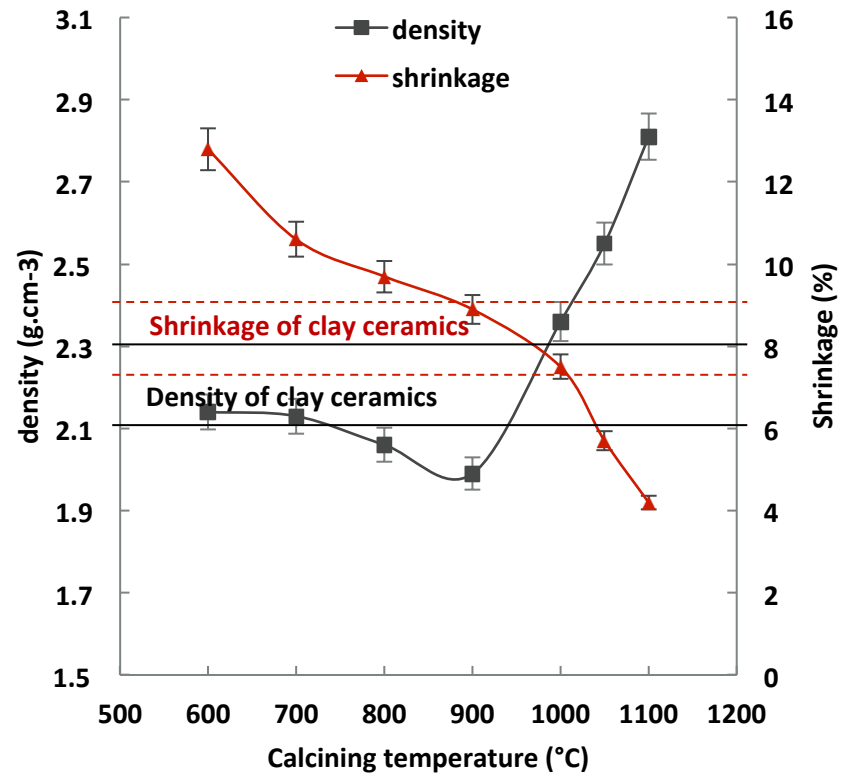
Effect of calcining temperature on density and shrinkage: 80 IBA- 20% glass mix

Wet milling 24 hours
Pressing Pressure: 32 Mpa
Firing temperature: 1080°C

Dry discharged sample



Wet discharged sample



Cost of processing

Cost of processing: IBA quantity

Assumptions:

- IBA is ~25 to 30% by mass of the Municipal Solid Waste (MSW) feedstock
- <500µm dry discharged IBA represents 10wt.% of total IBA
- <4 mm wet discharged IBA represents 40wt.% of total IBA

Dry discharge system:

- Monthey facility produces ~ 10,500 tonnes of less than 500µm IBA per year

Wet discharge system:

- In UK ~500,000 tonnes of less than 4 mm IBA produced per year

Cost of processing: IBA disposal costs

Switzerland¹:

	Haulage	Gate fee	Tax	Cost	
Method applied	(\$/ t)	(\$/ t)	(\$/ t)	\$/t	\$/ yr*
Stabilised in ultimate landfills	5.8	16.8	13	35.6	~ 373,800

United Kingdom²:

	Haulage	Gate fee	Tax	Cost	
Method applied	(\$/t)	(\$/t)	(\$/t)	\$/t	\$/ yr*
Non-hazardous landfills	5.8	48.5	128.3	182.6	~ 91.3 million

* assumption: 100% of the fine IBA is disposed of to landfills

¹ Data from CEWEP report, 2013

² Data from WRAP report, 2013

Cost of processing: Estimated lab scale, pilot scale and full scale costs

Scenario I: Ceramic tile production

Operation	Energy consumption ¹ (kWh/t fired product)	UK pilot plant operating costs per tonne IBA	Swiss pilot plant operating costs per tonne IBA
Milling	65	\$10.6	\$10.6
Spray Drying	7	\$1.2	\$1.2
Calcining	50	\$8.2	\$8.2
Pressing	14	\$2.3	\$2.3
Sintering	50	\$12.8	\$12.8
Landfill saving		\$182.6	\$35.6
Total²	186	- \$147.5	- \$0.5

¹Average values from EU BREF document on ceramic industries

²Total cost excludes the ceramic tile revenue to be defined by the application to be used. The tile can be used for the infrastructure (i.e. pavements) of the plant, therefore construction savings should be subtracted from the total. For Monthey plant the cost for mixing IBA with fly ash is excluded.

Cost of processing: Estimated lab scale, pilot scale and full scale costs

Scenario II: Ceramic powder production

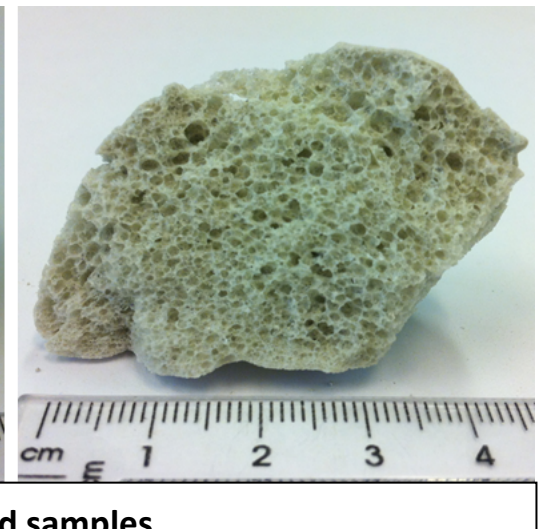
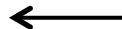
Operation	Energy consumption ¹ (kWh/t fired product)	UK pilot plant operating costs per tonne IBA	Swiss pilot plant operating costs per tonne IBA
Milling	65	\$10.6	\$10.6
Spray Drying	7	\$1.2	\$1.2
Calcining	50	\$8.2	\$8.2
Landfill saving		\$182.6	\$35.6
Total²	186	- \$162.6	- \$15.6

¹Average values from EU BREF document on ceramic industries

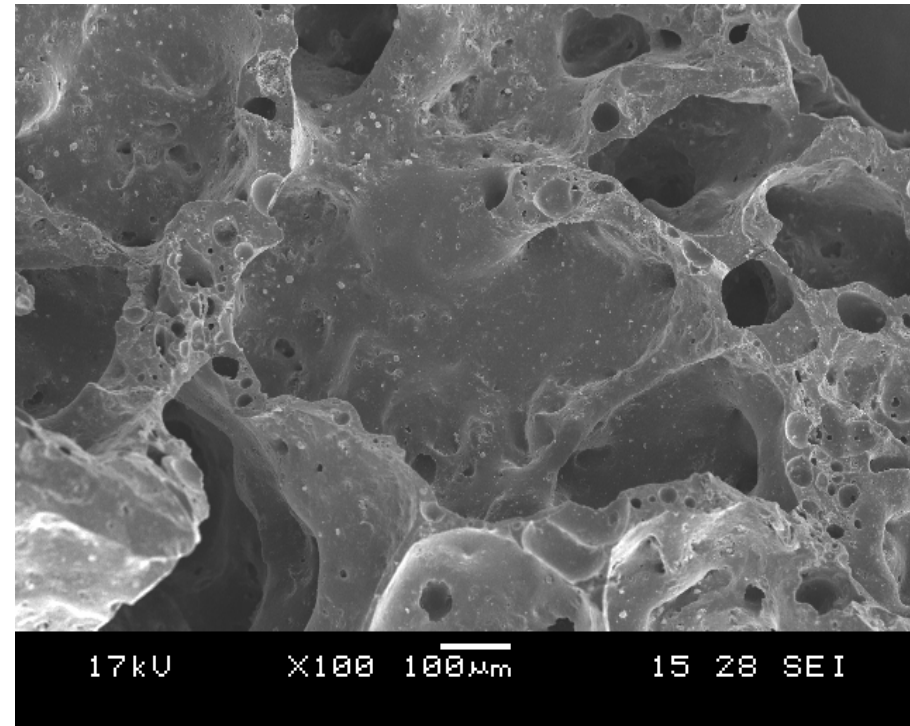
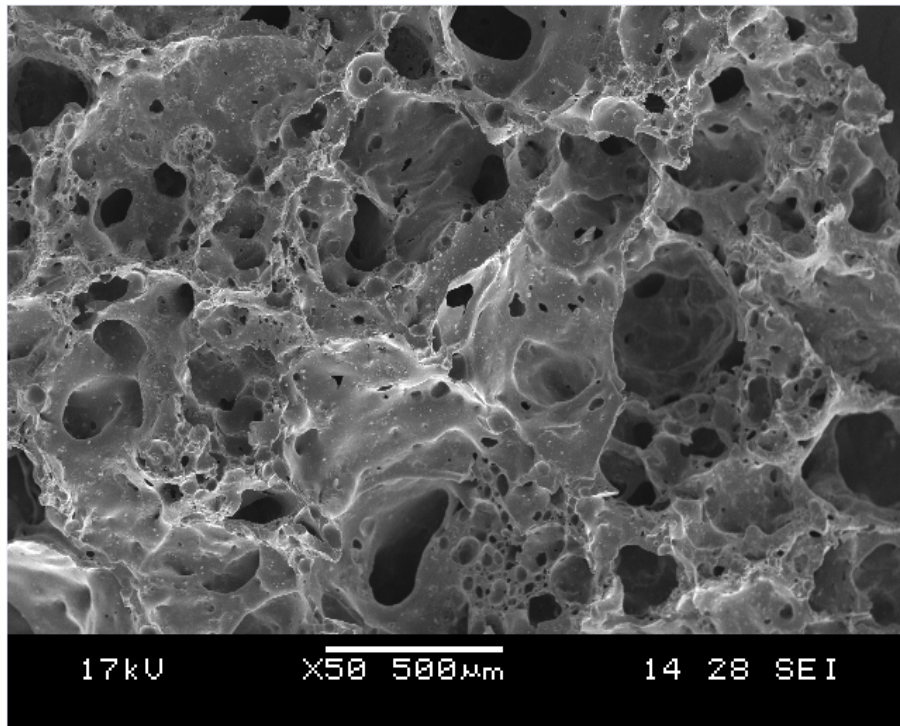
²Total cost excludes the ceramic powder revenue to be defined from the pyroxene ceramic to be used. For Monthey plant the cost for mixing IBA with fly ash is excluded.

Production of foamed materials containing fine IBA

Production of foamed glass containing IBA



Effect of rapid sintering: SEM images of foamed materials containing IBA



Conclusions

- Particle size, sintering and calcining temperature control properties and microstructure;
- Calcining at 1080°C produces:

Ceramics which have improved properties than commercial ceramic tiles

Different crystalline phases

- Calcining reduces the ANC and the leaching of metals compared to the as received fine IBA;
- Potential to manufacture powders suitable for ceramic production;
- Control of processing allows production of;

Dense monolithic ceramics

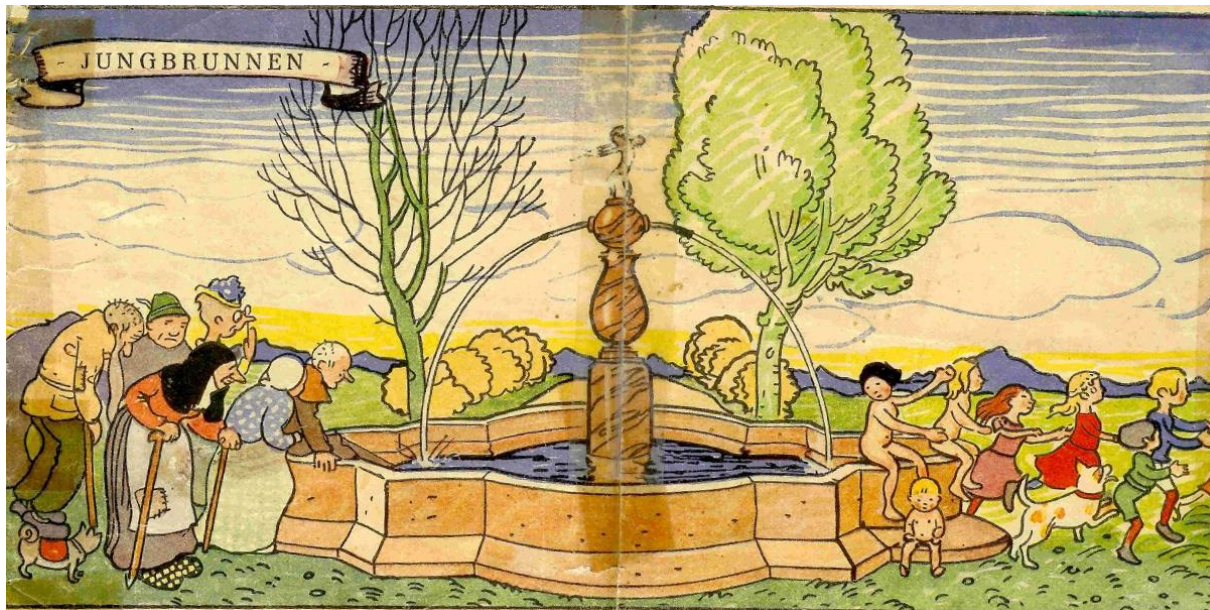
New lightweight foamed materials

Waste to Energy providing new material resources

Thank you very much for your attention!

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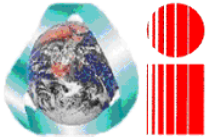
Chris Cheeseman: c.cheeseman@imperial.ac.uk



Acknowledgments



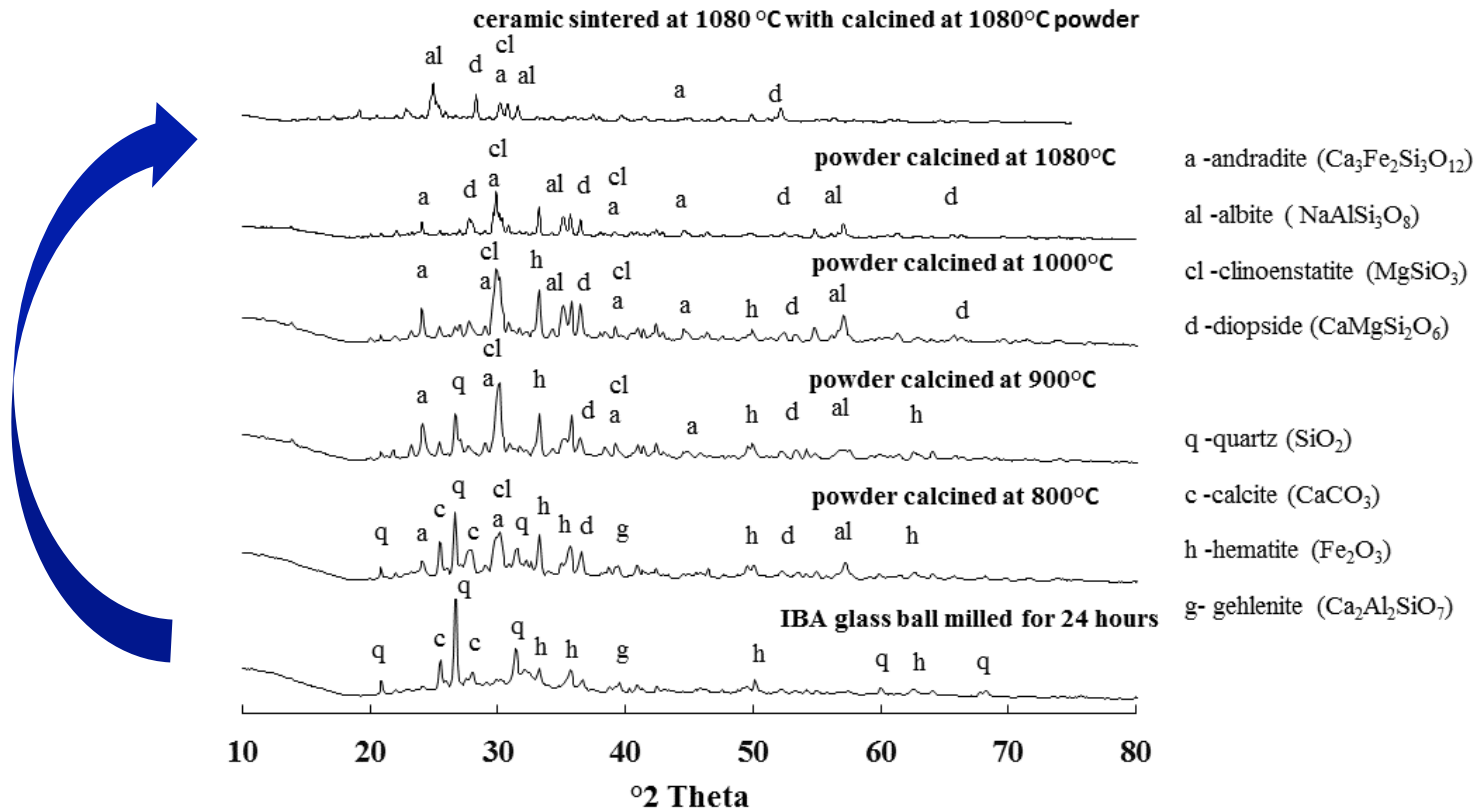
WtERT



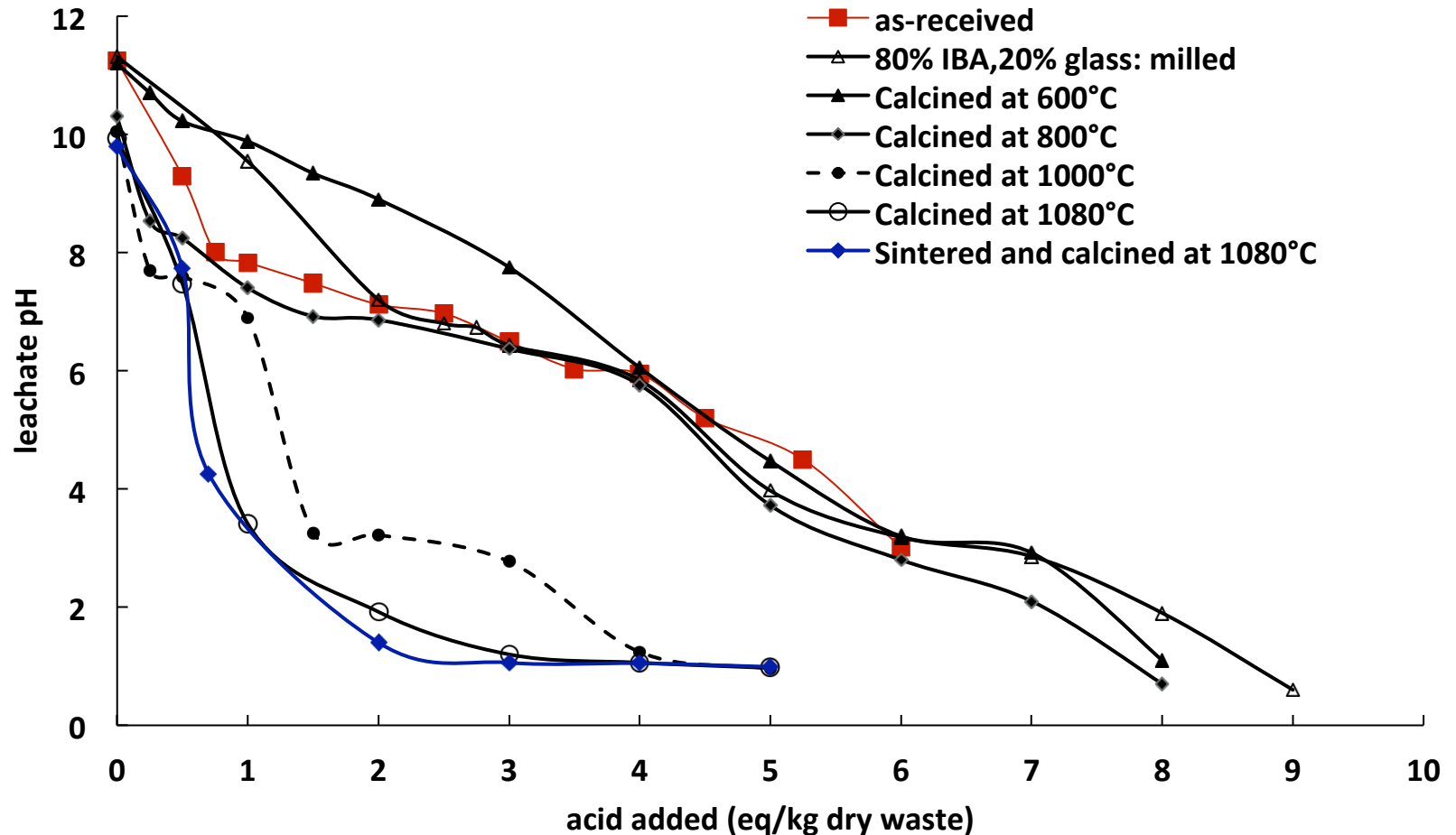
**Waste-To-Energy Research
and Technology Council**



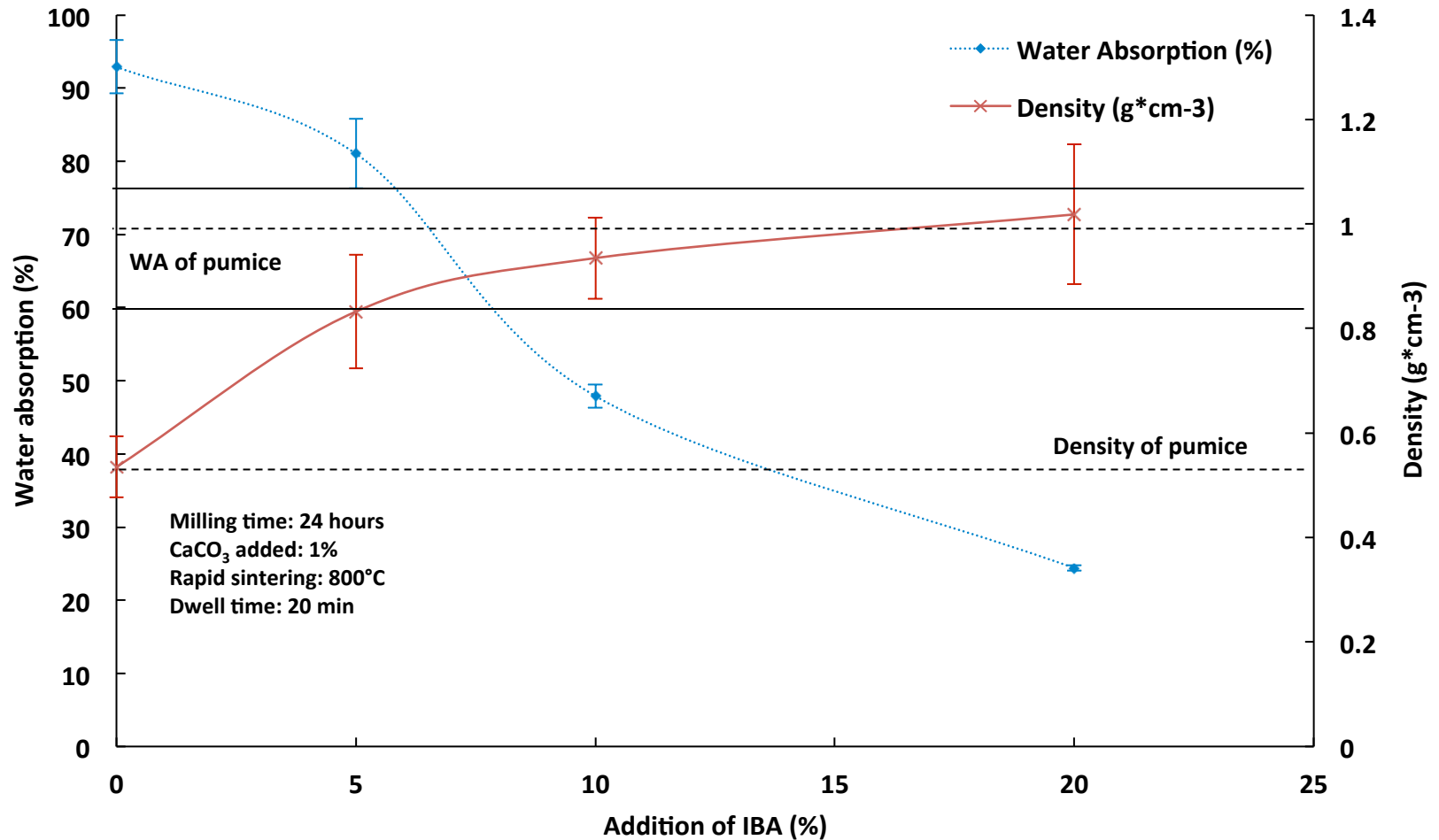
XRD during calcining: wet discharged IBA



Acid Neutralisation Capacity during calcining: Fine IBA from wet discharge process



Effect of rapid sintering: production of foamed materials



Acid Neutralisation Capacity

